



Reciprocating Internal Combustion Engines

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Summer School on Combustion
Course Length: 15 hrs

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Short course outline:

Engine fundamentals and performance metrics, computer modeling supported by in-depth understanding of fundamental engine processes and detailed experiments in engine design optimization.

Day 1 (Engine fundamentals)

Part 1: IC Engine Review, 0, 1 and 3-D modeling

Part 2: Turbochargers, Engine Performance Metrics

Day 2 (Combustion Modeling)

Part 3: Chemical Kinetics, HCCI & SI Combustion

Part 4: Heat transfer, NOx and Soot Emissions

Day 3 (Spray Modeling)

Part 5: Atomization, Drop Breakup/Coalescence

Part 6: Drop Drag/Wall Impinge/Vaporization/Sprays

Day 4 (Engine Optimization)

Part 7: Diesel combustion and SI knock modeling

Part 8: Optimization and Low Temperature Combustion

Day 5 (Applications and the Future)

Part 9: Fuels, After-treatment and Controls

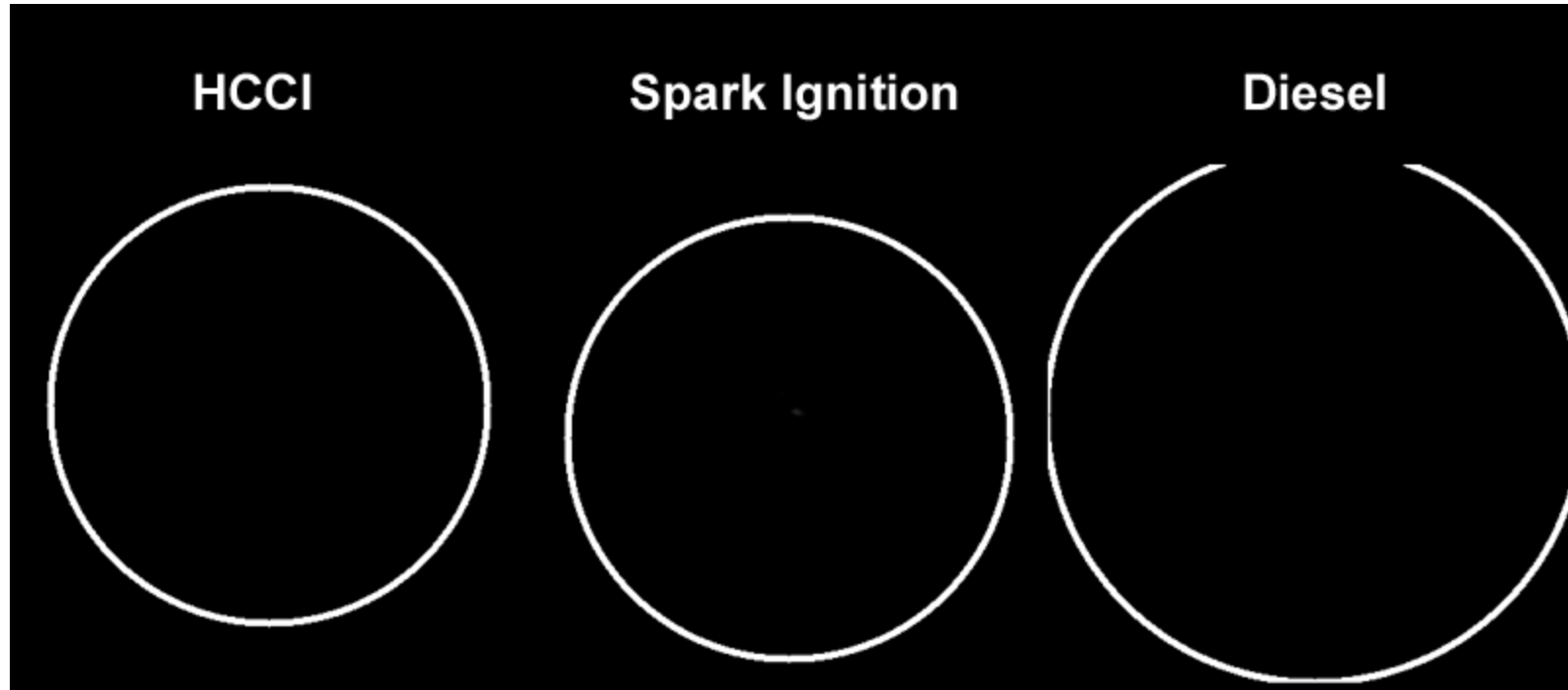
Part 10: Vehicle Applications, Future of IC Engines





Modes of engine combustion

<http://www.erc.wisc.edu/combustion.php>



HCCI uses a hybrid combustion strategy. Premixed fuel and air is inducted, but instead of igniting with a spark as in a SI engine, the high temperature from compression causes the mixture to spontaneously react, like in a diesel engine. Ignition occurs at slightly different times at different locations in the chamber.

