



Leeds

Combustion Chemistry

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UNIVERSITY OF LEEDS

Background 1

- Combustion involves the oxidation of a fuel, ideally leading, for an organic fuel such as octane or ethanol, to the formation of carbon dioxide and water, with the release of heat.
- The overall chemical equation, e.g.
$$\text{C}_2\text{H}_5\text{OH} + 3.5\text{O}_2 \rightarrow 2\text{CO}_2 + 3\text{H}_2\text{O}$$
does not describe the way in which the reaction occurs.
- Instead the reaction involves a sequence of elementary, or single step reactions, many of which involve atoms or radicals, which are short-lived species with high reaction rates.

Background 2

This series of lectures examines how the rates of these elementary reactions can be determined experimentally and understood theoretically; how chemical mechanisms describing the overall sequence of reactions can be constructed and then used to model the chemistry of combustion systems.

An example - $\text{H}_2 + \text{O}_2$

The overall reaction is: $2\text{H}_2 + \text{O}_2 \rightarrow 2\text{H}_2\text{O}$

A minimal set of the component elementary reactions is:

1. $\text{H}_2 + \text{O}_2 \rightarrow \text{H} + \text{HO}_2$
2. $\text{H} + \text{O}_2 \rightarrow \text{OH} + \text{O}$
3. $\text{O} + \text{H}_2 \rightarrow \text{OH} + \text{H}$
4. $\text{OH} + \text{H}_2 \rightarrow \text{H} + \text{H}_2\text{O}$
5. $\text{H} + \text{O}_2 + \text{M} \rightarrow \text{HO}_2 + \text{M}$
6. $\text{H}, \text{O}, \text{OH} \rightarrow \text{wall}$
7. $\text{HO}_2 + \text{HO}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2$

Rates of elementary reactions

- The rate of each elementary reaction is determined by the reactant concentrations and the rate coefficient, k . k depends on T and, in some cases p .

We also need to know the products of the reaction, which in some cases isn't clear.

- Example: reaction 2:** $\text{H} + \text{O}_2 \rightarrow \text{OH} + \text{O}; k_2$

Rate of this reaction = $-\text{d}[\text{H}]/\text{d}t = k_2[\text{H}][\text{O}_2] = \text{d}[\text{OH}]/\text{d}t = \text{d}[\text{O}]/\text{d}t$

- k_2 depends on temperature and this is usually expressed in Arrhenius form:

$$k_2 = A \exp(-E_a/RT)$$

or modified Arrhenius form:

$$k_2 = AT^n \exp(-E_a/RT)$$

A is the A factor, E_a the activation energy, n the temperature exponent and R the gas constant.

- One aim of experimental and theoretical studies of elementary reactions is to determine A , E_a , n
- Definitions: **order of reaction**; **units** of rate coefficients

Relationship between forward and reverse rate coefficients (e.g. $\text{H}_2 + \text{O}_2 \rightarrow \text{H} + \text{HO}_2$ and the reverse)

$$K = \frac{\prod_{\text{products}} (a_i^{\nu_i})}{\prod_{\text{reactants}} (a_i^{\nu_i})}$$

a is the *activity*. For ideal systems, $a = p/p^\circ = c/c^\circ$ so that K is dimensionless. Other definitions of equilibrium constants are:

$$K_c = \frac{\prod_{\text{products}} (c_i^{\nu_i})}{\prod_{\text{reactants}} (c_i^{\nu_i})} \quad K_p = \frac{\prod_{\text{products}} (p_i^{\nu_i})}{\prod_{\text{reactants}} (p_i^{\nu_i})}$$

These have dimensions if $(\sum \nu_i)_{\text{reactants}} \neq (\sum \nu_i)_{\text{products}}$

At equilibrium, forward rate = reverse rate:

$$k_f \prod_{\text{products}} (c_i^{\nu_i}) = k_r \prod_{\text{reactants}} (c_i^{\nu_i}) \quad \frac{k_f}{k_r} = K_c$$

Detailed balance
Use of thermodynamic databases

Thermodynamic relations (more detail on Wednesday)

At constant T , the Gibbs energy, G is given by:

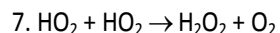
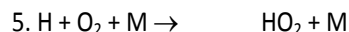
$$\Delta G = \Delta H - T\Delta S$$

and the equilibrium constant is related to ΔG by:

$$RT\ln K = -\Delta G$$

The equilibrium constant, K , can be calculated from tabulated values of the enthalpy H and entropy S , and hence the reverse rate coefficient (say) determined from the forward rate coefficient and K .

Constructing coupled differential (rate) equations from chemical mechanisms



The chemical mechanism is set up together with the associated rate coefficients

The coupled rate equations are then written down for each species
 $d[\text{X}]/dt$ = Total rate of forming X - Total rate of removing X:

$$\frac{d[\text{H}]}{dt} = k_1[\text{H}_2][\text{O}_2] - k_2[\text{H}][\text{O}_2] + k_3[\text{O}][\text{H}_2] + k_4[\text{OH}][\text{H}_2] - k_5[\text{H}][\text{O}_2][\text{M}] - k_6[\text{H}]$$

$$\frac{d[\text{O}]}{dt} = k_2[\text{H}][\text{O}_2] - k_3[\text{O}][\text{H}_2] - k_6[\text{O}]$$

etc

Solve the set of coupled differential equations numerically, subject to initial conditions.

The quasi steady state approximation, QSSA

- The QSSA is sometimes used to simplify kinetic problems
- Consider the scheme:

$A \rightarrow B \rightarrow C$, with rate coefficients k_1 and k_2

Set up the rate equations, with $a = [A]$, etc.

$$\frac{da}{dt} = -k_1 a; \quad \frac{db}{dt} = k_1 a - k_2 b$$

$$a = a_0 \exp(-k_1 t)$$

$$b = \frac{a_0 k_1}{(k_2 - k_1)} \{ \exp(-k_1 t) - \exp(-k_2 t) \}$$

$$c = a_0 - a - b$$

QSSA continued

Figure (a): $k_1 > k_2$ $b = \frac{a_0 k_1}{(k_1 - k_2)} \{ \exp(-k_2 t) - \exp(-k_1 t) \}$

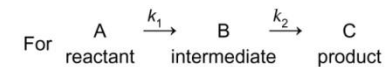
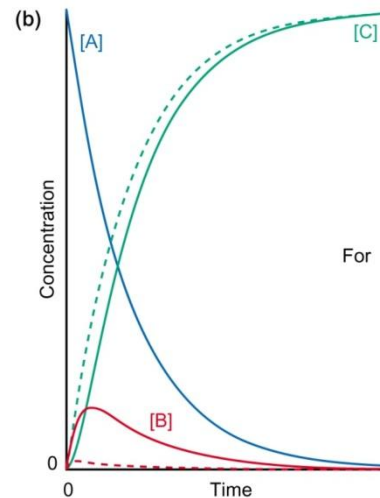
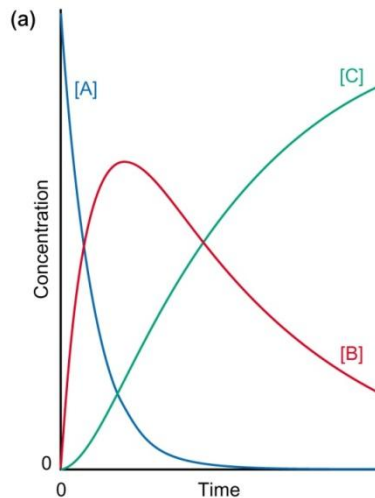


Figure (b): full, $k_2 = 5k_1$
 dashed, $k_2 = 50k_1$

Figure (b): $k_1 < k_2$ $b = \frac{a_0 k_1}{(k_2 - k_1)} \{ \exp(-k_1 t) - \exp(-k_2 t) \}$

For $k_1 \ll k_2$ and for times long compared with $(k_2)^{-1}$

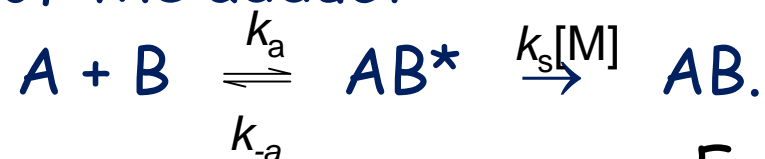
$$b = \frac{a_0 k_1}{(k_2 - k_1)} \{ \exp(-k_1 t) \} \approx \frac{a_0 k_1}{k_2} \{ \exp(-k_1 t) \} = \frac{a k_1}{k_2}$$

$$\therefore b \ll a \text{ and } \frac{db}{dt} \ll \frac{da}{dt}$$

- QSSA: $db/dt \approx 0$: rate of forming of B \approx rate of removing B

Pressure dependent association reaction

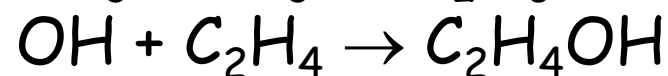
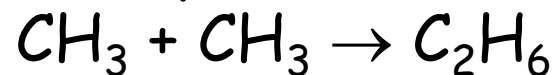
An association reaction involves collisional stabilisation of the adduct:



Apply QSSA:

$$k = \frac{k_a k_s [M]}{k_{-a} + k_s [M]}$$

Examples include



$$\text{As } [M] \rightarrow \infty, k \rightarrow k_a = k^\infty$$

$$\text{As } [M] \rightarrow 0, k \rightarrow \frac{k_a k_s [M]}{k_{-a}} = k_0 [M]$$

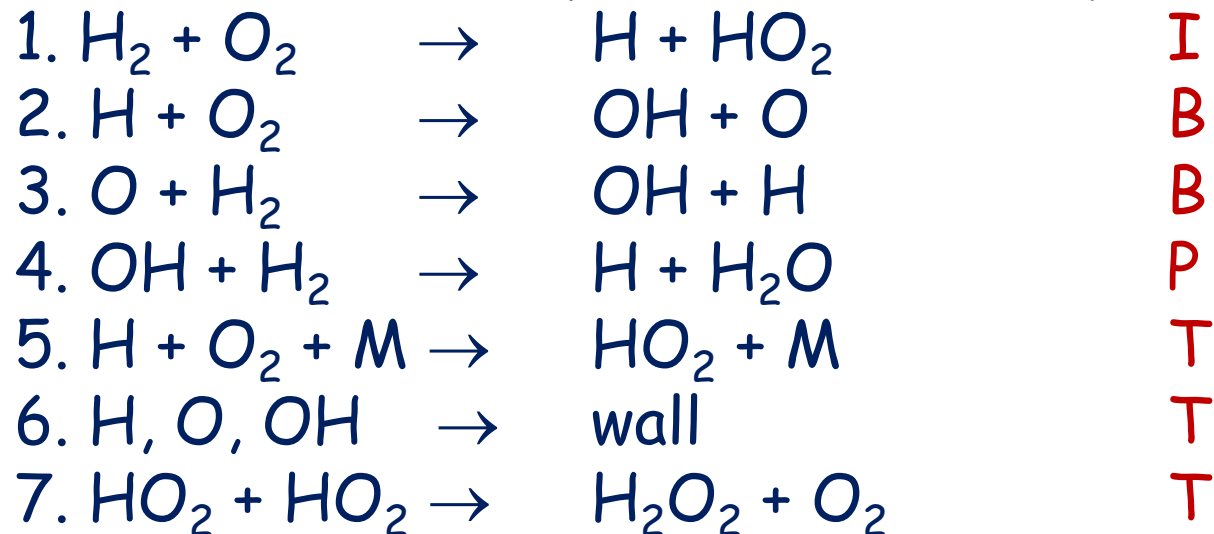
Substituting in first equation

$$k = \frac{k_0 [M] k^\infty}{k^\infty + k_0 [M]}$$

Similar treatment
for dissociation
reactions

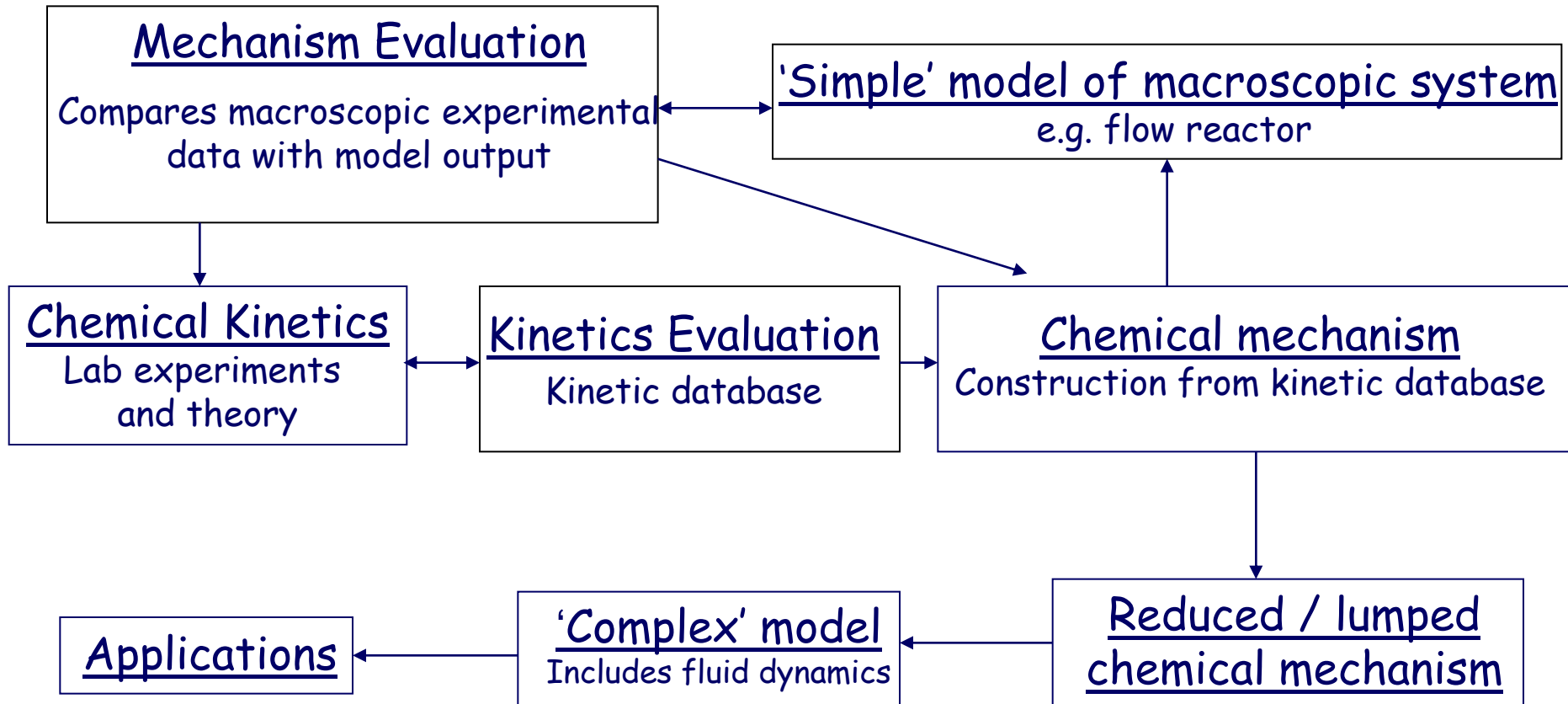
Types of elementary reaction in combustion

A minimal set of the component elementary reactions is:



- Types of reaction: I = initiation; B = branching; P = propagation, T = termination

Reaction kinetics contributions to combustion models



Understanding
Similar approaches in atmospheric chemistry,
interstellar chemistry.

Synopsis

- Topic 1: Experimental measurements of rate coefficients and product yields for elementary reactions.
- Topic 2: Linking experiment and theory.
- Topic 3: Thermodynamics.
- Topic 4: Rate coefficient evaluation
- Topic 5: Mechanism construction and evaluation.
- Topic 6: NO_x chemistry.
- Topic 7: Combustion emissions, climate change and air quality.

Measurement of rates of elementary reactions 1

- Concentrate on reactions of atoms and radicals; say something briefly about reactions that don't involve radicals and are involved in initiation steps
- Need to cover a range of T from 1000 to 3000 K for reactions involved in high temperature combustion reactions; 600 - 1000 K for low T oxidation in the autoignition regime; 200 - 300 K for reactions of combustion generated pollutants in the lower atmosphere (the troposphere)

Measurement of rates of elementary reactions 2

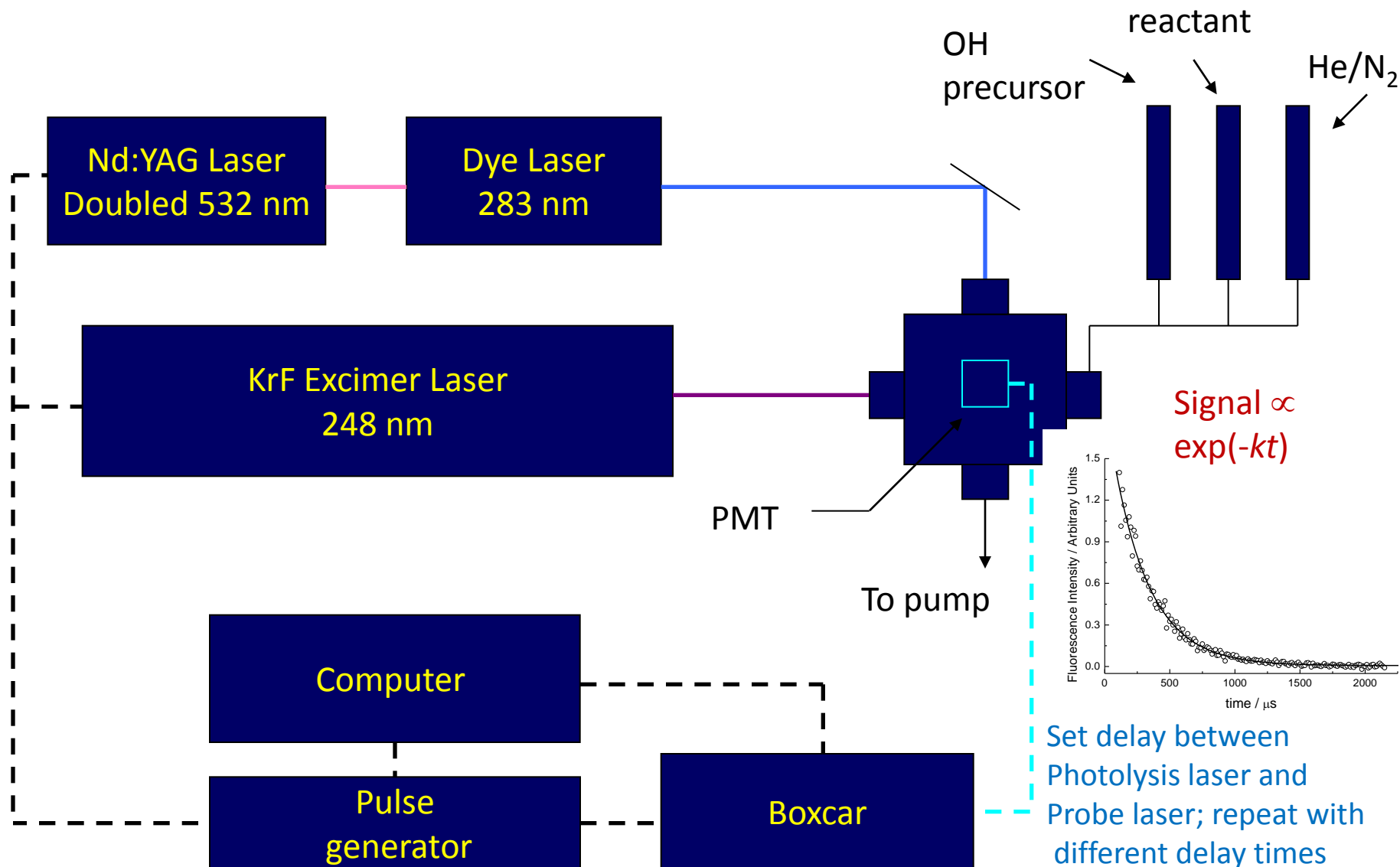
- Ideally, isolate the individual reaction and study it at the appropriate combustion conditions.
- Not always possible:
 - May have to model the system to extract k s of interest
 - May need to extrapolate to appropriate T , p . Ideally achieve this with the help of theory.