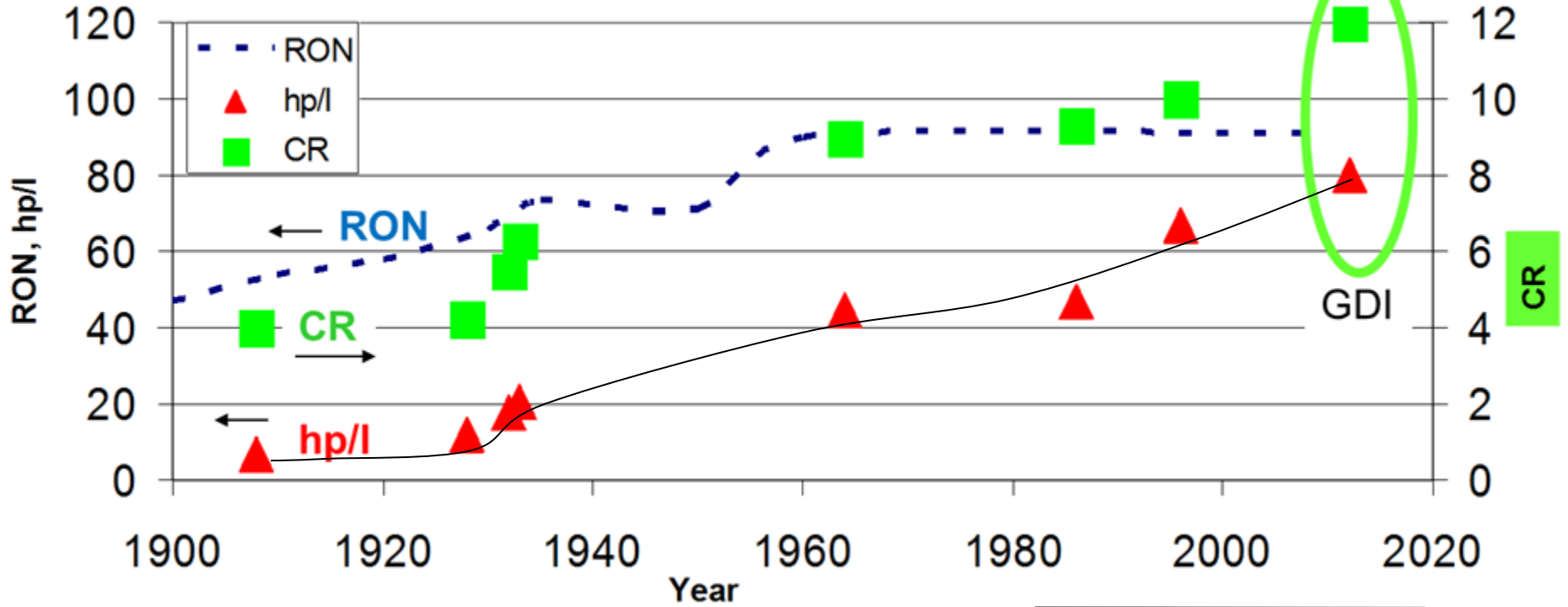
One feature of HCCI combustion is how quickly the fuel is consumed.





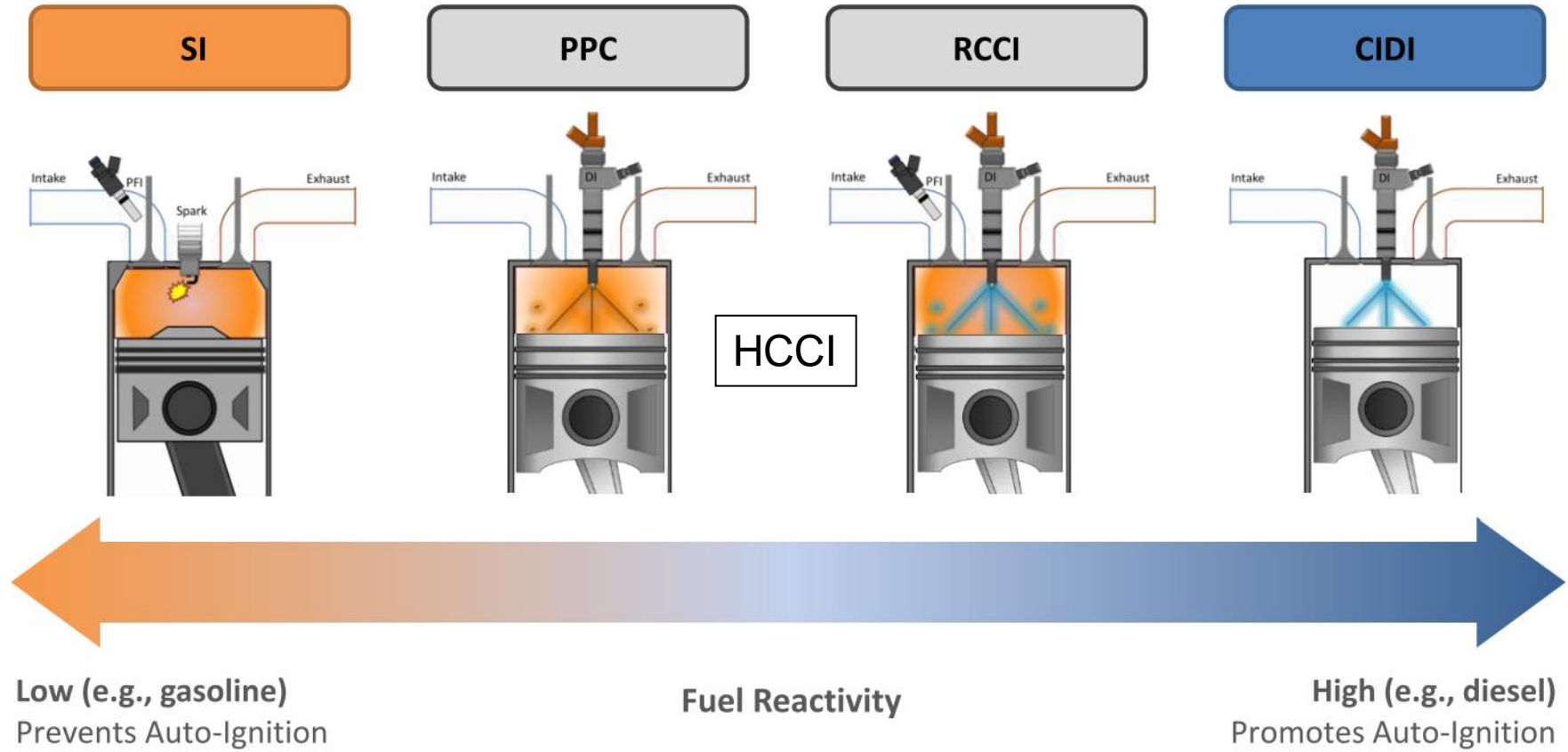
Chemistry: importance of fuels

RON History - Regular Gasoline, USA





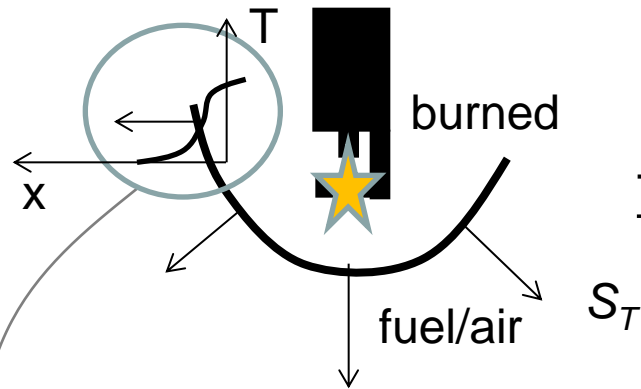
New advanced combustion regimes





Basic combustion concepts – Spark Ignition (SI)

How can SI engines operate with engine speeds from 100 to 20,000 rev/min?



Turbulence!

Kinetic energy, $k \sim V_{piston}^2$

Integral length scale $l_I \sim L_{piston}$

Kinetic energy dissipation rate,
 $\varepsilon \sim V_{piston}^3 / L_{piston}$

Diffusivity, $D \sim k^2 / \varepsilon \sim V_{piston} L_{piston}$

Because turbulent flame speed, S_T , scales with rpm!

Characteristic Time Combustion (CTC) model

Reitz & Bracco, 1983; Abraham, 1985

Species conversion rate (Y_i , species mass fraction, * local equilibrium solution)

$$\frac{dY_i}{dt} = -\frac{Y_i - Y_i^*}{\tau_c} \quad ; \quad \tau_c \sim k/\varepsilon \sim L_{piston} / V_{piston}$$

Mallard-Le Chatelier propagating wave speed:

$$S_T = \sqrt{D \frac{dY_i}{dt}} \sim V_{piston}$$

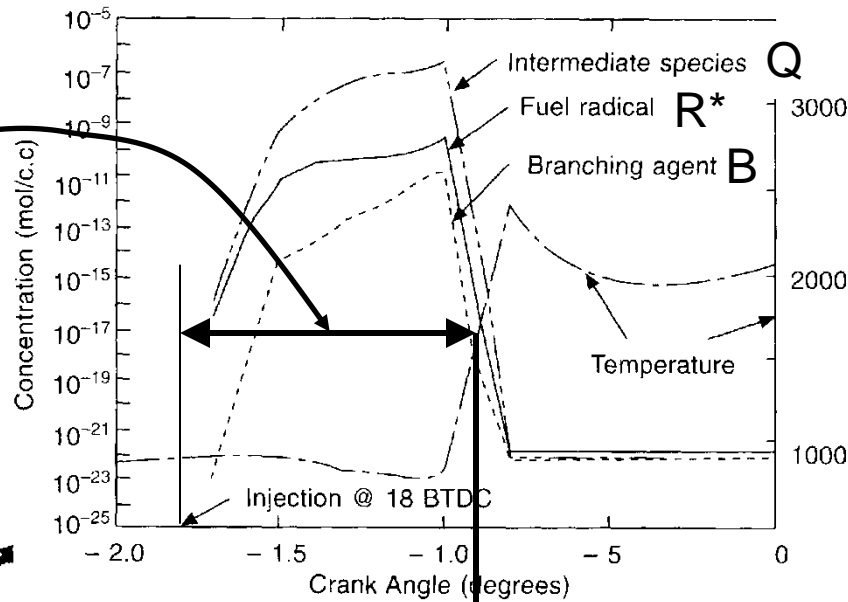
Glassman, 1996



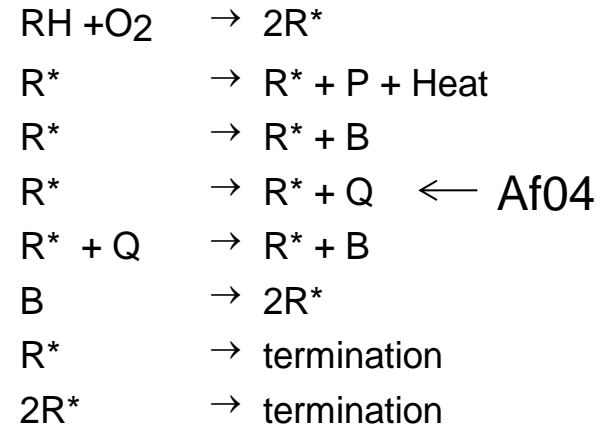


Basic combustion concepts – Diesel (CI)