Techniques

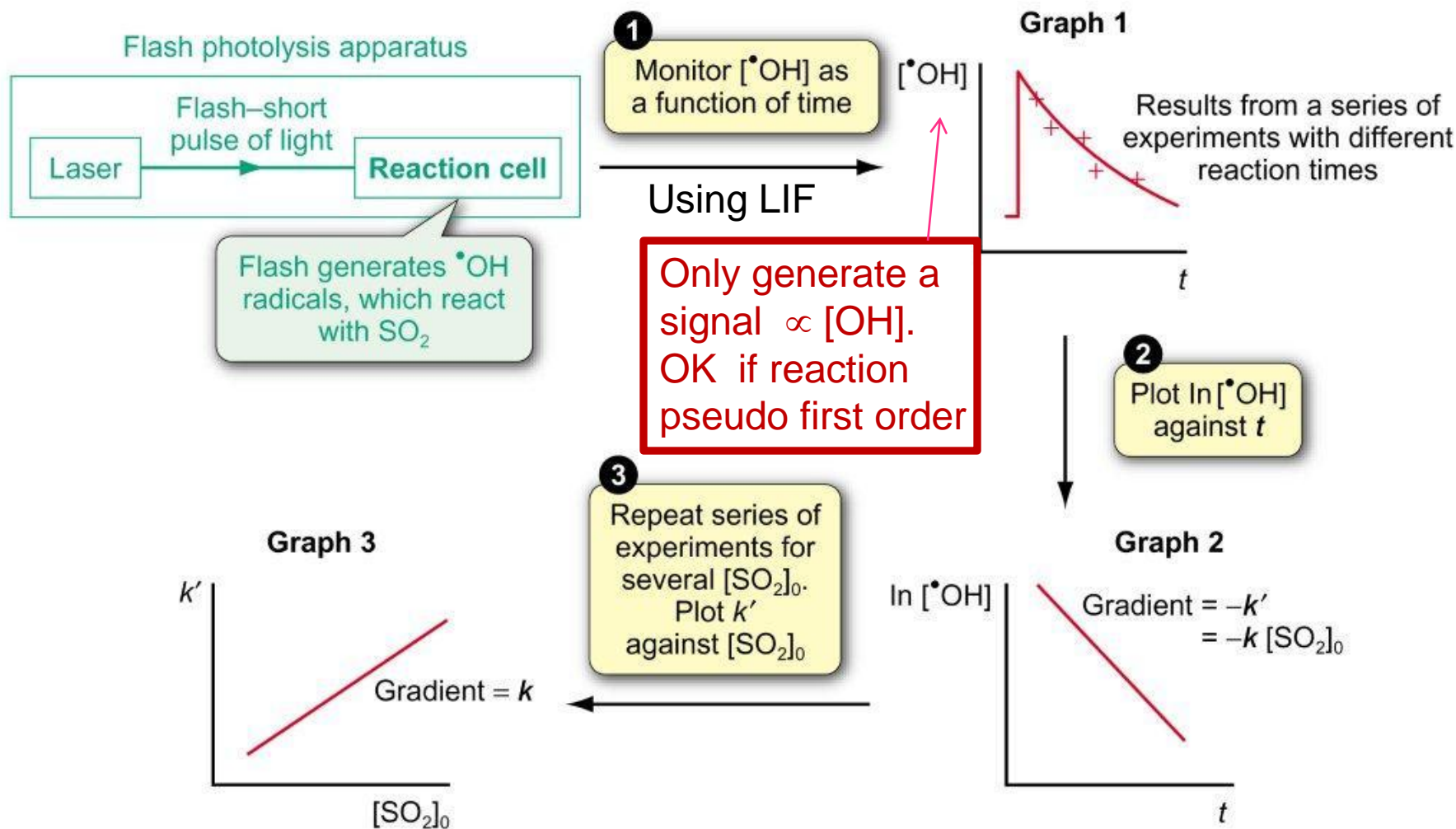
- Pulsed laser photolysis (laser flash photolysis)
- Shock tubes
- Flow tubes for elementary reactions and whole systems
- Static studies of whole systems

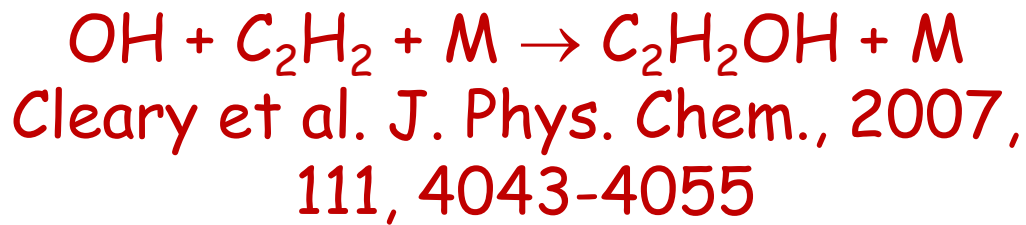
Pulsed laser photolysis

Laser flash photolysis (LFP) / laser induced fluorescence (LIF) for the study of OH + reactant

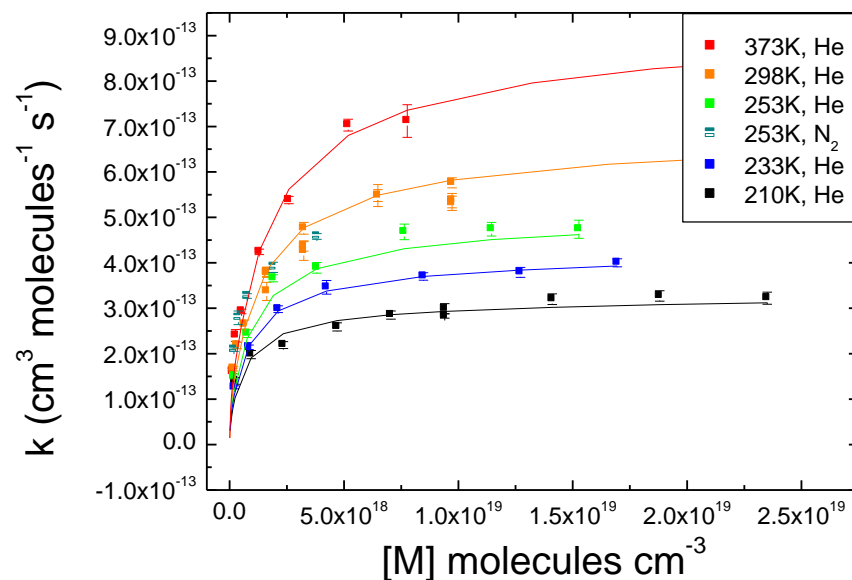
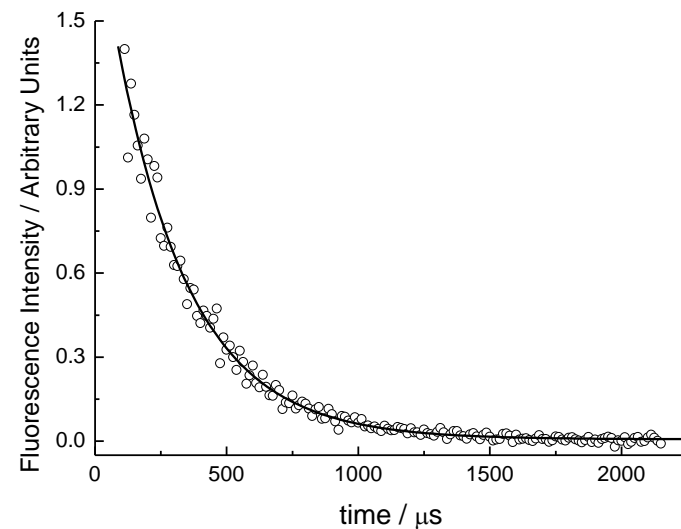
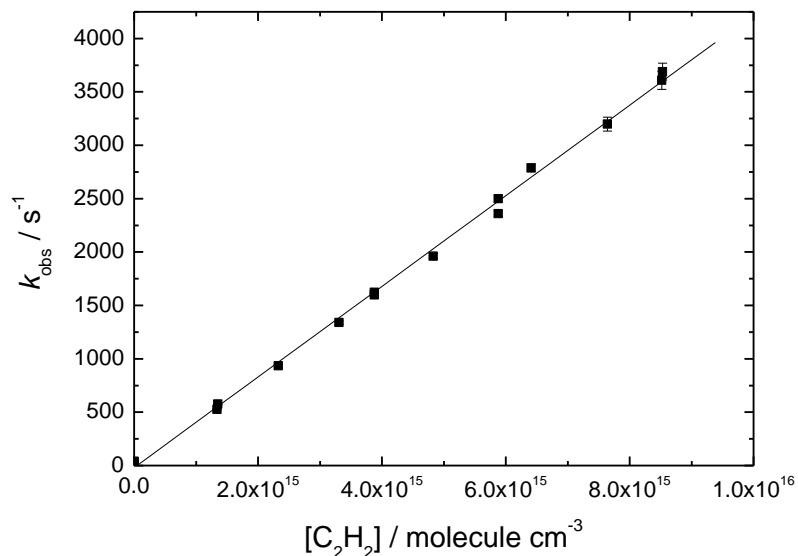


Procedure for determining rate coefficients for pseudo first order reactions using LFP for $\text{OH} + \text{SO}_2$



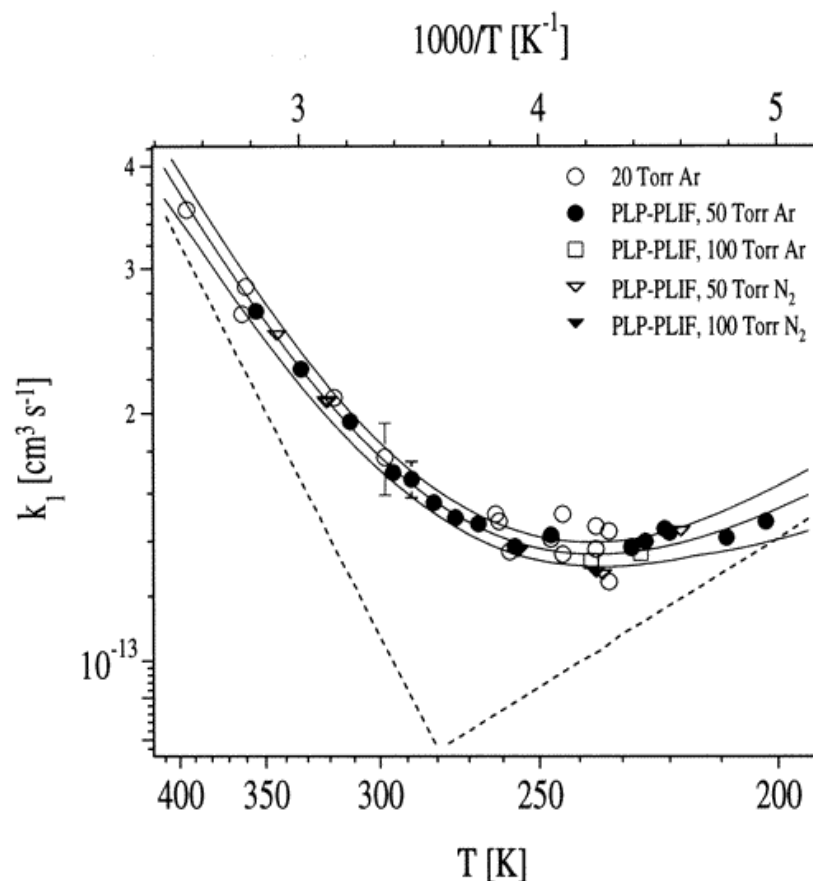
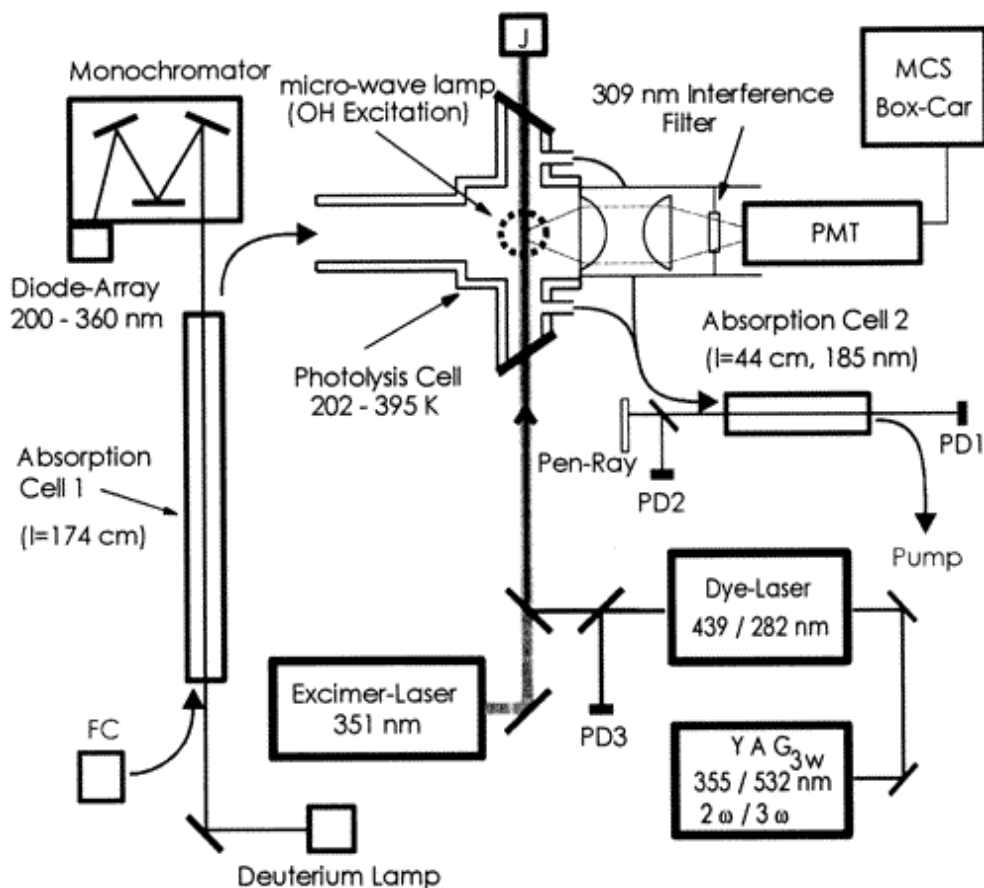


- Pressure dependent (association) reaction.
- Study as a function of temperature and pressure



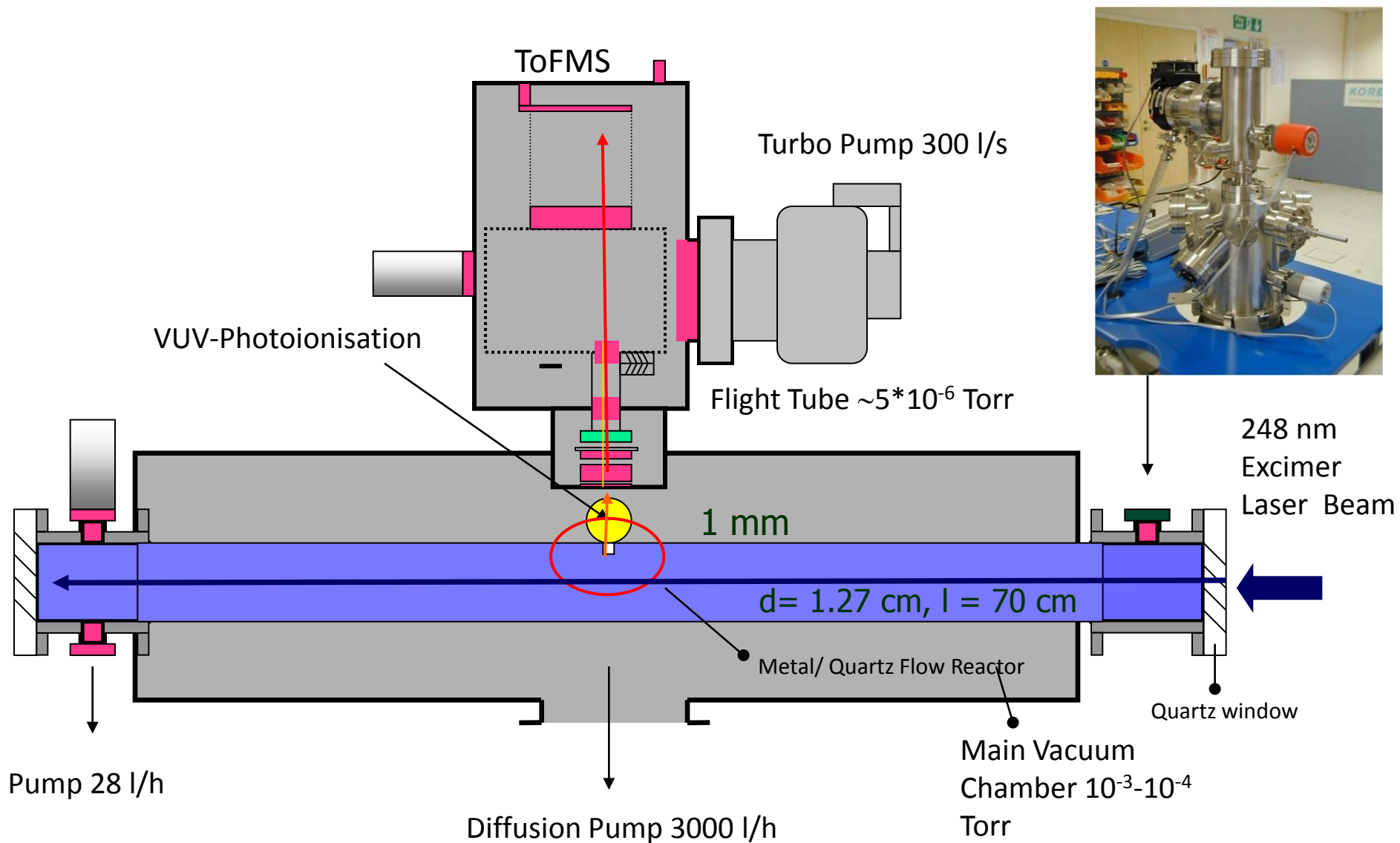
OH + acetone, J N Crowley, JPCA, 2000, 104,2695

laser flash photolysis, resonance fluorescence/laser induced fluorescence **to measure [OH] (relative)**. Optical measurement of **[acetone]** before and after reactor.