Ignition Delay



Shell Ignition Model

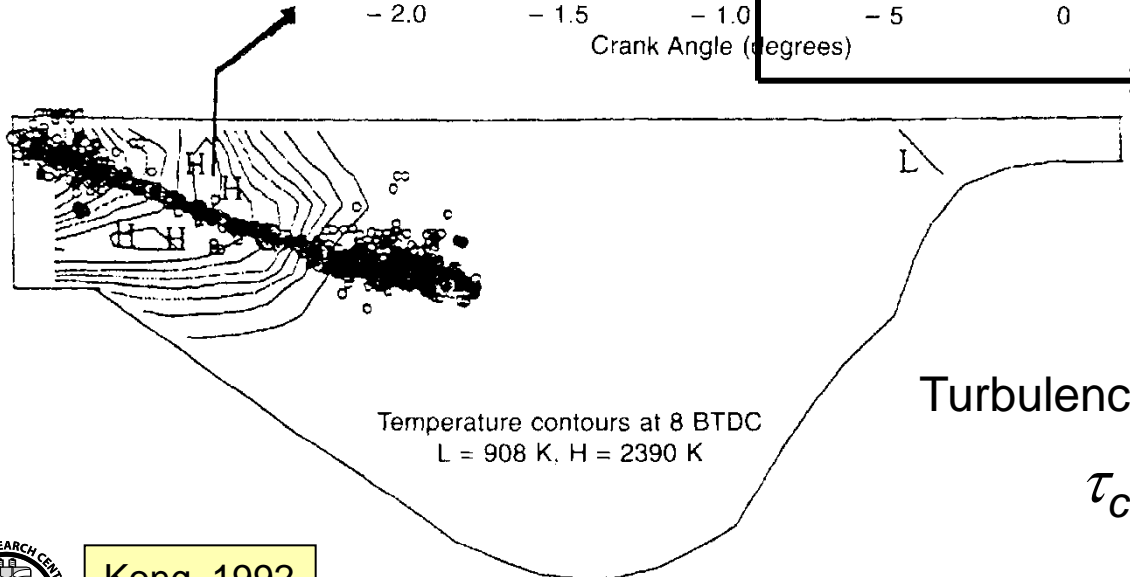


Switch to Characteristic Time Combustion model

$$\frac{dY_i}{dt} = -\frac{Y_i - Y_i^*}{\tau_c}$$

Turbulence generated by fuel injection

$$\tau_c \sim k/\varepsilon \sim L_{nozzle} / V_{nozzle}$$



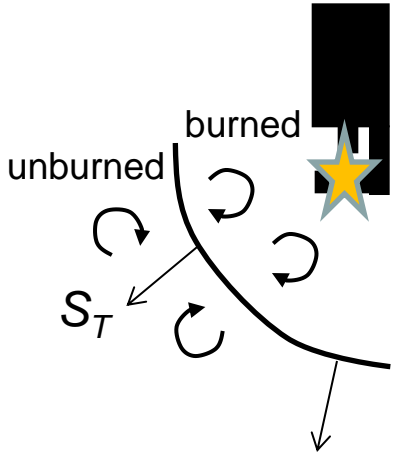
Kong, 1992





Turbulent mixing

Spark-ignition

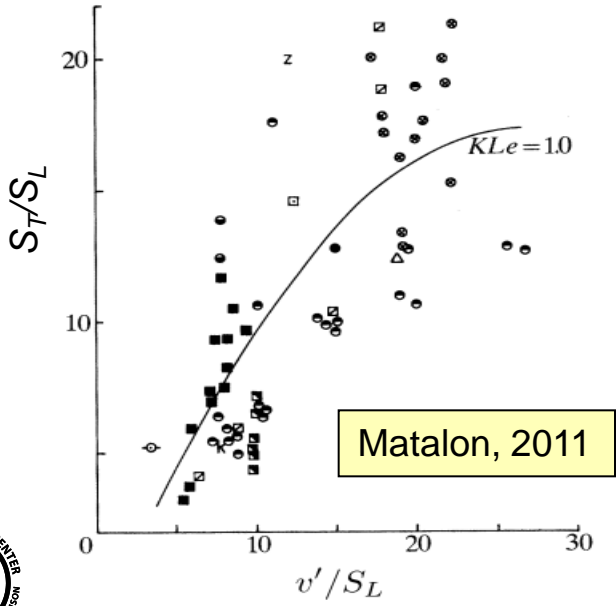
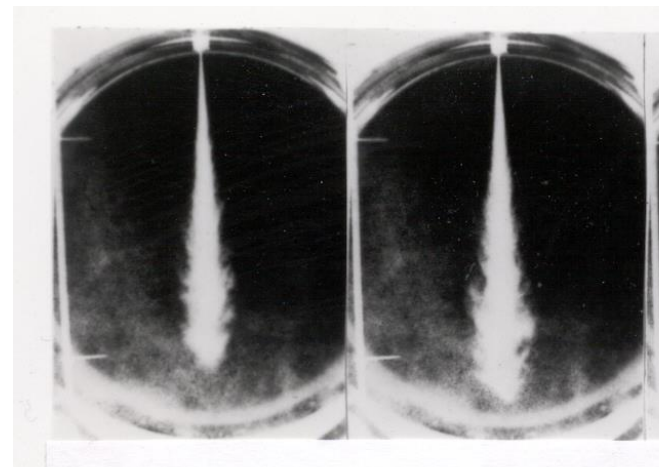