Detection using time of flight mass spectrometry

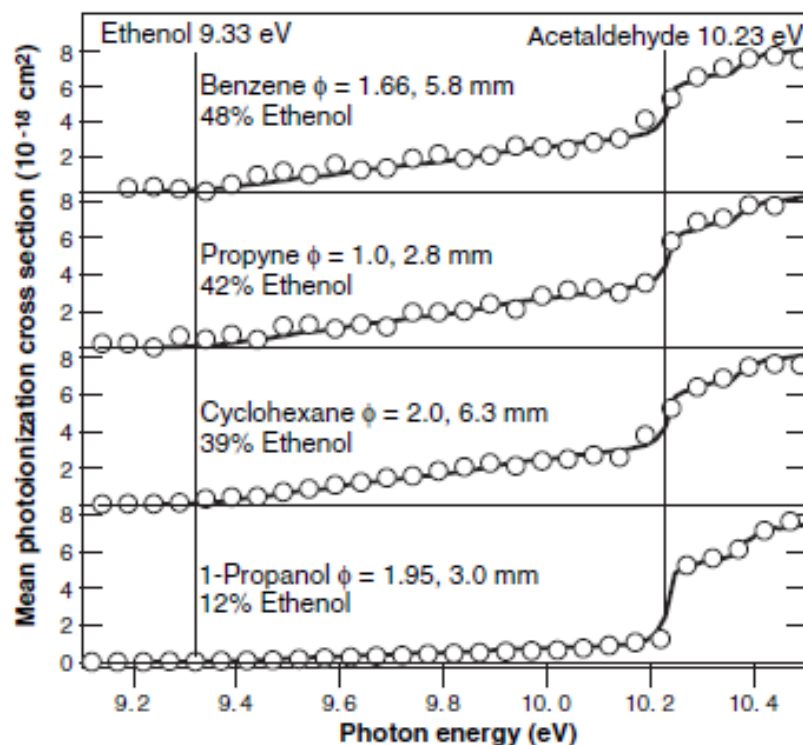
Blitz et al. Rev. Sci. Inst. 2007, 78, 034103



Application of synchrotron radiation for photoionization (SVUV-PIMS) to distinguish isomers in flames

1. ALS, USA

- ALS is tuneable and so it is feasible to distinguish isomers, which have the same mass, through their differing photoionization efficiency curves.
- Traces show $m/z=44$ for different flames:
acetaldehyde: CH_3CHO
ethanol: $\text{CH}_2=\text{CHOH}$

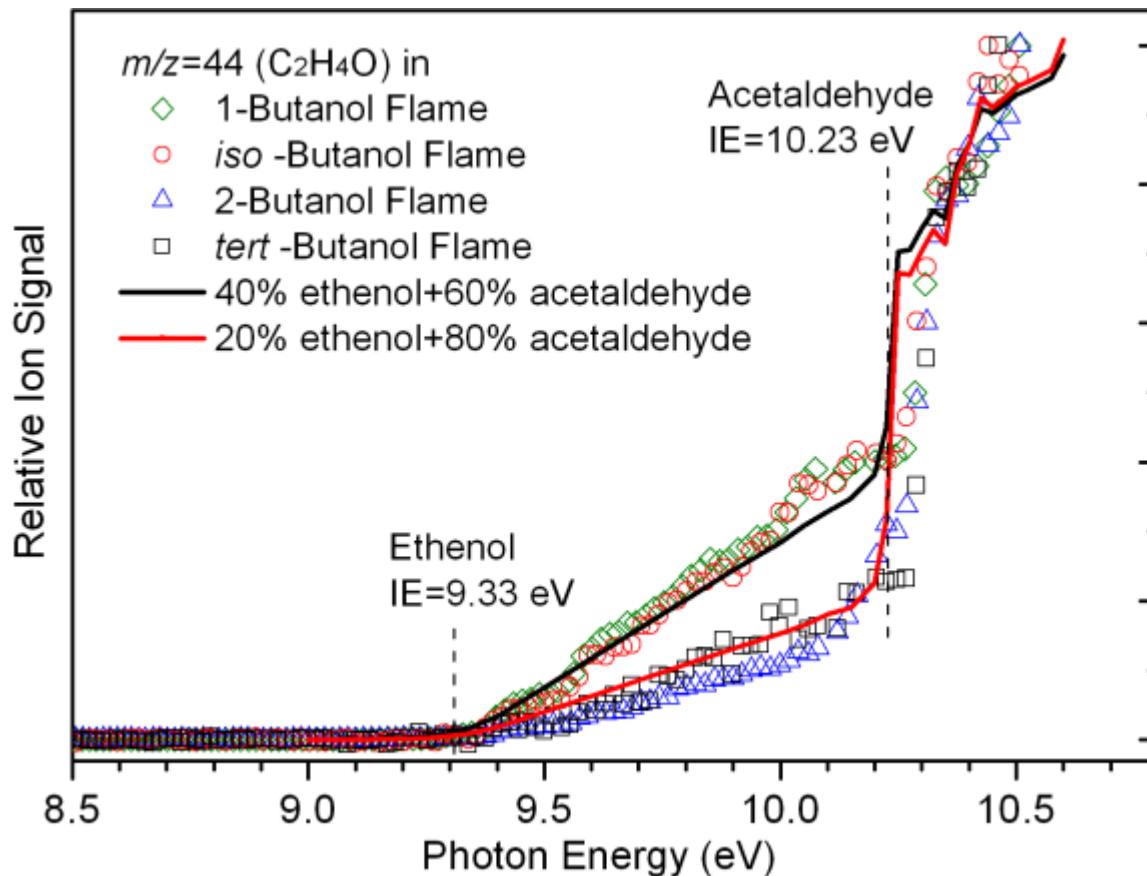


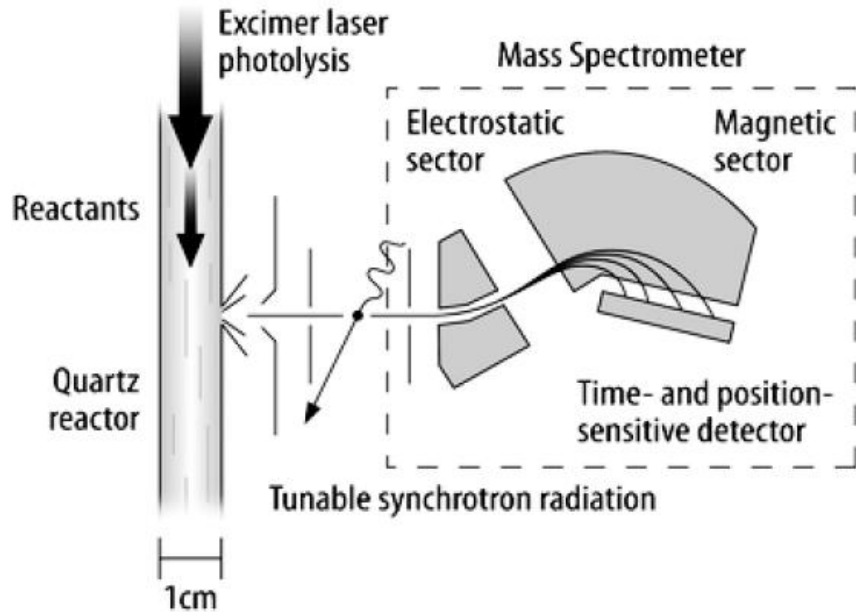
Taatjes et al. *Science* 2005, **308**, 1887

2. NSRL China

Various butanol flames,

- Yang et al. Combust. Flame 148 (2007) 198-209.

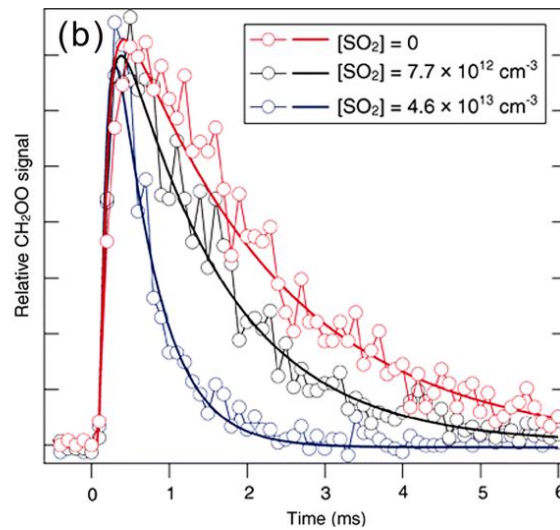
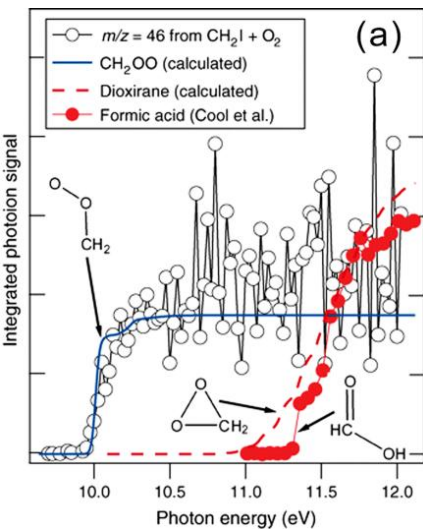




SVUV-PIMS for kinetics

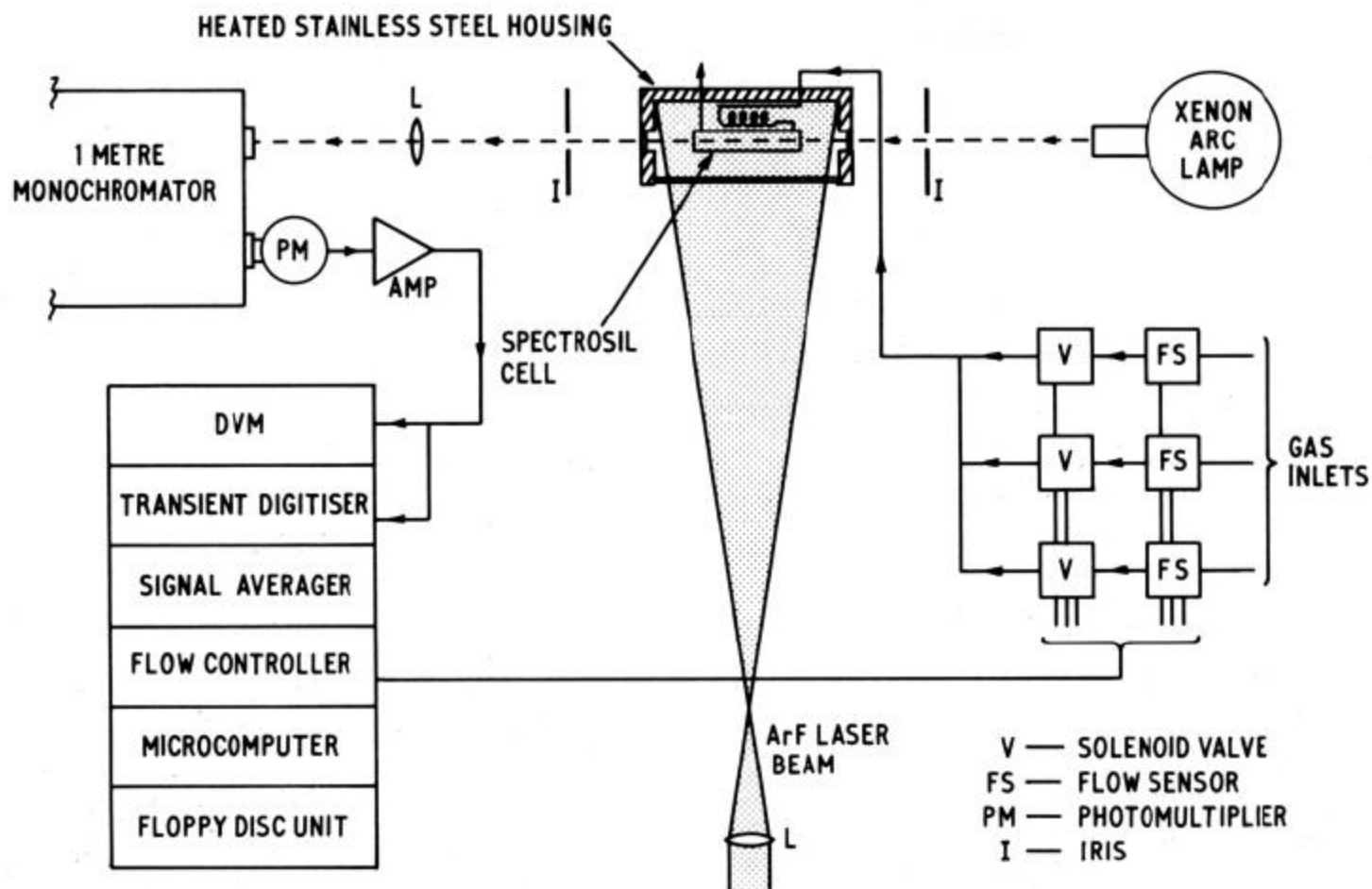
Taatjes et al., PCCP, 2008, 10, 20 - 34

(a) The calculated photoionization spectra of the Criegee intermediate CH_2OO and dioxirane, the experimental photoionization spectrum for formic acid, as well as schematic chemical structures, are shown.



(b) Time-dependent CH_2OO signals for various concentrations of SO_2 . Solid lines represent fits to the data traces, including convolution with a measured instrument response function, from which pseudo-first order decay constants are derived Welz et al. Science 335, 204-207

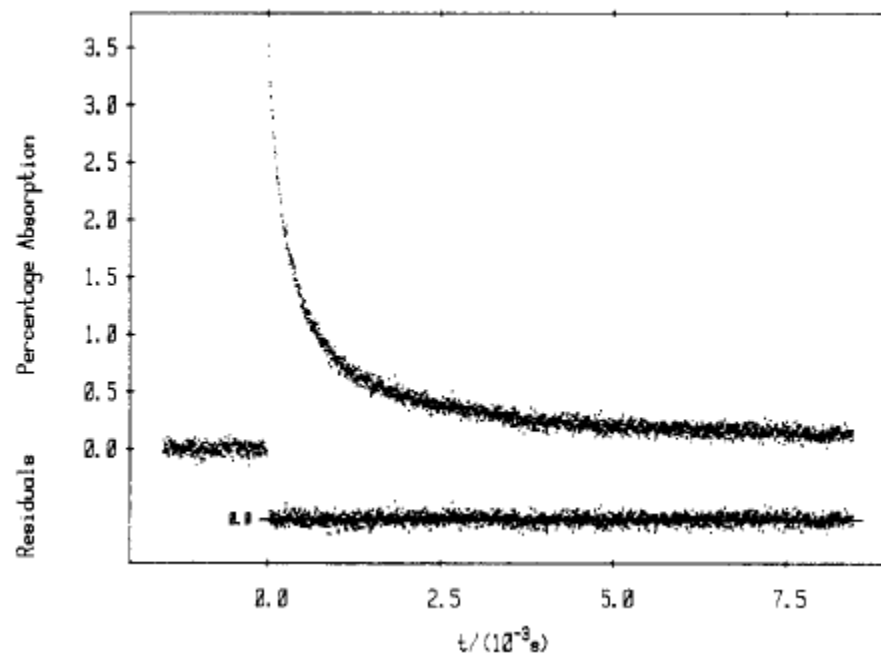
Radical detection using absorption spectroscopy: $C_3H_5 + C_3H_5$



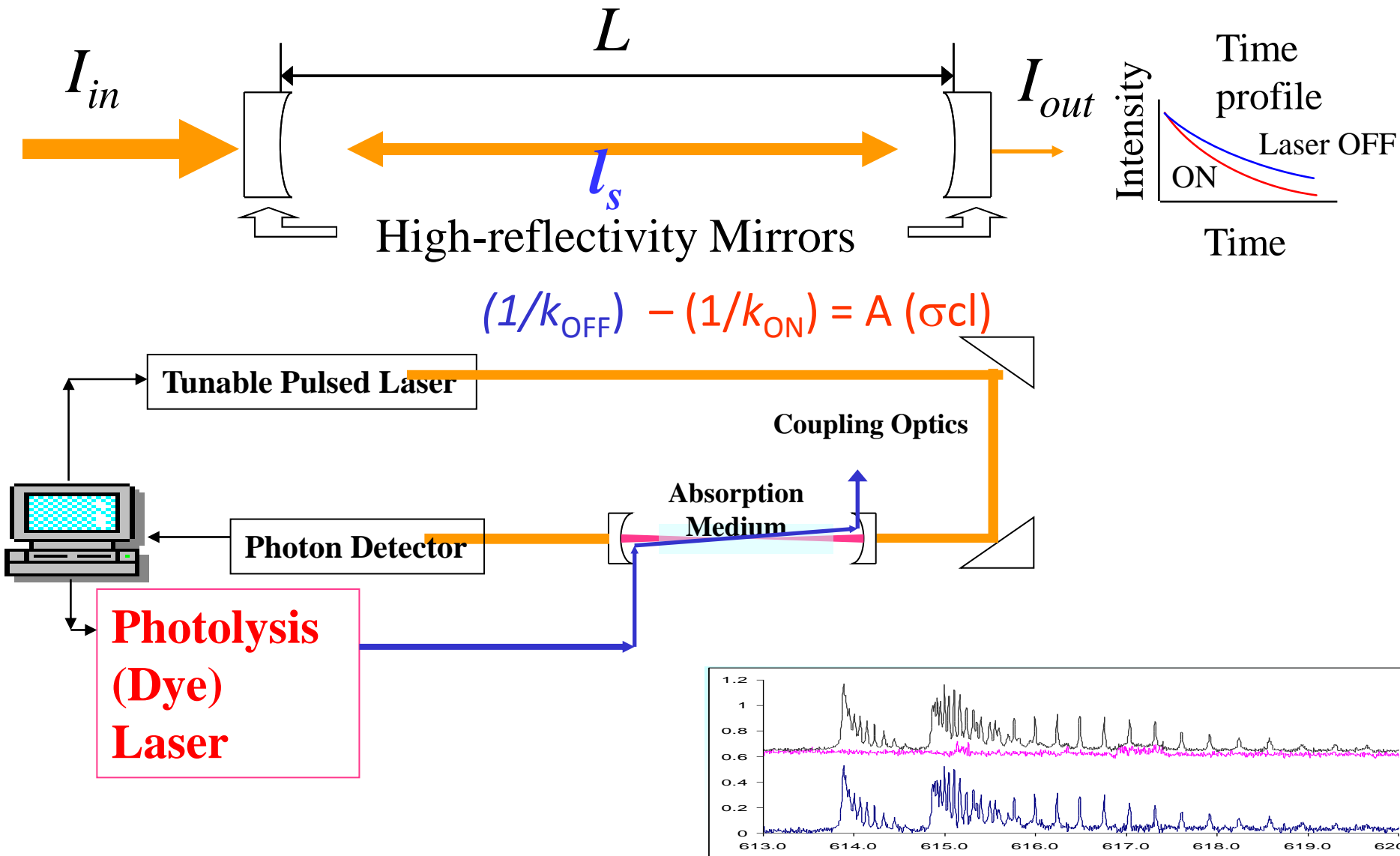
Reaction is second order in the radical - need the absolute concentration to determine k .

$C_3H_5 + C_3H_5$: Absorption spectroscopy 2

- Reaction is second order in C_3H_5
- Need to know absolute concentration of radical - absorption spectroscopy provides a good route to this. (see J. Phys. Chem. 1985, 89, 2268-2274 for discussion for CH_3)
- $I/I_0 = \exp(-\sigma[C_3H_5]L)$ where I_0 is the incident and I the transmitted light intensity, σ is the absorption cross section and L is the path length.

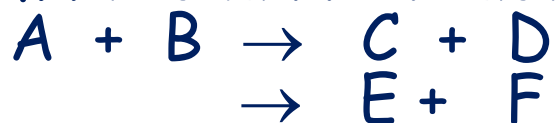


Detection of HCO using cavity ring down spectroscopy (CRDS)

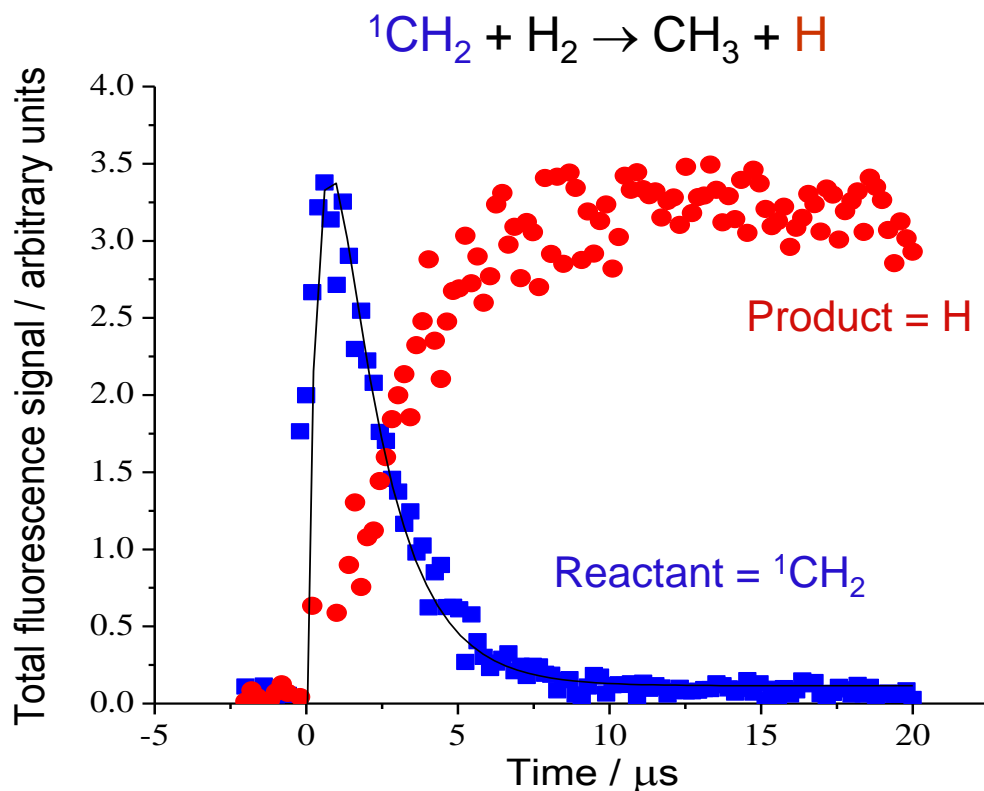


Determination of product yields by Laser Flash Photolysis 1

- Use laser pulse to generate radical on short timescale (~ 10 ns)
- Observe radical concentration vs time. Obtain kinetics from decay time constant
- Also observe product - calibration gives channel yield for a multi channel reaction:



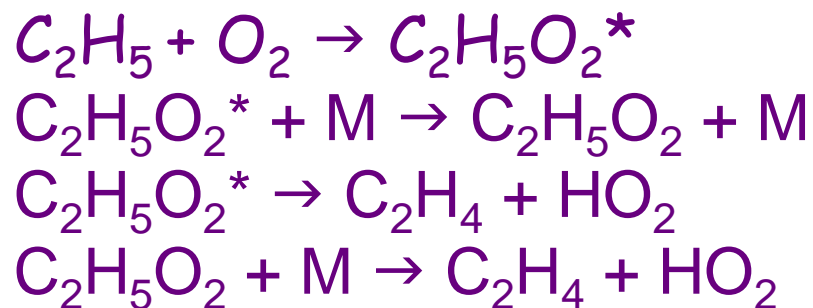
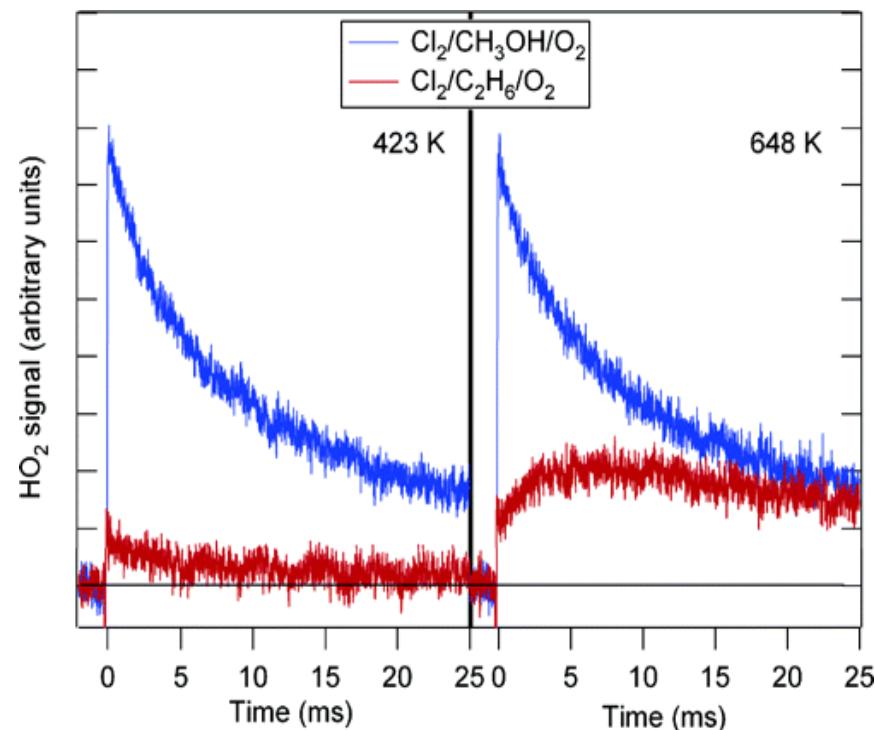
Detection technique :
laser induced
fluorescence
for CH_2 and H



Determination of product yields by Laser Flash

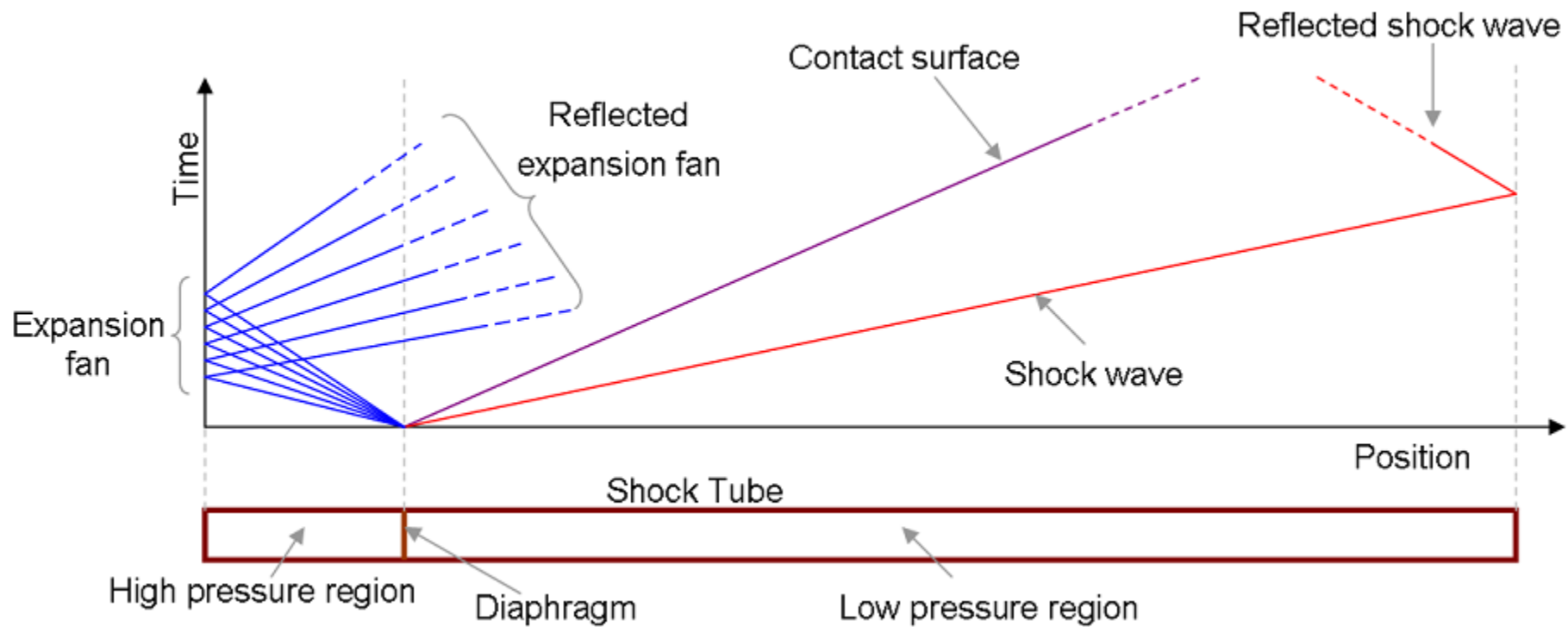
Photolysis 2: $C_2H_5 + O_2$

- Taatjes et al. (J. Phys. Chem. A 104 (2000) 11549 - 11560) observed the formation of OH and HO_2 , determining the fractional yields. Used 100% yield of HO_2 from $CH_2OH + O_2$ to calibrate the system.
- HO_2 yield \uparrow as $T \uparrow$ and $p \downarrow$
- Two timescales at higher T
- OH yield is small.
- Theoretical interpretation and relevance to autoignition chemistry will be discussed later

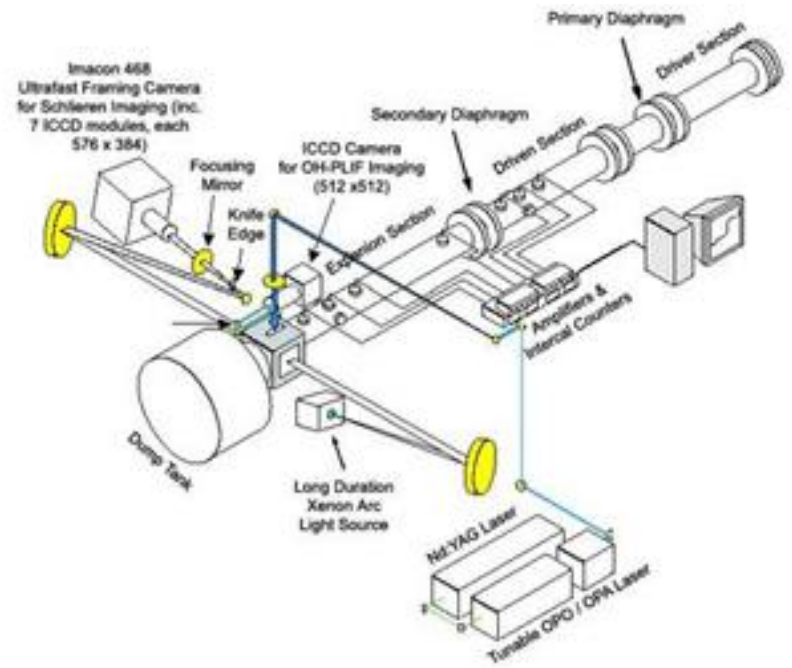
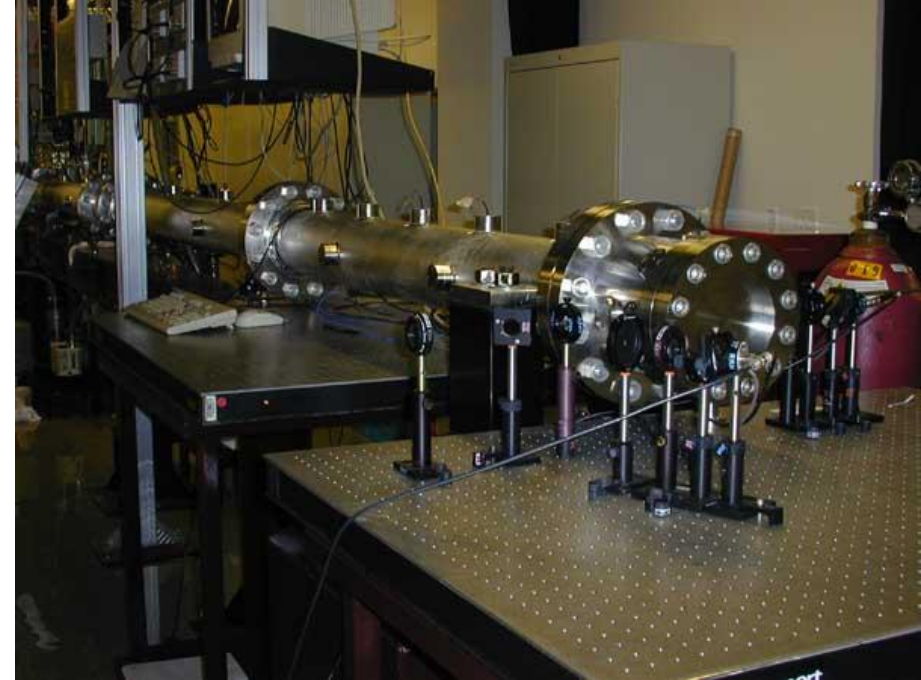


Shock tubes

Shock tube - basics

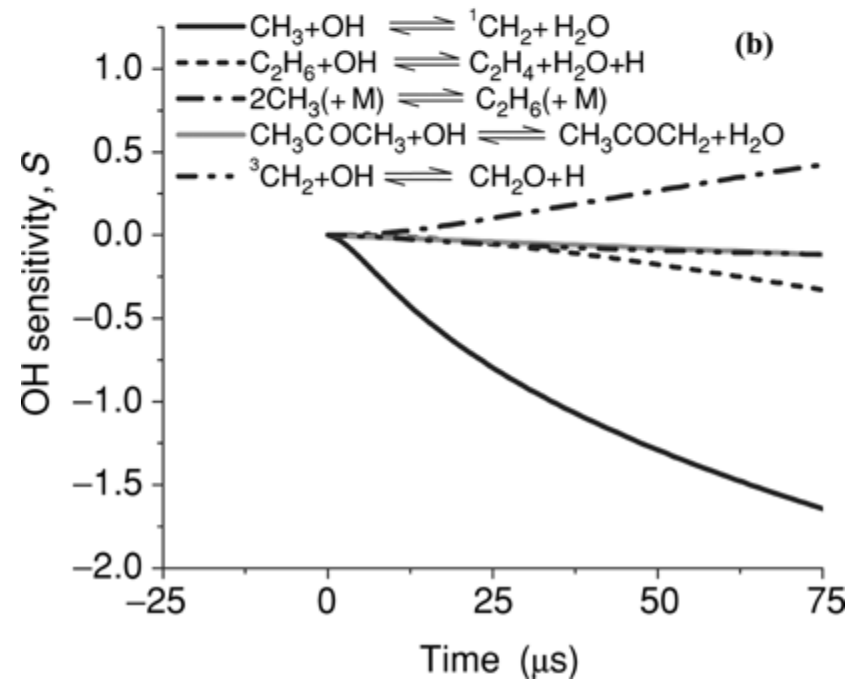
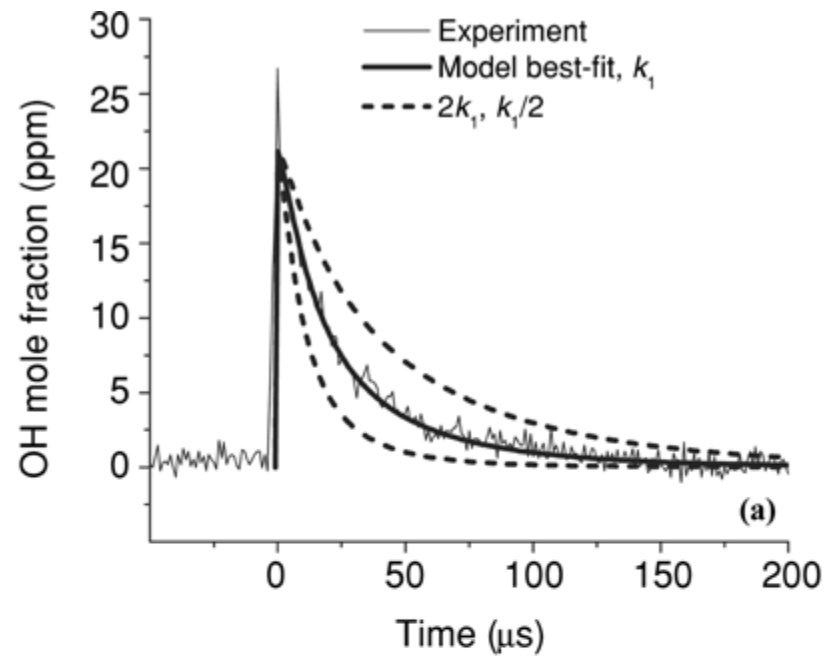