Hot products with Cold reactants

$$\tau \sim k/\epsilon$$

$$\sim L_{piston} / V_{piston}$$

High turbulence
- faster combustion



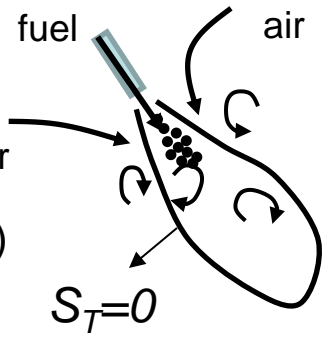
Injected fuel with entrained air

Diesel

$$\tau \sim k/\epsilon$$

$$\sim L_{nozzle} / V_{nozzle}$$

Delayed ignition (PCCI)
- better mixing

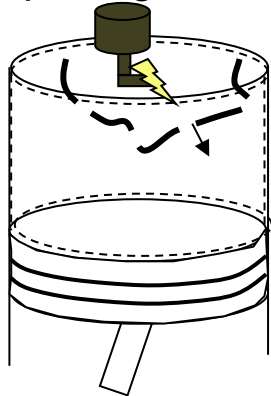




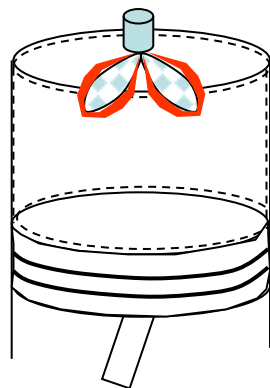
Summary of combustion regimes

- Gasoline engine spark-ignition with flame propagation:
 - High turbulence for high flame speed \rightarrow heat losses. Issues: NO_x and UHC/CO, knock (CR, fuels), throttling losses \rightarrow low thermal efficiency TE ~25%
- Diesel engine with spray (diffusion) combustion:
 - Rich mixtures (soot) & high temperatures (NO_x) \rightarrow higher TE ~45%
- H/Premixed Charge Compression Ignition – LTC, chemistry controlled (CR):
 - Sensitive to fuel, poor combustion/load control, low NO_x-soot \rightarrow TE ~50%

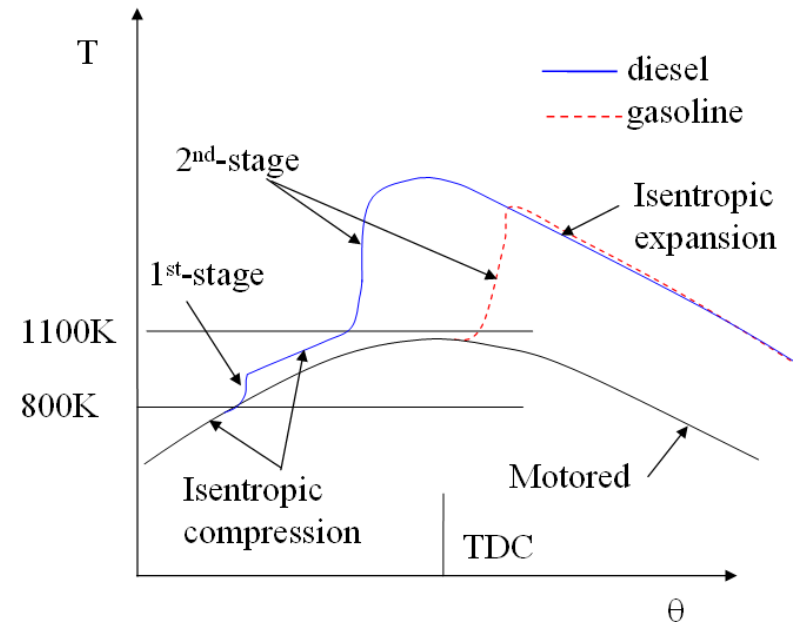
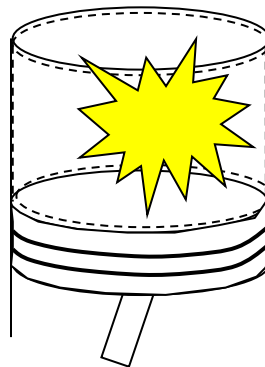
spark-ignition