Shock tube: Hanson lab at Stanford



Shock tubes

- Compressive heating of reaction mixture
- Radicals generally formed from thermal dissociation of precursor
- Single shot, so no signal averaging, but impressive optimisation of signal
- Generally need to assess secondary reactions and use numerical chemical model with sensitivity analysis to show viability of measurements.
- Example: Measurement of $\text{CH}_3 + \text{OH}$ by the Hanson group



OH + HCHO, 934 K to 1670 K, 1.6 atm
Int J Chem Kinet 37: 98-109, 2005

- Behind reflected shock waves. OH radicals shock-heating tert-butyl hydroperoxide
- OH concentration time-histories were inferred from laser absorption using the R1(5) line of the OH A-X (0, 0) band near 306.7 nm.
- Other reactions contribute to the OH time profile, especially $\text{CH}_3 + \text{OH}$.
- Rate coefficient determined by fitting to detailed model (GRI-Mech - see Wednesday), with addition of acetone chemistry, deriving from dissociation of OH precursor (t-butylhydroperoxide). Detailed uncertainty analysis

Determination of k and uncertainty analysis

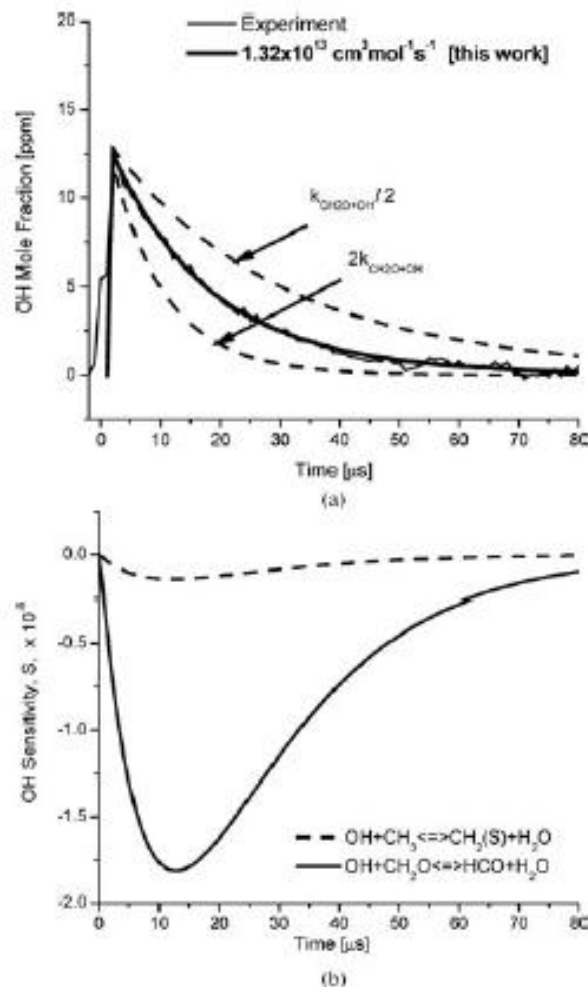


Figure 2 (a) OH concentration time history. 13.25 ppm TBHP, 80 ppm $(\text{CH}_2\text{O})_3$, Ar; initial reflected shock conditions: 1229 K, 1.64 atm. (b) Sensitivity analysis. 13.25 ppm TBHP, 80 ppm $(\text{CH}_2\text{O})_3$, Ar; initial reflected shock conditions: 1229 K, 1.64 atm. $S = (dX_{\text{OH}}/dk_i)(k_i)$, where k_i is the rate constant for reaction i .

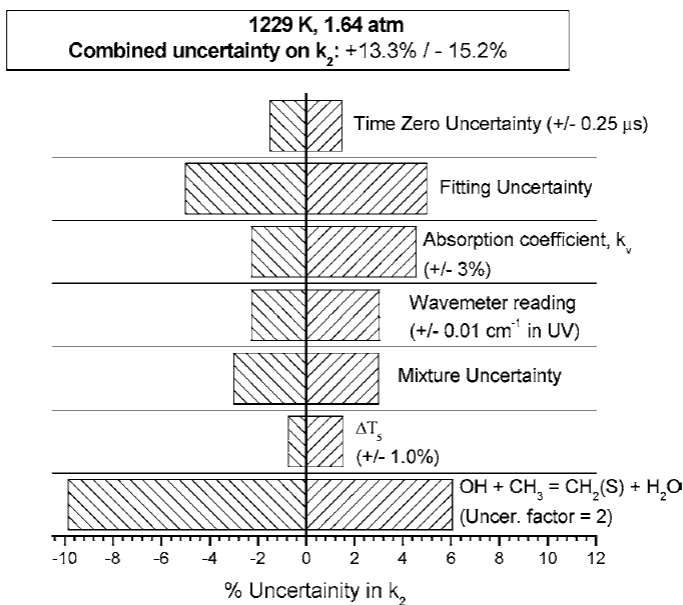


Figure 3 Uncertainty analysis for rate coefficient of $\text{CH}_2\text{O} + \text{OH} = \text{HCO} + \text{H}_2\text{O}$. Initial reflected shock conditions: 1229 K, 1.64 atm; individual error sources were applied separately and their effect on the rate of reaction (2) was determined. Uncertainties were combined to yield an overall uncertainty estimate for k_2 .

Arrhenius plot for OH + HCHO

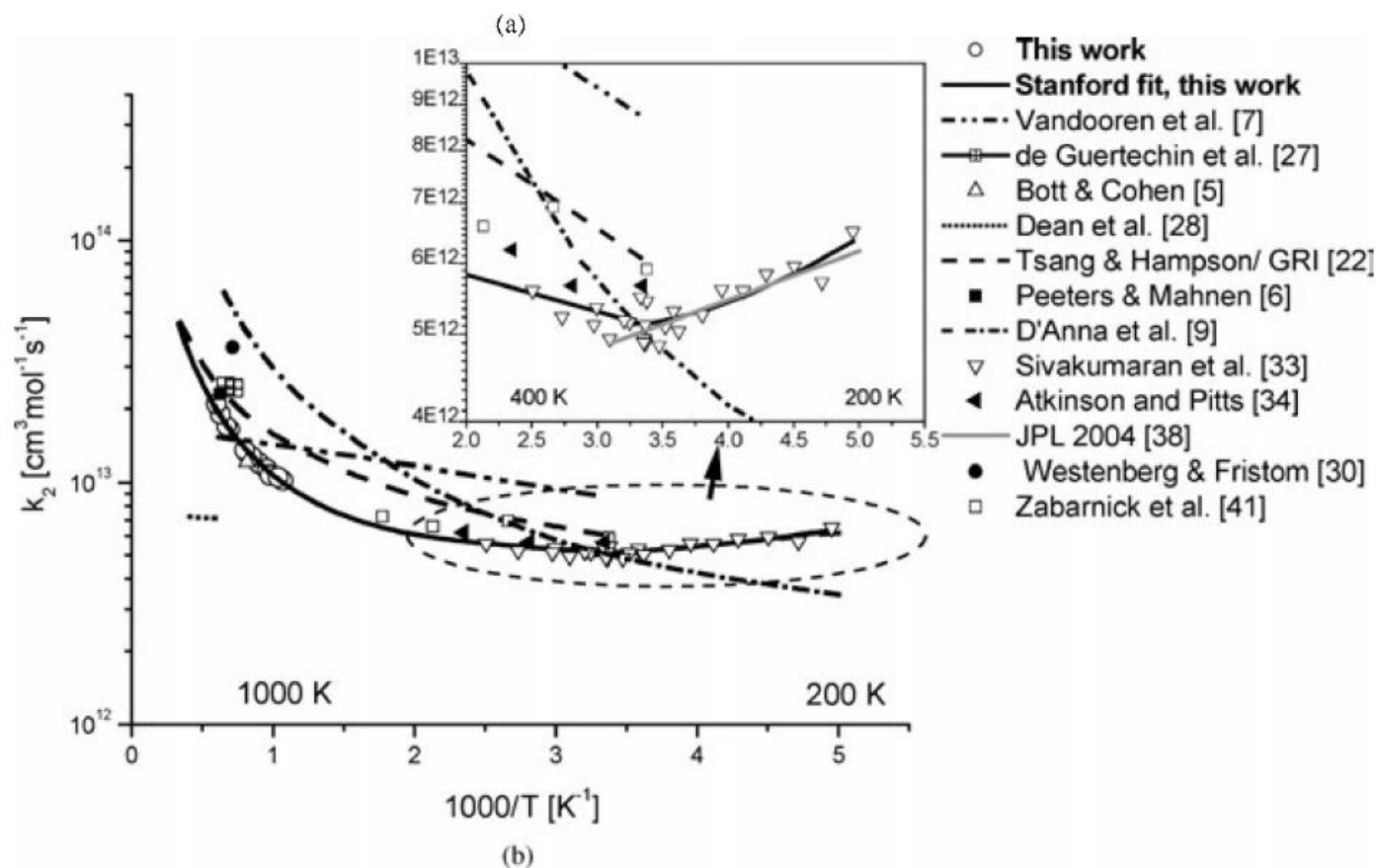


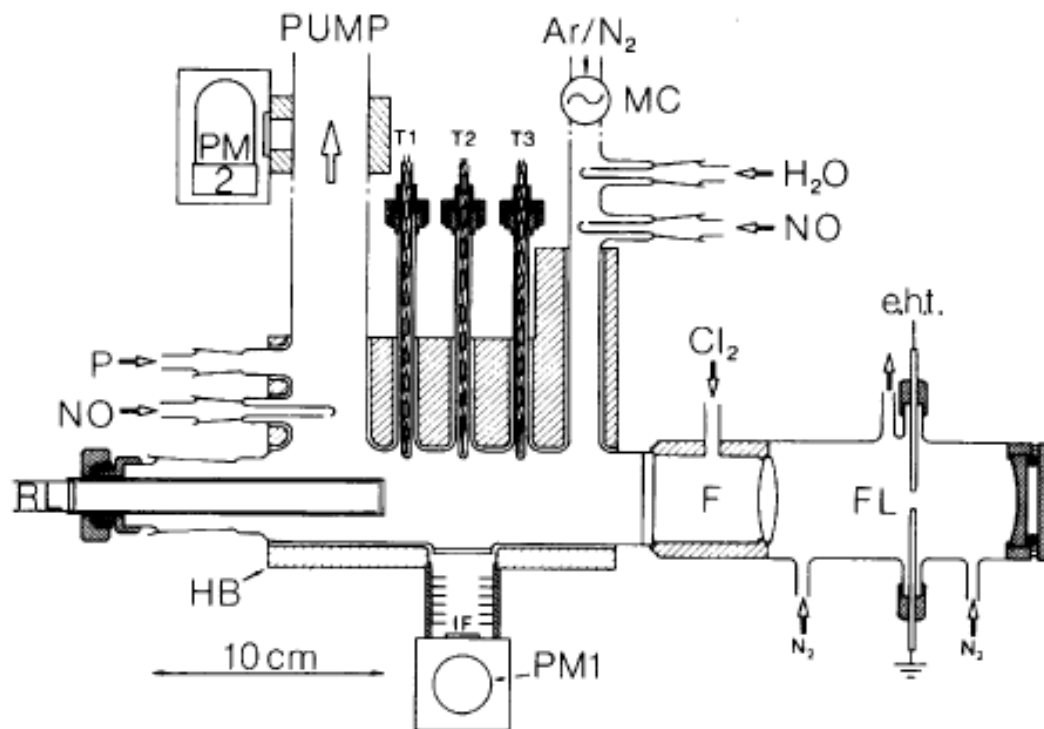
Figure 7 (a) Arrhenius plot for $\text{CH}_2\text{O} + \text{OH} = \text{HCO} + \text{H}_2\text{O}$ at high temperatures (800–2500 K). (b) Arrhenius plot for $\text{CH}_2\text{O} + \text{OH} = \text{HCO} + \text{H}_2\text{O}$ at all temperatures (200–2500 K) and low (200–500 K) temperatures.

- $k_2 = 7.82 \times 10^7 T^{1.63} \exp(531/T) / \text{cm}^3 \text{mol}^{-1} \text{s}^{-1}$

Flow tubes for elementary reactions and whole
systems

Combined flow tube and pulsed photolysis: $O + OH$

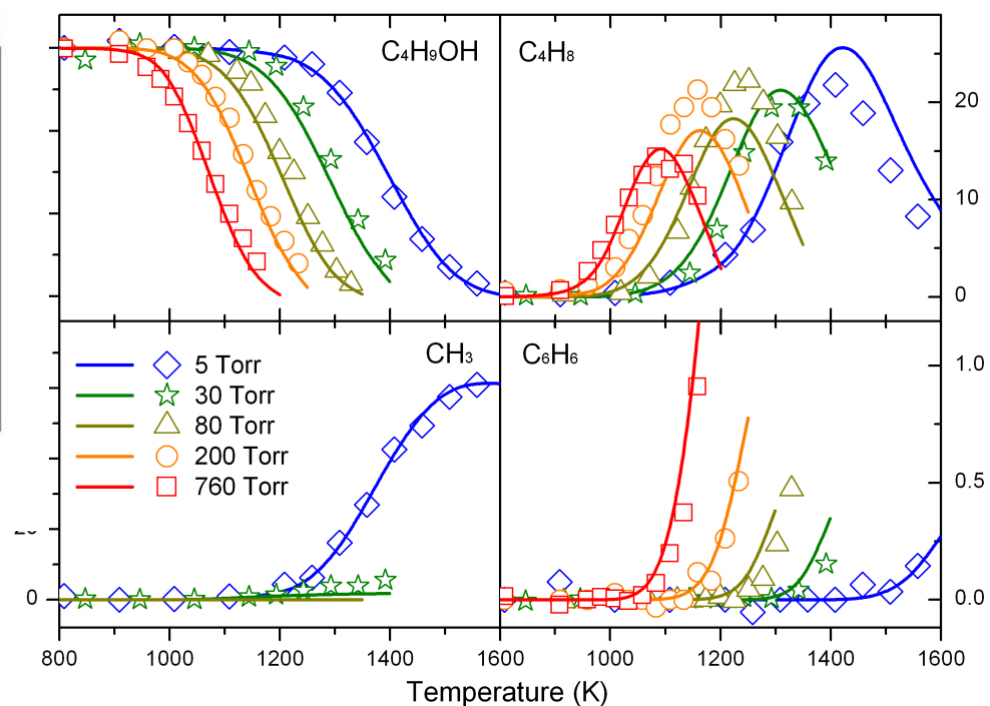
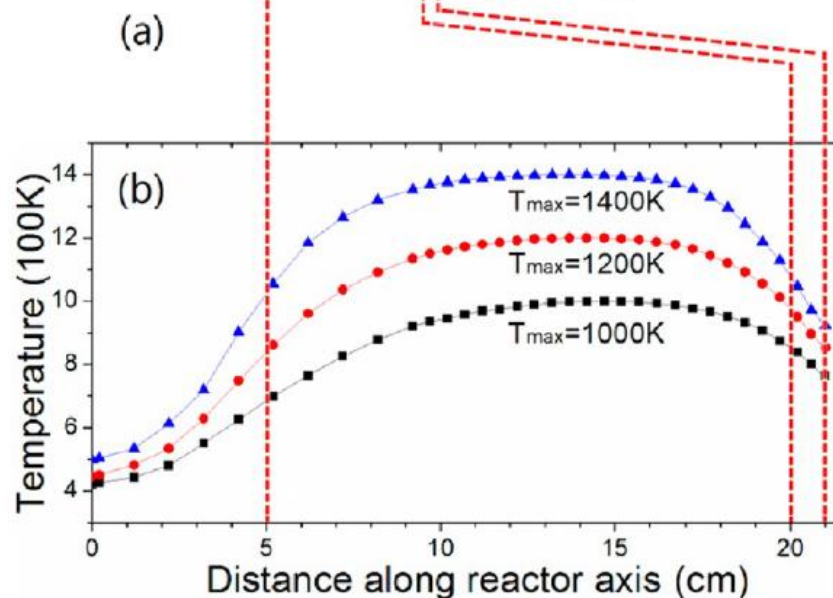
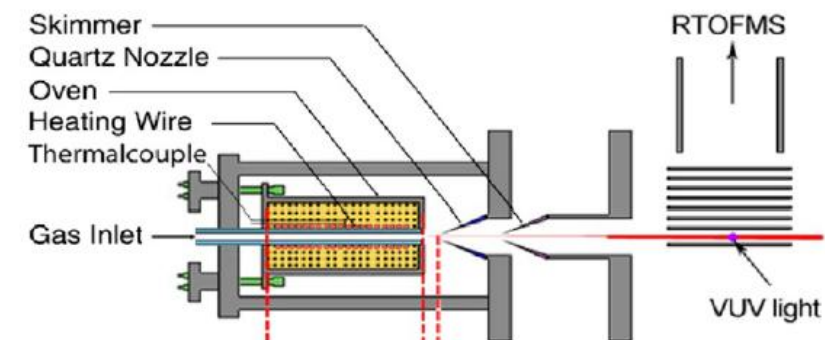
Howard and Smith, J. Chem. Soc Faraday Trans. 2, 1981, 77, 997-1008



- O generated in discharge, OH by pulsed photolysis, with $[O] \gg [OH]$. $[O]$ generated from $N + NO$ and concentration determined by titration.

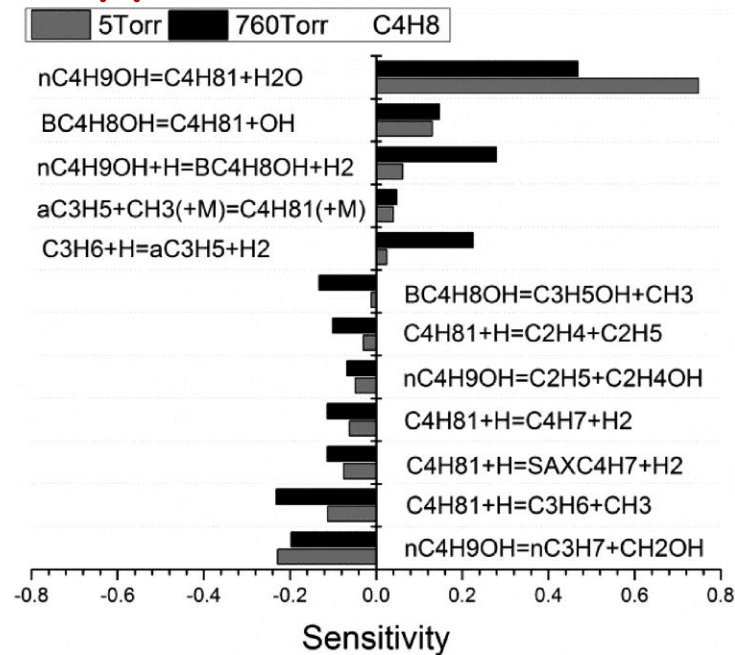
Pyrolysis of butanol using molecular beam sampling from a plug flow reactor

Cai et al. (Energy & Fuels, 26, 5550-5568 (2012))

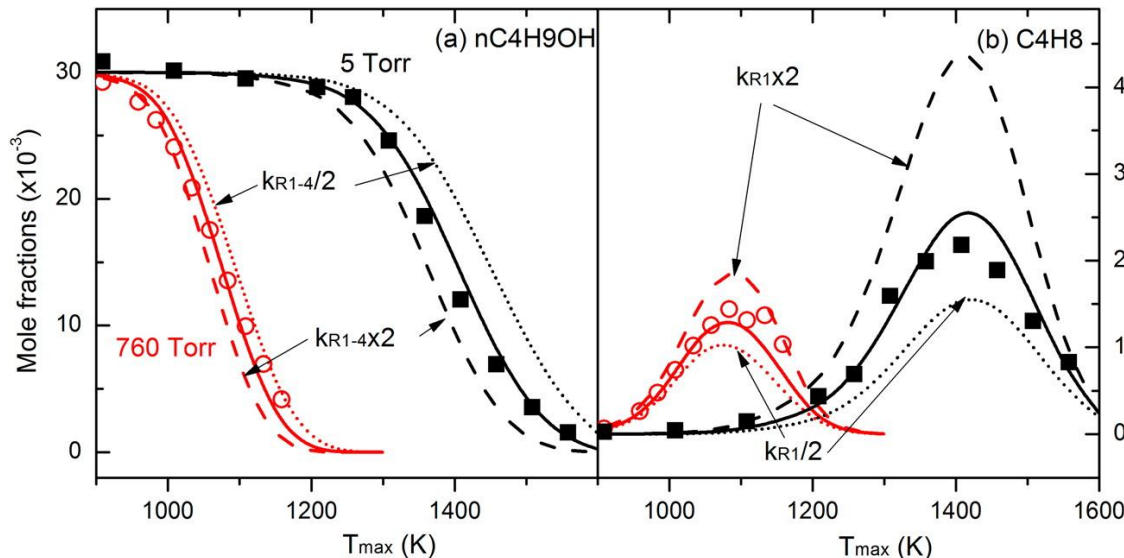


Use of species concentrations in flow reactor to determine rate coefficients: butanol dissociation

Cai et al. (Energy & Fuels, 5550-5568 (2012))



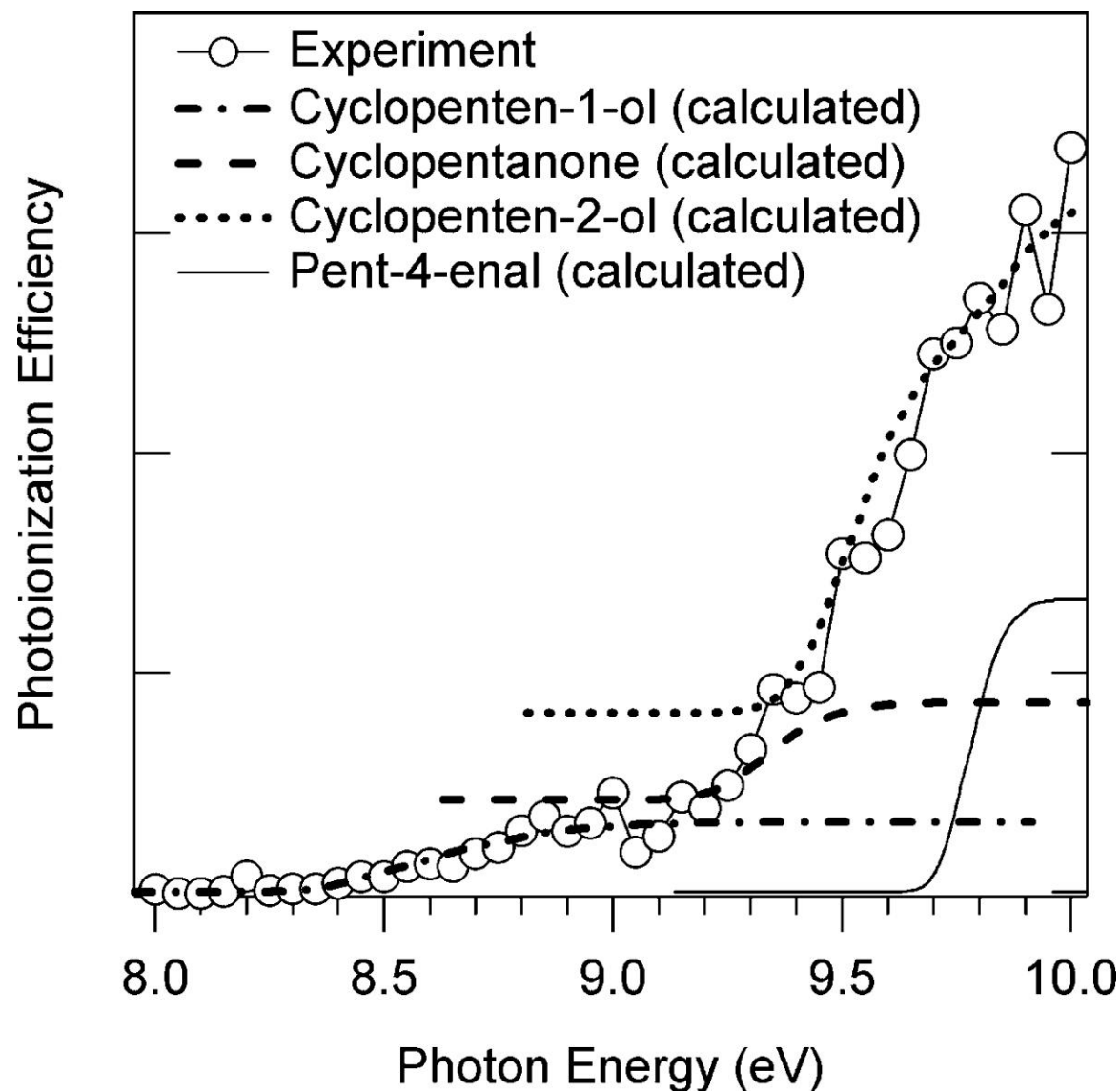
C₄H₈ sensitivity
 $T_{max} = 1450$ K under
 5 Torr (gray) and
 $T_{max} = 1100$ K under
 760 Torr (black)



Experimental mole fraction
 profiles (symbols) and modeling
 results (lines) of nC₄H₉OH
 pyrolysis at 5 and 760 Torr.

Decomposition of photoionization curves in a flow tube study of cyclopentene oxidation

J. Phys. Chem. A 2008, 112, 13444-13451



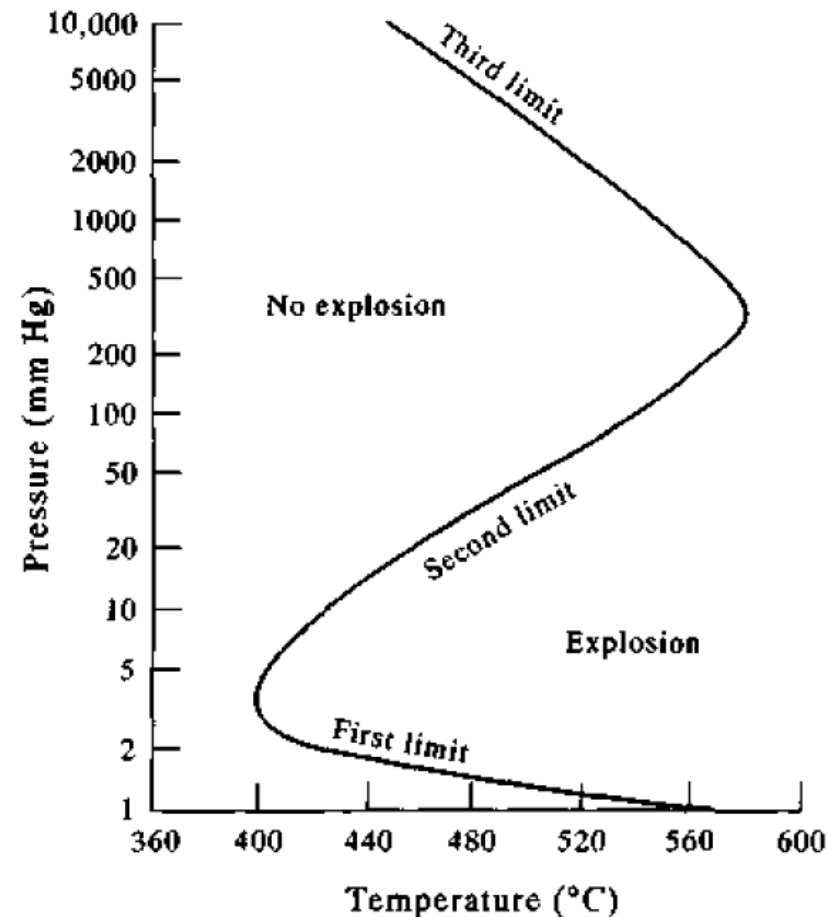
Schematic decomposition of the best fit to the experimental photoionization efficiency spectrum into the substituent calculated photoionization efficiency curves of the three isomers: 1-*c*-C₅H₇OH, *c*-C₅H₈O, and 2-*c*-C₅H₇OH. The isomeric photoionization efficiency curves are scaled by their weighting in the fit to the overall spectrum and vertically displaced for clarity.

Static reactors: Early studies of alkane oxidation kinetics and mechanism by Baldwin, Walker and co-workers

- The techniques rely on end product analysis using gas chromatography. Three techniques were used:
 - Addition of small amounts of alkane, RH, to a slowly reacting $\text{H}_2 + \text{O}_2$ mixture at $\sim 750 \text{ K}$ allowed measurements of, e.g. OH, H, $\text{HO}_2 + \text{RH}$. $\text{H}_2 + \text{O}_2$ provides a well-controlled environment containing the radicals. (JCS Faraday Trans 1., 1975, 71, 736)
 - Oxidation of aldehydes (550 - 800 K). Aldehydes act as a source of alkyl radicals, e.g. $2\text{-C}_3\text{H}_7$ from $2\text{-C}_3\text{H}_7\text{CHO}$ (JCS Faraday Trans 2., 1987, 83, 1509)
 - Decomposition of tetramethylbutane (TMB) in the presence of O_2 . System acts as a source of HO_2 . (JCS Faraday Trans 1., 1986, 82, 89)

Interaction of elementary reactions in $\text{H}_2 + \text{O}_2$

- There are three ignition (explosion) limits. In each case, there is a competition between a termination reaction (removing radicals, decelerating the rate) and a branching reaction (accelerating the rate)
- First limit - competition between termination at the wall e.g. $\text{H} \rightarrow \text{wall}$ (rate \uparrow as pressure \downarrow) and $\text{H} + \text{O}_2 \rightarrow \text{OH} + \text{O}$.
- Second limit - competition between $\text{H} + \text{O}_2 + \text{M} \rightarrow \text{HO}_2 + \text{M}$ (rate \uparrow as pressure \uparrow) and $\text{H} + \text{O}_2 \rightarrow \text{OH} + \text{O}$. HO_2 is an unreactive radical and reacts mainly by $\text{HO}_2 + \text{HO}_2 + \text{M} \rightarrow \text{H}_2\text{O}_2 + \text{M}$.
- Third limit - H_2O_2 dissociates generating OH radicals ($\text{H}_2\text{O}_2 + \text{M} \rightarrow 2\text{OH}$) and propagation and branching recommence



An analysis of the explosion limits of hydrogen-oxygen mixtures

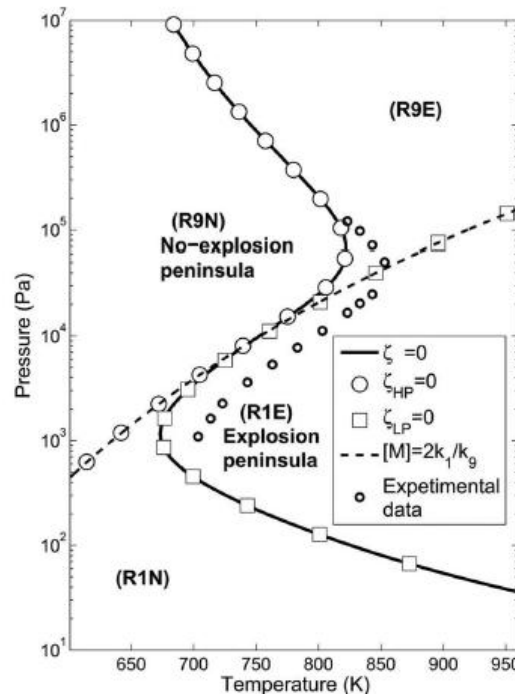
Xianming Wang (王贤明)¹ and Chung K. Law^{1,2,a)}

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(Received 26 December 2012; accepted 12 March 2013; published online 4 April 2013)

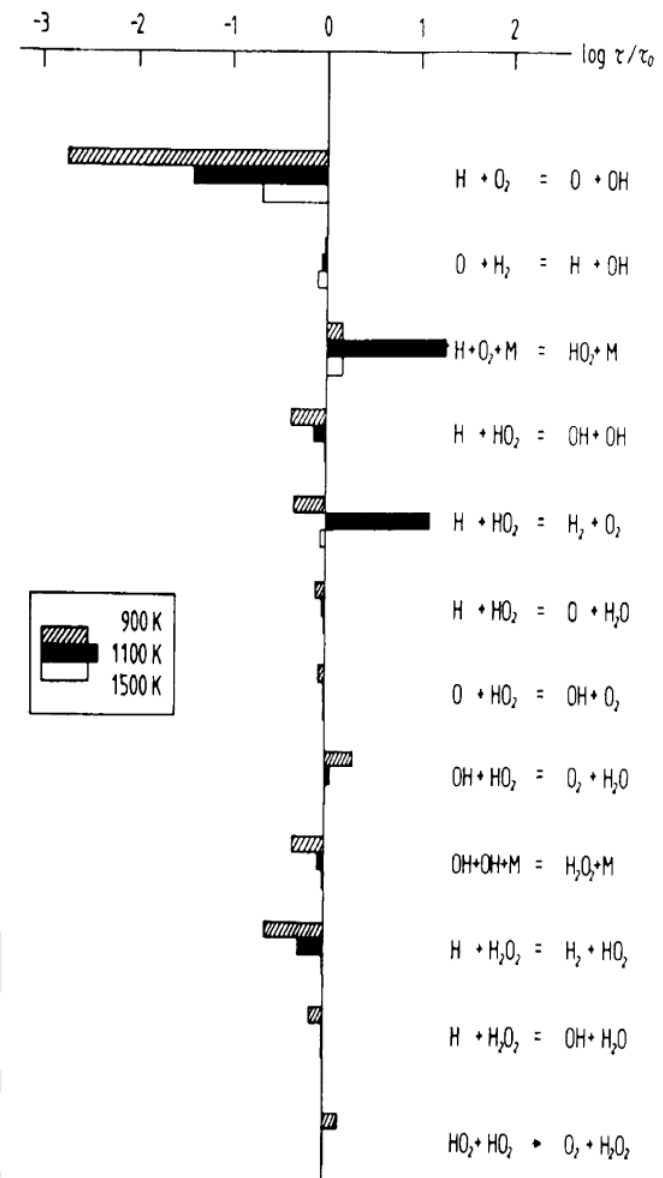
In this study, the essential factors governing the Z-shaped explosion limits of hydrogen-oxygen mixtures are studied using eigenvalue analysis. In particular, it is demonstrated that the wall destruction of H and HO₂ is essential for the occurrence of the first and third limits, while that of O, OH, and H₂O₂ play secondary, quantitative roles for such limits. By performing quasi-steady-state analysis, an approximate, cubic equation for the explosion limits is obtained, from which explicit expressions governing the various explosion limits including the state of the loss of non-monotonicity are derived and discussed. © 2013 American Institute of Physics. [<http://dx.doi.org/10.1063/1.4798459>]

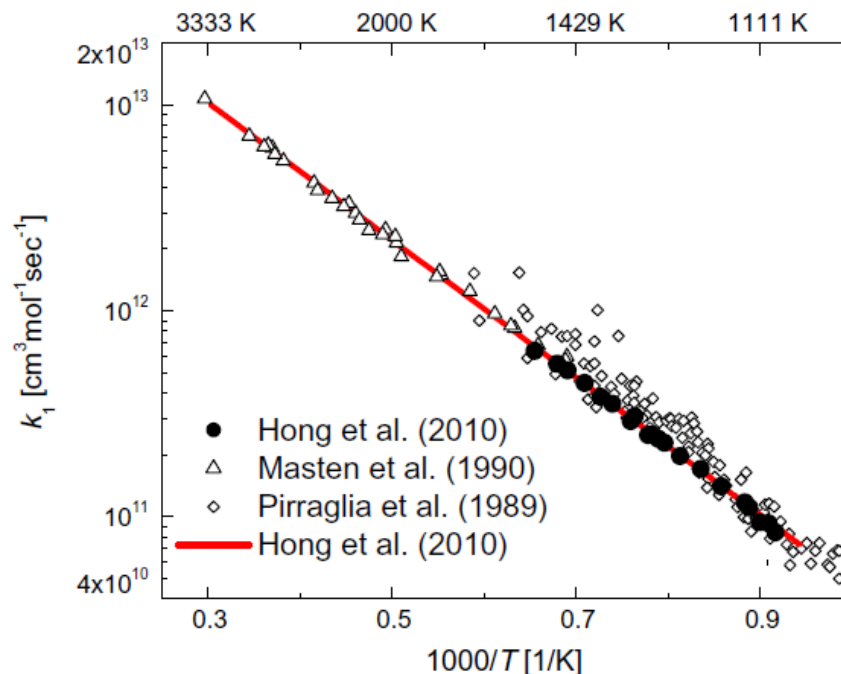


A recent paper discussing the explosion limits for H₂/O₂

Hydrogen oxygen system

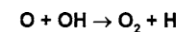
- Review by Miller et al. (Proc Comb. Inst., 2005, 30, 45-88)
- Slide shows sensitivities for ignition delay times (8% H₂, 2% O₂, 90% Ar, 1 bar).
- Note the significance of the H + O₂ branching step, the termination step H + O₂ + M and the H + HO₂ steps