diesel



H/PCCI



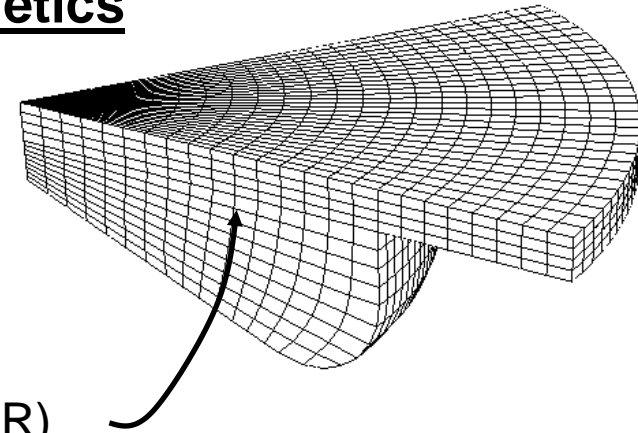


Premixed volumetric combustion & chemical kinetics

Species and energy conservation equations

$$\left(\frac{\partial \rho_i}{\partial t}\right) + \nabla \cdot (\rho_i \mathbf{u}) = \nabla \cdot [\rho D \nabla \left(\frac{\rho_i}{\rho}\right)] + \dot{\rho}_i^c + \dot{\rho}_i^s$$

$$\left(\frac{\partial (\rho I)}{\partial t}\right) + \nabla \cdot (\rho \mathbf{u} I) = -p \nabla \cdot \mathbf{u} - \nabla \cdot \mathbf{J} + \rho \varepsilon + \dot{Q}^c + \dot{Q}^s + \dot{Q}^r$$



Constant volume combustion – Well-Stirred-Reactor (WSR)

$$\frac{dY_i}{dt} = \frac{W_i}{\rho} \sum_{k=1}^{n_r} (\nu''_{k,i} - \nu'_{k,i}) \omega_k(\mathbf{Y}, T), \quad i = 1, \dots, n_s$$

$$\sum_{i=1}^{n_s} \nu'_{k,i} M_i = \sum_{i=1}^{n_s} \nu''_{k,i} M_i, \quad k = 1, \dots, n_r$$

$$\omega_k(\mathbf{Y}, T) = \kappa_{f,k} \prod_{i=1}^{n_s} \left(\frac{\rho Y_i}{W_i}\right)^{\nu'_{k,i}} - \kappa_{b,k} \prod_{i=1}^{n_s} \left(\frac{\rho Y_i}{W_i}\right)^{\nu''_{k,i}}$$

$$\kappa_{f,k}(T) = A_k T^{b_k} \exp\left(-\frac{E_k}{RT}\right) \quad ; \quad \kappa_{b,k}(T) = \kappa_{f,k}(T) / K c_{eq,k}(T)$$

$$K c_{eq,k}(T) = \exp(-\Delta g_k^0) \left(\frac{p_{atm}}{RT}\right)^{\sum_{i=1}^{n_s} (\nu''_{k,i} - \nu'_{k,i})}$$

$$\frac{dT}{dt}(\mathbf{Y}, T) = -\frac{1}{\bar{c}_v(\mathbf{Y}, T)} \sum_{i=1}^{n_s} \left(\frac{e_i(T)}{W_i} \frac{dY_i}{dt}(\mathbf{Y}, T)\right)$$

- I specific internal energy
- M_i chemical label
- n_r reactions
- n_s species
- $\nu'_{k,i}, \nu''_{k,i}$ reactant/product stoichiometric coefficients
- Y_i mass fraction
- W_i molecular weight
- e_i species energy

$$10 \quad e_i = R_{mol} \left[(a_i - 1) T + \frac{b_i}{2} T^2 + \frac{c_i}{3} T^3 + \frac{d_i}{4} T^4 + \frac{e_i}{5} T^5 + f_i \right]$$



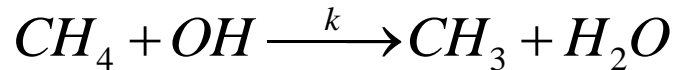


Homogeneous charge: no spatial gradients

$$\frac{\partial Y_i}{\partial t} = \omega_i / \rho$$

$$\frac{\partial T}{\partial t} = - \sum_{i=1}^{n_s} \frac{\Delta h_{f,i}^0 \omega_i}{\rho c_p}$$