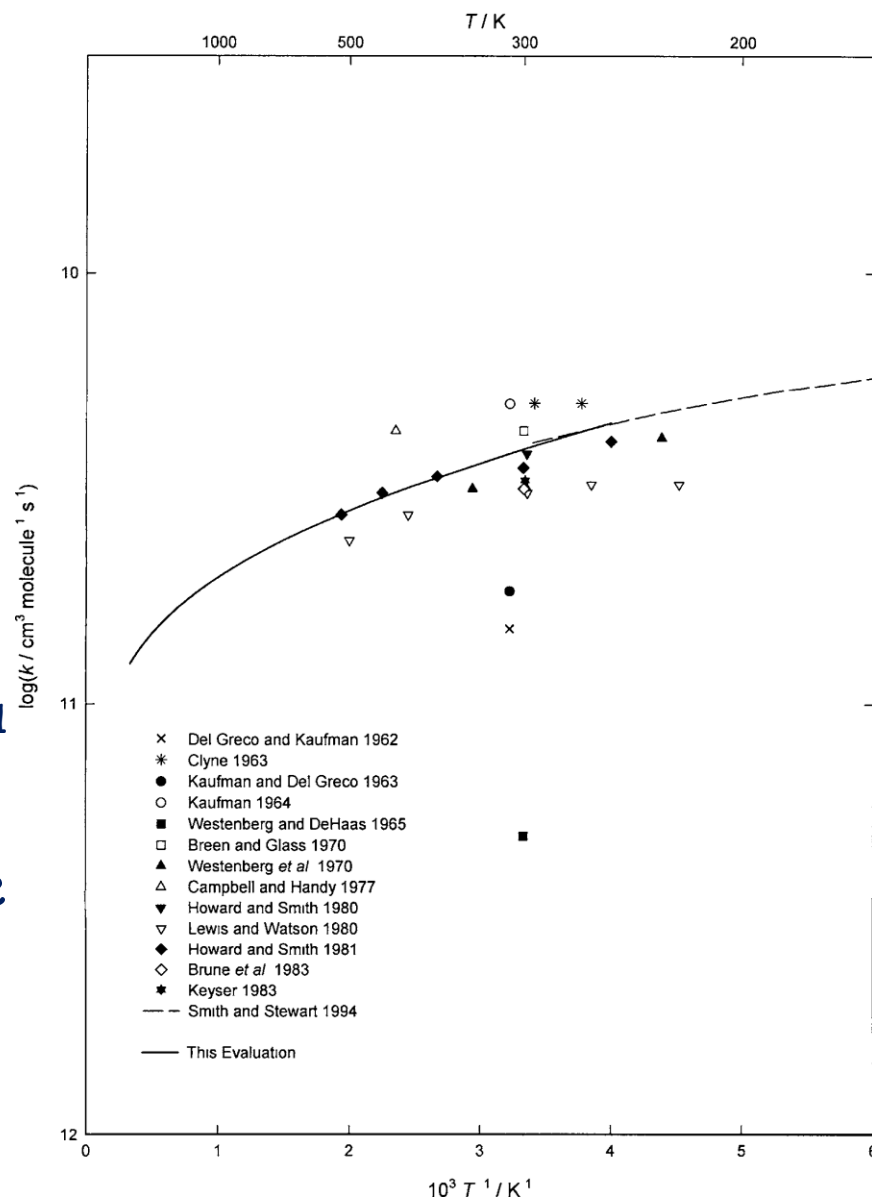


- From Hong et al., shock tube measurements. Comb Flame 2011, 158, 633, $k = 1.7 \times 10^{-10} \exp(-7670/T)$ (1100 - 3370 K). Uncertainty $\pm 10\%$.
- See Burke et al. Int J Chem Kinet, 2012, 44, 444, who support the rate coefficient
- See discussions on evaluation in later lectures.

Reverse reaction: $O + OH \rightarrow H + O_2$



- Studied 150 - 500 K, mainly by discharge flow / laser flash photolysis.
- Not of great importance in combustion, but provides additional information on reverse reaction through thermodynamics
- $k = 2.00 \times 10^{-10} T^{-0.352} \exp(113/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ over the range 250-3000 K.
- $\Delta \log k = \pm 0.2$ over the range 250-3000 K.



Second branching step

$$\text{O} + \text{H}_2 \rightarrow \text{OH} + \text{H}$$

- Sutherland et al. (21st Symp(Int) Comb, 1986, 929). Used flash photolysis, monitoring O by resonance fluorescence, and shock tube, generating O by flash photolysis of NO and monitoring by ARAS. ()
- Davidson and Hanson (Comb and Flame, 1990, 82, 445) used shock tube, generating O by laser flash photolysis of NO and by pyrolysis of N₂O. O monitored by ARAS

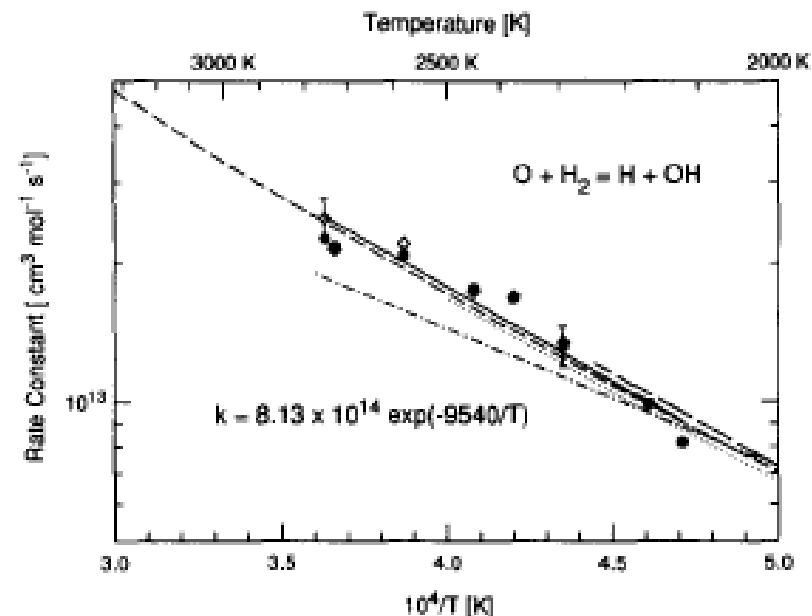
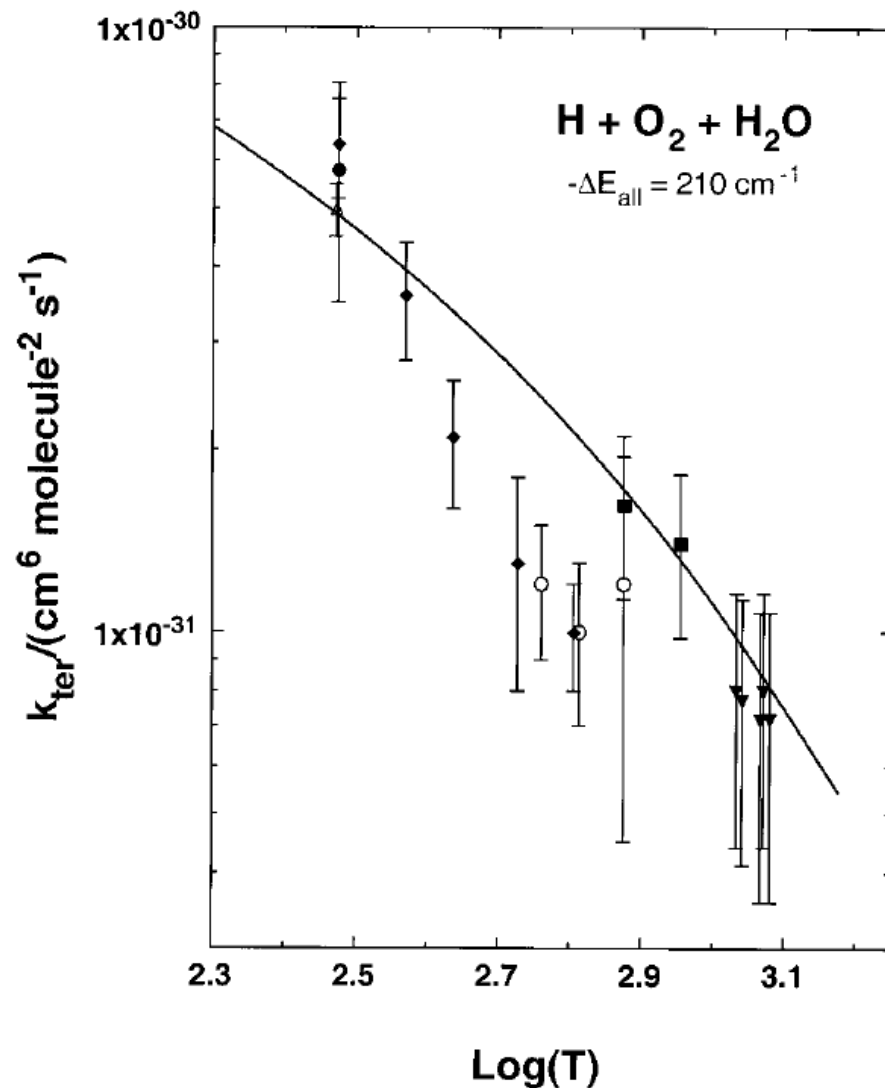
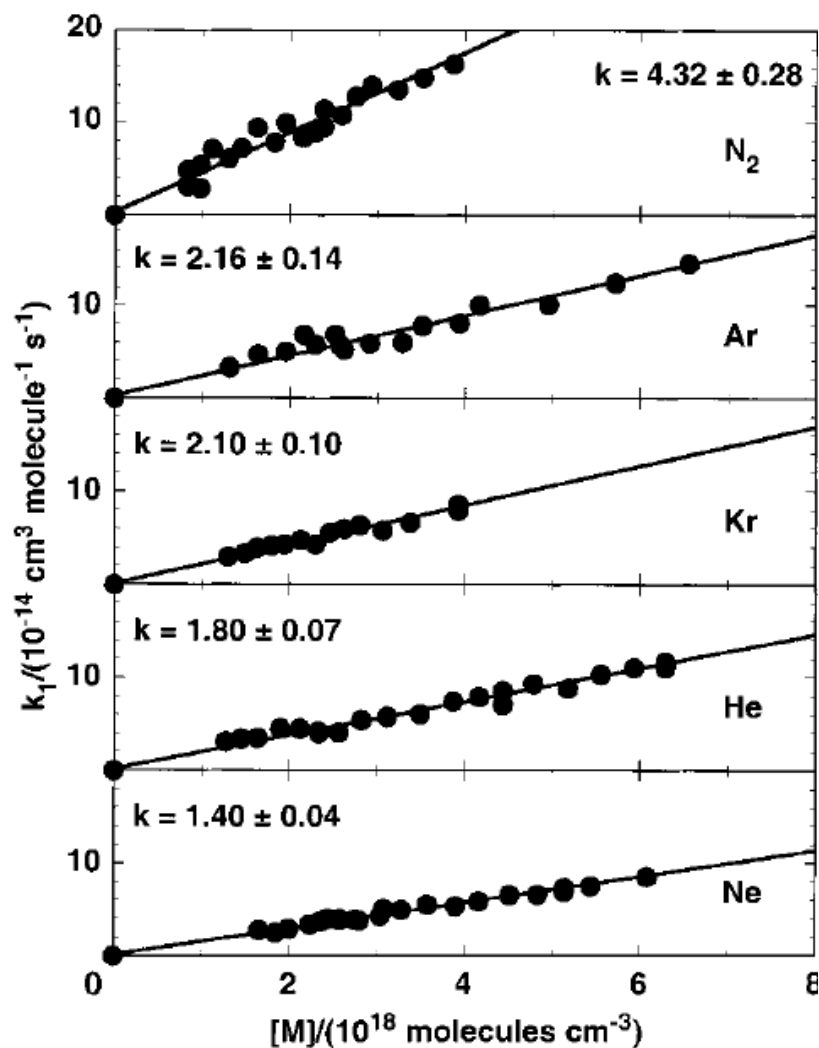


Fig. 2. Arrhenius diagram: $\text{O} + \text{H}_2 \rightarrow \text{OH} + \text{H}$. Filled circles—data derived from photolysis method. Open diamonds—data derived from pyrolysis method. Error bars represent $\pm 10\%$. Solid line—best fit to present data. Dotted line—Sutherland et al. [8]. Dashed line—Nataranjan and Roth [9]. Dot-dashed line—Pamidimukkala and Skinner [10]. Long-dashed line—Shin et al. [11].

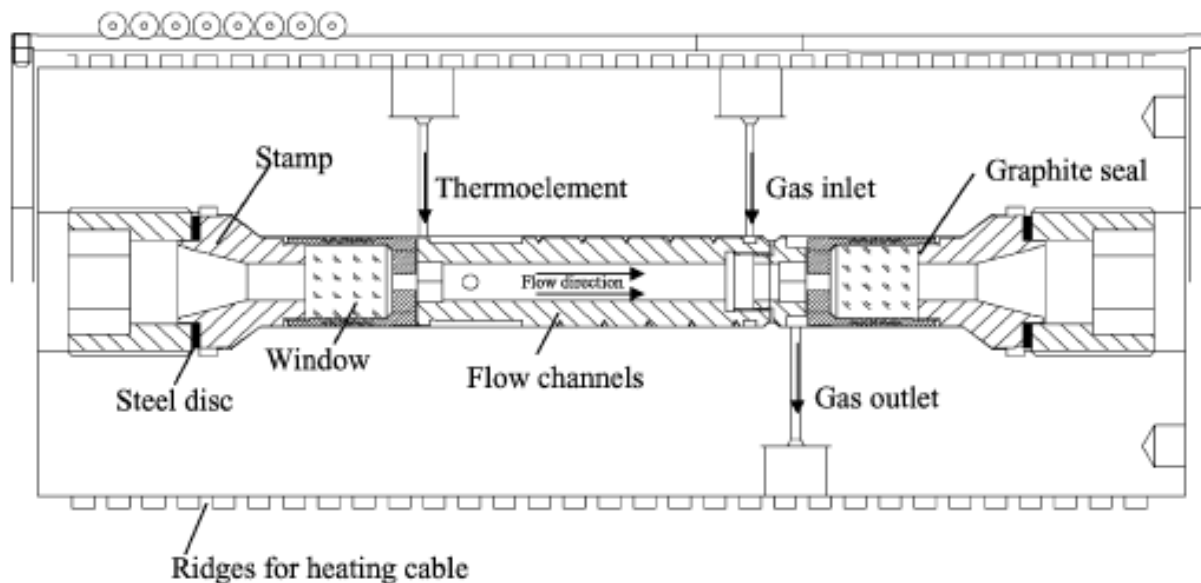


- Termination step at lower T, converting reactive H into less reactive HO₂. Acts as a route to branching through formation of H₂O₂ through HO₂ + HO₂ (and HO₂ + RH in hydrocarbon combustion)
- Reaction is at the third order limit except at higher pressures.
- Michael et al. J. Phys. Chem. A 2002, 106, 5297-5313 used flash photolysis at room T for a wide range of third bodies, and a shock tube at higher T for Ar, O₂ and N₂. Showed that H₂O is an unusually effective third body.
- Detailed analysis of collision frequencies and energy transfer parameters.



Units of k : $10^{-32} \text{ cm}^6 \text{ molecule}^{-2} \text{ s}^{-1}$

High pressure pulsed photolysis / flow reactor
Fernandes et al. Phys. Chem. Chem. Phys., 2008, 10,
4313-4321



- $\text{H} + \text{O}_2 + \text{M} \rightarrow \text{HO}_2 + \text{M}$, 300 - 900 K, 1.5 - 950 bar
- H from photolysis NH_3 at 193 nm
- HO_2 detected by absorption spectroscopy at 230 nm.
- At these higher pressures, the reaction moves into the fall-off region

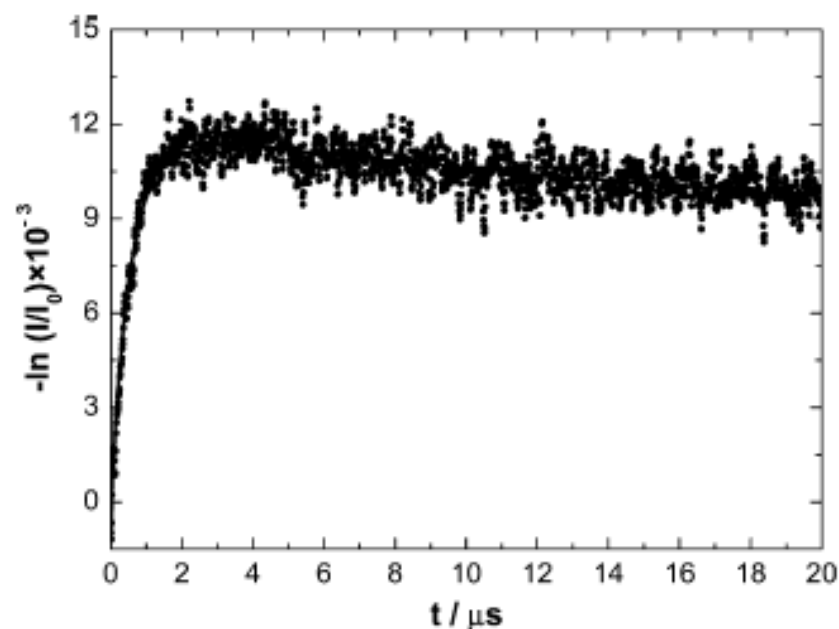


Fig. 2 Absorption-time profile of HO_2 ($\lambda = 230$ nm, $T = 600$ K, $p = 300$ bar, $\text{M} = \text{N}_2$).

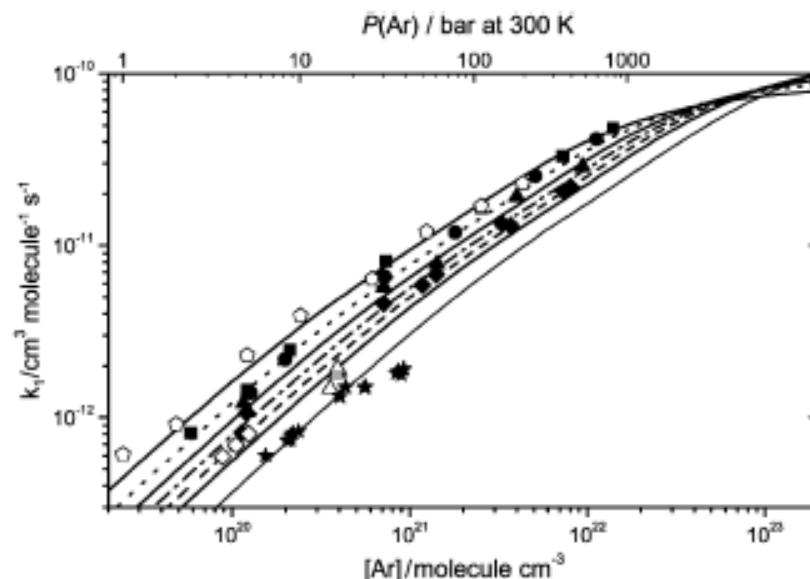


Fig. 5 Falloff curves for the recombination $\text{H} + \text{O}_2 (+\text{Ar}) \rightarrow \text{HO}_2$ ($+\text{Ar}$) (representative upper pressure scale for 300 K; $T/\text{K} = 300$ (■), 400 (●), 500 (▲), and 600 (◆) from this work; 300 (○, ref. 19), 820 (◇, ref. 20), 1200 (★, ref. 22), and 1325 (△, ref. 21); the fitted curves at left from top to bottom are for $T/\text{K} = 300, 400, 500, 600, 700, 820$, and 1200, resp.).



- Data for different third bodies and temperatures can be rationalised and placed on the same plot using reduced falloff curves. Requires calculation of high pressure limiting rate coefficient (that isn't accessible to experiment for this reaction.)

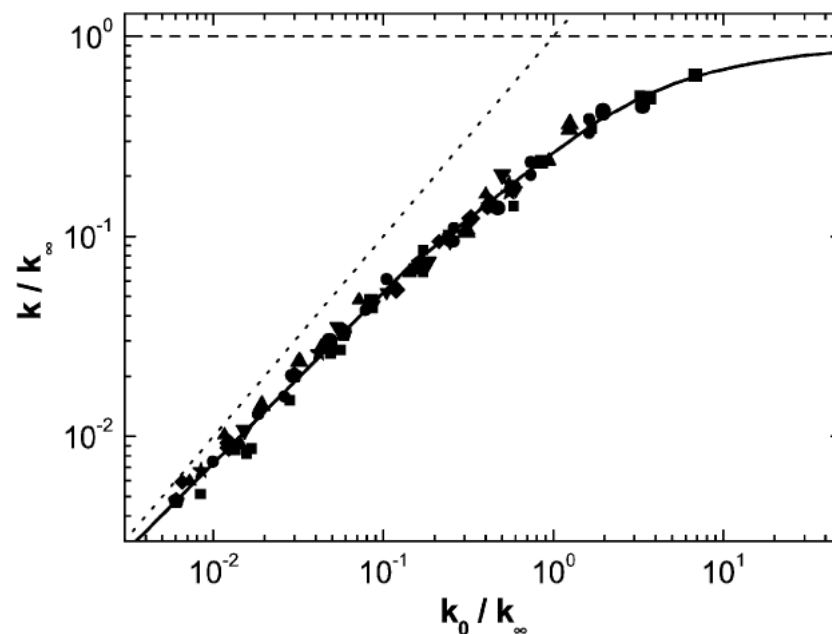
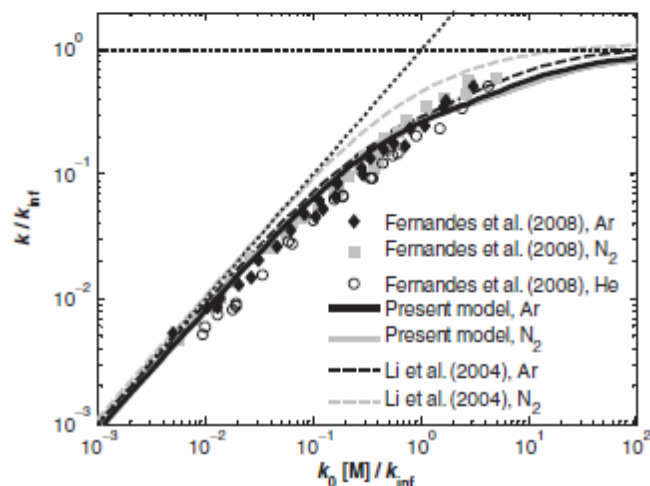
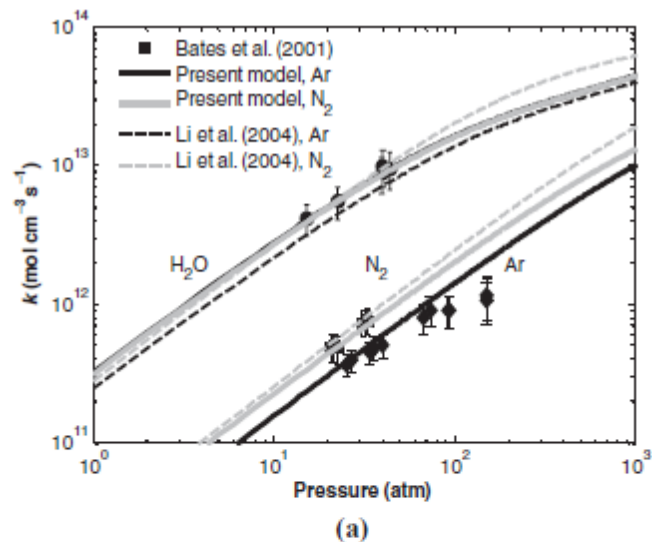


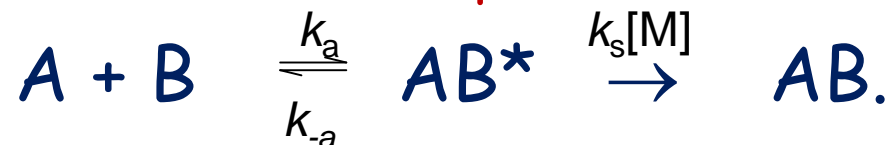
Fig. 7 Doubly reduced falloff curves for the recombination $\text{H} + \text{O}_2 (+\text{M}) \rightarrow \text{HO}_2 (+\text{M})$ in the bath gases $\text{M} = \text{He}, \text{Ar}, \text{and } \text{N}_2$ (experimental points from this work from Tables 1–3; $T/\text{K} = 300$ (■), 400 (●), 500 (▲), 600 (▼), 700 (◆), 800 (★), and 900 (◆), see text).

Most recent evaluation: Burke et al, Int J Chem Kinet 2012, 44, 444



- See paper for detailed discussion of Troe parameters (next slide), uncertainties etc.

Recall earlier slide: Pressure dependent association reactions



$$\text{As } [M] \rightarrow \infty, k \rightarrow k_a = k^\infty$$

$$\text{As } [M] \rightarrow 0, k \rightarrow \frac{k_a k_s [M]}{k_{-a}} = k_0 [M]$$

$$k = \frac{k_a k_s [M]}{k_{-a} + k_s [M]}$$

$$k = \frac{k_0 [M] k^\infty}{k^\infty + k_0 [M]}$$

Similar treatment
for dissociation
reactions

- This is the Lindemann-Hinshelwood model of pressure dependent unimolecular reactions.
- The treatment is an approximation because (i) k_{-a} depends on the energy of AB^* (ii) deactivation of AB^* takes place in a number of steps.
- These have the effect of *broadening* the fall-off curve (k vs $[M]$). These effects have been incorporated in a fitting procedure developed by Troe that is widely used in parameterising rate coefficients for use in combustion modelling

Troe Fitting

Need to represent $k(T,P)$ for Global Models

Standard is Troe Fitting

$$k(T,p) = \frac{k_0[M]k^\infty}{k^\infty + k_0[M]} F \quad \log_{10} F = \frac{\log_{10} F_{cent}}{1 + \left[\frac{\log_{10}(p^*) + c}{N - d(\log_{10}(p^*) + c)} \right]^2}$$
$$p^* = k_0[M]/k^\infty \quad d = 0.14$$

$$c = -0.4 - 0.67 \log_{10} F_{cent} \quad N = 0.75 - 1.27 \log_{10} F_{cent}$$

Fit k_0 & k^∞ to modified Arrhenius $k_0 = A_0 T^{n_0} \exp(-E_0/T)$

Fit F_{cent} to:

$$F_{cent} = (1-a) \exp(-T/T^{***}) + a \exp(-T/T^*) + \exp(-T^{**}/T)$$



- < 800 K. Flash photolysis, absorption spectroscopy
- Open circles: shock tube, absorption spectroscopy (Kappel et al, Phys Chem Chem Phys, 2002, 4, 4392)
- Reference 5: Hippler et al. J Chem Phys 1990, 93, 1755
- Significant disagreement > 1000 K
- Burke et al. 'Difficult to discern which, if any, (of the high T) determinations is reliable.' More measurements needed under combustion conditions.

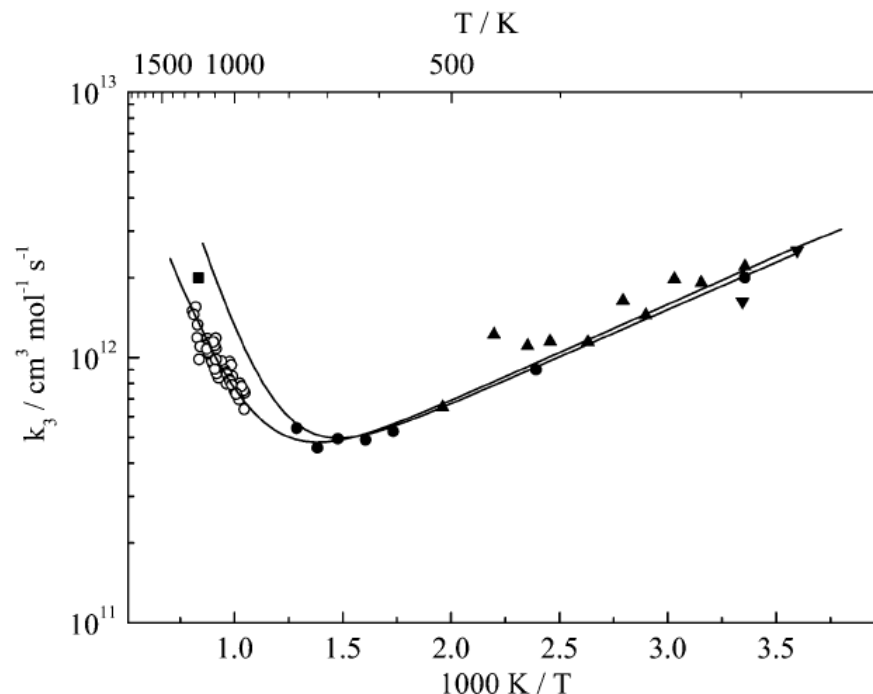


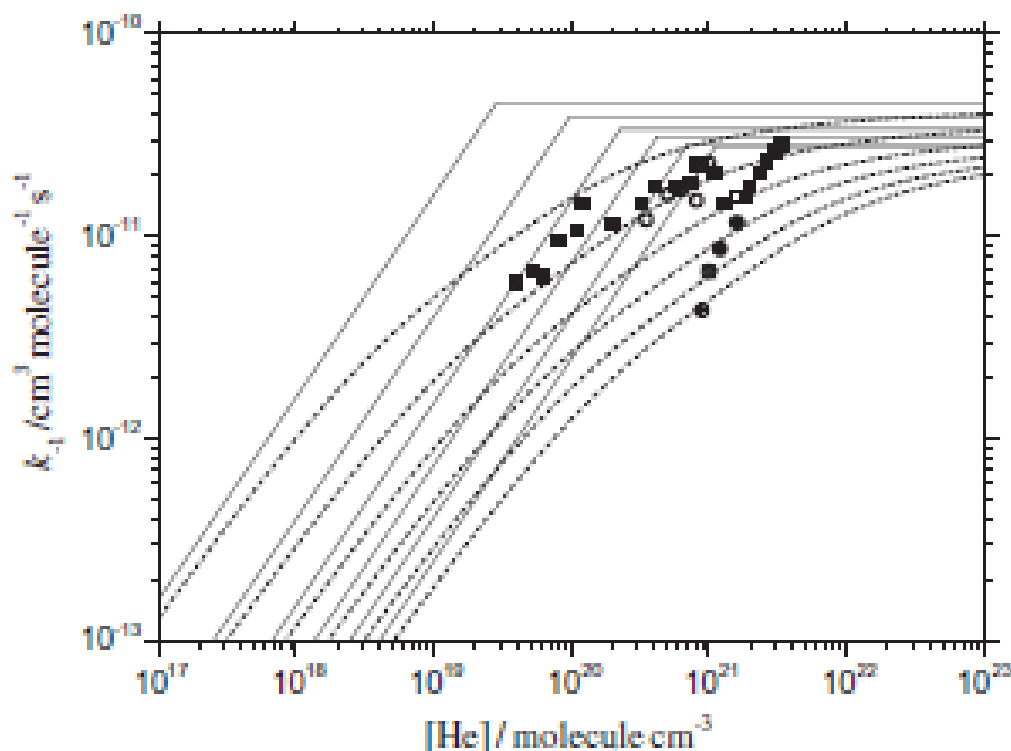
Fig. 10 Rate constants k_3 (■: ref. 2, ▲: ref. 35, ▼: ref. 36, ●: ref. 37, ○ and lower line: this work, upper line: ref. 5).



- Troe, Combustion and Flame 2011, 158, 594-601 The thermal dissociation/recombination reaction of hydrogen peroxide $\text{H}_2\text{O}_2 \rightleftharpoons 2\text{OH}$ Analysis and representation of the temperature and pressure dependence over wide ranges.
- Reaction is far from the high pressure limit. To obtain a representation of $k(T,p)$, Troe used the statistical adiabatic channel model to calculate k_∞ , using an ab initio surface (Phys. Chem. Chem. Phys. 10 (2008) 3915; J. Chem. Phys. 111 (1999) 2565).
- An important aspect of this work was the use of thermodynamics to relate forward and reverse reactions, using the revised enthalpy of formation of OH - see Wednesday lecture on thermodynamics

Association reaction

- Flash photolysis coupled with saturated LIF.
- Use pressure dependence to separate from $O + H_2O$ channel
- Also problems with secondary reactions (see paper)

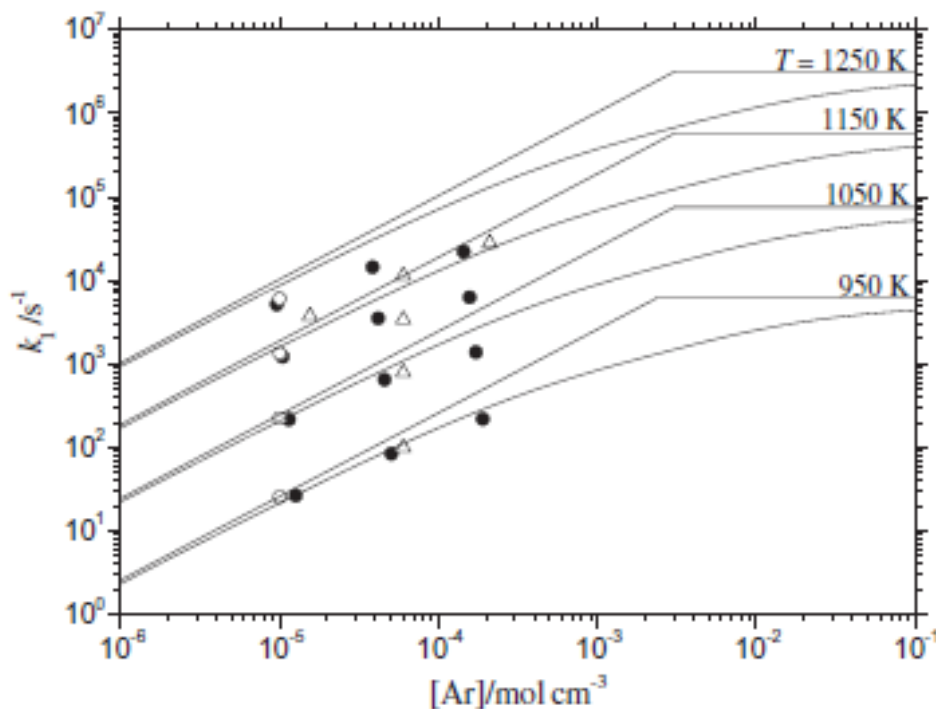


Reaction is second order in radical, so absolute concentration is needed

Fig. 3. Experimental recombination rate coefficients k_{-1} and their modelled falloff representation ($M = \text{He}$, experimental points from Refs. [30,31] at $T/K = 210$ (\circ), 298 (\blacksquare), 406 (\square), 510 (\bullet), 614 (\odot), and 694 (\oplus); full lines = modelled limiting low and high pressure rate coefficients from Section 5 of this work; dashed lines = falloff representation by Eq. (3.3) with $F_c = 0.37$ and $N = 1.32$).

Dissociation reaction

- Flow reactor and static studies at lower T and shock tube measurements above 950 K (see below)

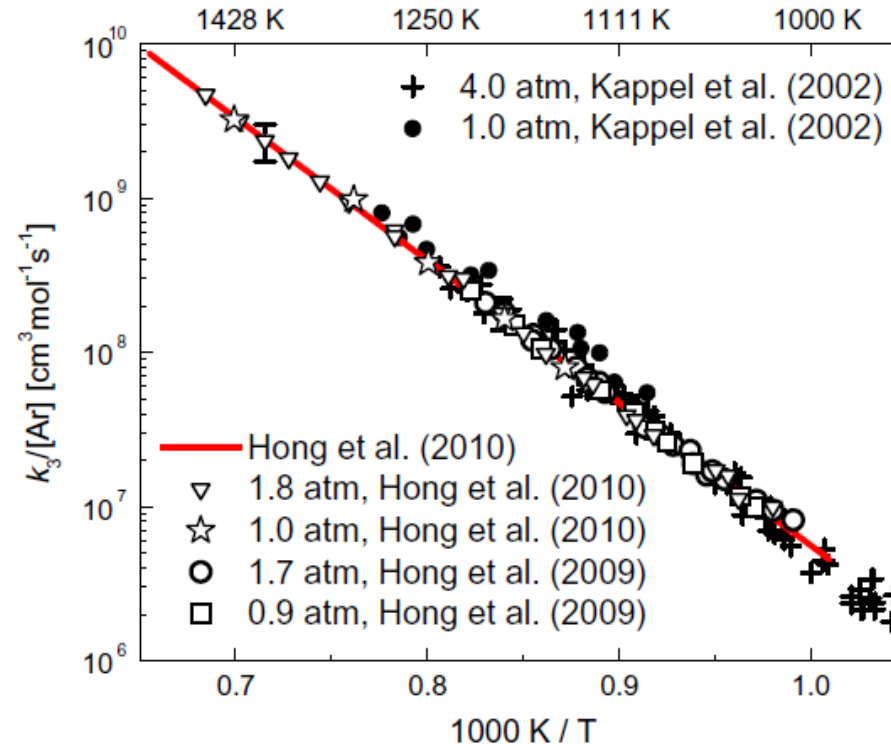


Overall reaction

- Dissociation and association data fitted to Troe expression (see earlier) using theoretical high pressure limit and equilibrium constant

H_2O_2 dissociation

Hong et al. Comb Flame 2011, 158, 633



- Data refer to low pressure limit. Used shock tube with laser absorption detection of H_2O and OH