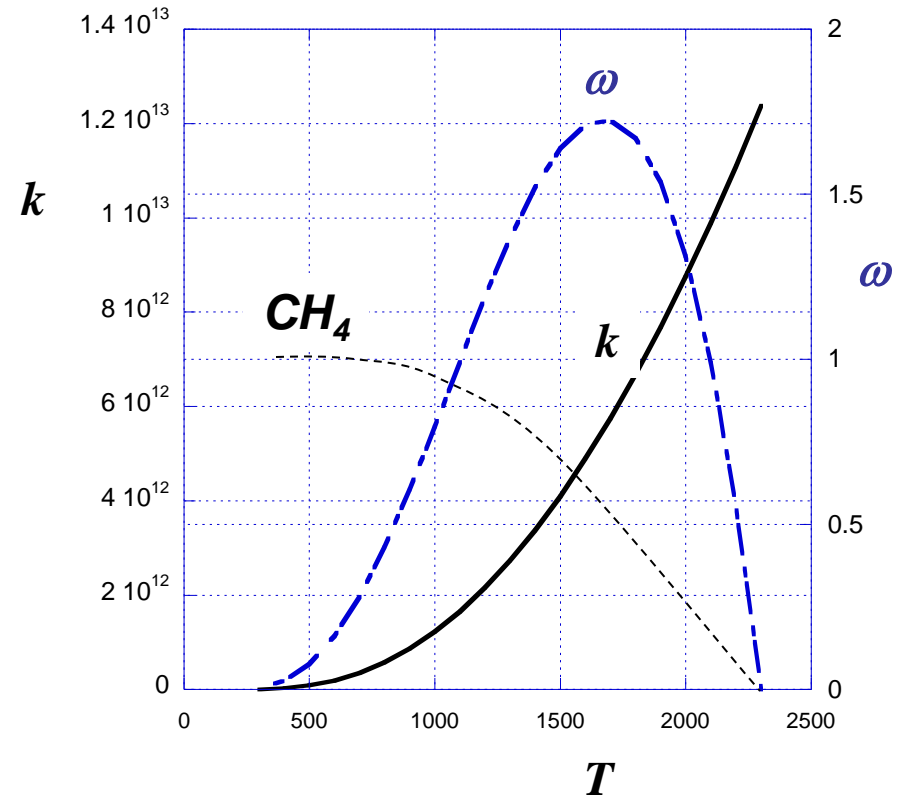
Consider single overall reaction



$$k = AT^b \exp(-E/RT)$$

$$\frac{d[CH_4]}{dt} = -k[CH_4][OH] = \frac{\omega_{CH_4}}{\rho W_{CH_4}}$$

$$A = 1.6 \cdot 10^7 \text{ (cm, mol, s)}, b = 1.83, E = 11.6 \text{ (kJ / mol)}$$





HCCI: Ignition delay

$$\frac{\partial Y_i}{\partial t} = \omega_i / \rho$$

$$\frac{\partial T}{\partial t} = - \sum_{i=1}^{n_s} \frac{\Delta h_{f,i}^0 \omega_i}{\rho c_p}$$

Consider single component system

$$U = \frac{T - T_{unburned}}{T_{burned} - T_{unburned}}$$

Example:

$$\frac{dU}{dt} = F(U) = \beta U^{m+1} (1-U)^m$$

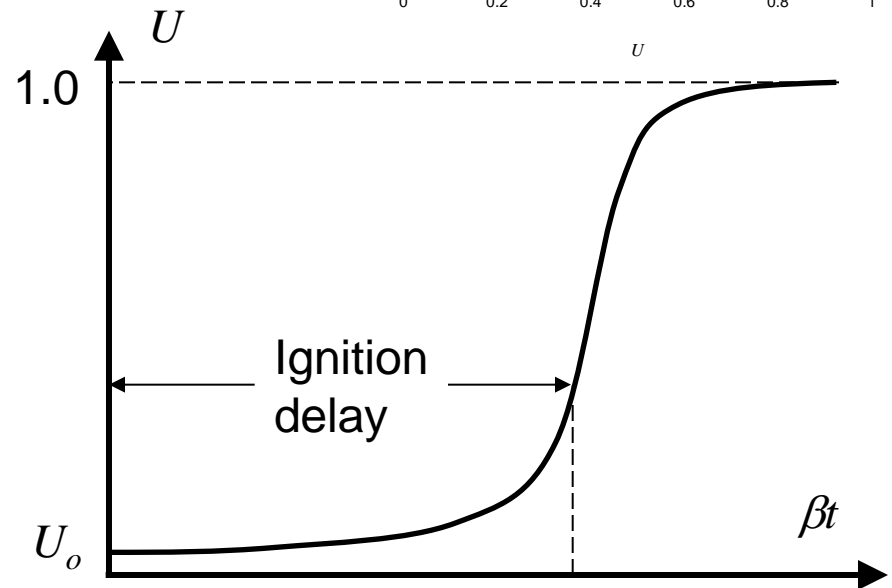
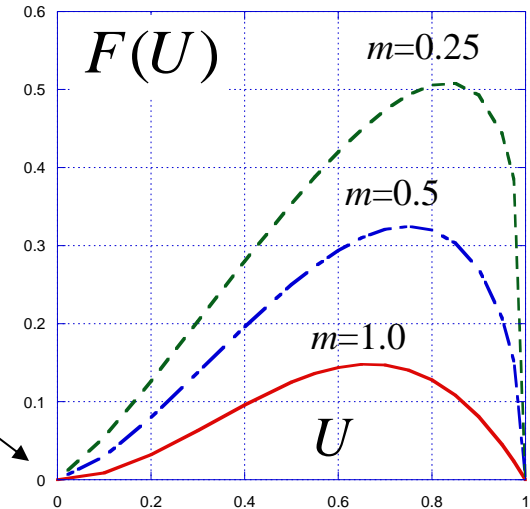
For $U \rightarrow U_0$: $m\beta t = \frac{1}{U_0^m} - \frac{1}{U^m}$

So, time to reach, say, $5U_0$:

Ignition delay:

$$\beta t = \frac{4}{5mU_0^m}$$

Cold boundary difficulty

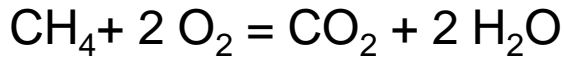


$$m\beta t = \text{Const.} - \frac{1}{U^m} {}_2F_1(-m, m; (1-m); U)$$





Combustion chemistry models – CH₄ (15 spec, 31 react.)



H₂ O₂ chemistry ↑

Hydrogen-Oxygen Chain

- 1 H + O₂ ⇌ OH + O
- 2 H₂ + O ⇌ OH + H
- 3 H₂ + OH ⇌ H₂O + H
- 4 H₂O + O ⇌ 2 OH

Hydroperoxyl Formation and Consumption

- 5^b H + O₂ + M ⇒ HO₂ + M
- 6 HO₂ + H ⇒ 2 OH
- 7 HO₂ + H ⇒ H₂ + O₂
- 8 HO₂ + H ⇒ H₂O + O
- 9 HO₂ + OH ⇒ O₂ + H₂O

Conversion of Carbon Monoxide to Carbon Dioxide

- 10 CO + OH ⇌ CO₂ + H

Methane Consumption

- 11 CH₄ + H ⇌ H₂ + CH₃
- 12 CH₄ + OH ⇒ H₂O + CH₃

High temperature ↑

Initiation
H atom abstraction

Methylidyne Reactions

- 27 CH + O₂ ⇒ CHO + O
- 31 CH + OH ⇒ CH₂O + H

Methyl Reactions

- 13 CH₃ + O ⇒ CH₂O + H
- 14 CH₃ + OH ⇒ CH₂O + H + H
- 15 CH₃ + OH ⇒ CH₂O + H₂
- 16^c CH₃ + H ⇒ CH₄
- 23 CH₃ + H ⇒ CH₂ + H₂
- 28 CH₃ + OH ⇒ CH₂ + H₂O

Formaldehyde Reactions

- 17 CH₂O + H ⇒ CHO + H₂
- 18 CH₂O + OH ⇒ CHO + H₂O

Formyl Reactions

- 19 CHO + H ⇒ CO + H₂
- 20 CHO + OH ⇒ CO + H₂O
- 21 CHO + O₂ ⇒ CO + HO₂
- 22 CHO + M ⇒ CO + H + M

Methylene Reactions

- 24 CH₂ + O₂ ⇒ CO₂ + H₂
- 25 CH₂ + O₂ ⇒ CO + OH + H
- 26 CH₂ + H ⇌ CH + H₂
- 29 CH₂ + OH ⇒ CH₂O + H
- 30 CH₂ + OH ⇒ CH + H₂O

End

Start

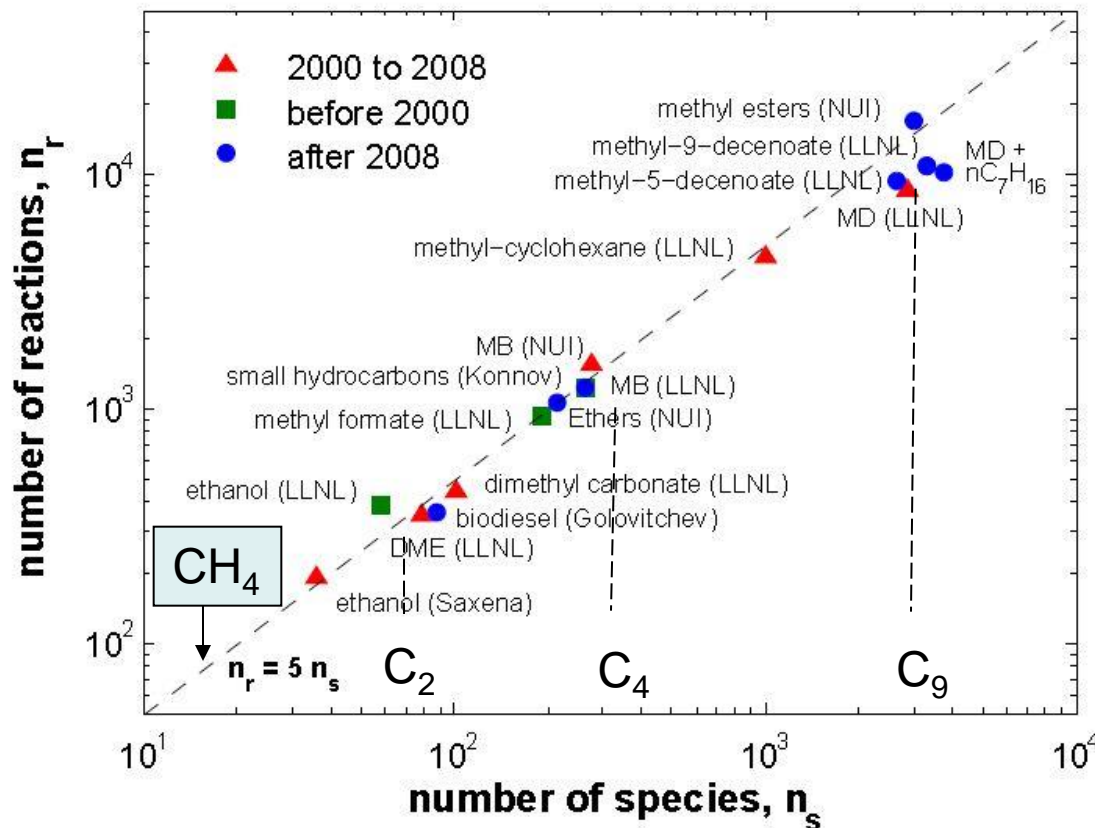
Conversion to products by sequential fragmentation by H abstraction



Chemical kinetic mechanisms for engine simulations

Requirements for mechanisms for practical engine simulations:

- Size can not be too large due to CPU time limitation ~ 100 species
- Capable of predicting auto-ignition delay time accurately
- Contain proper reactions for pollutant formation precursors

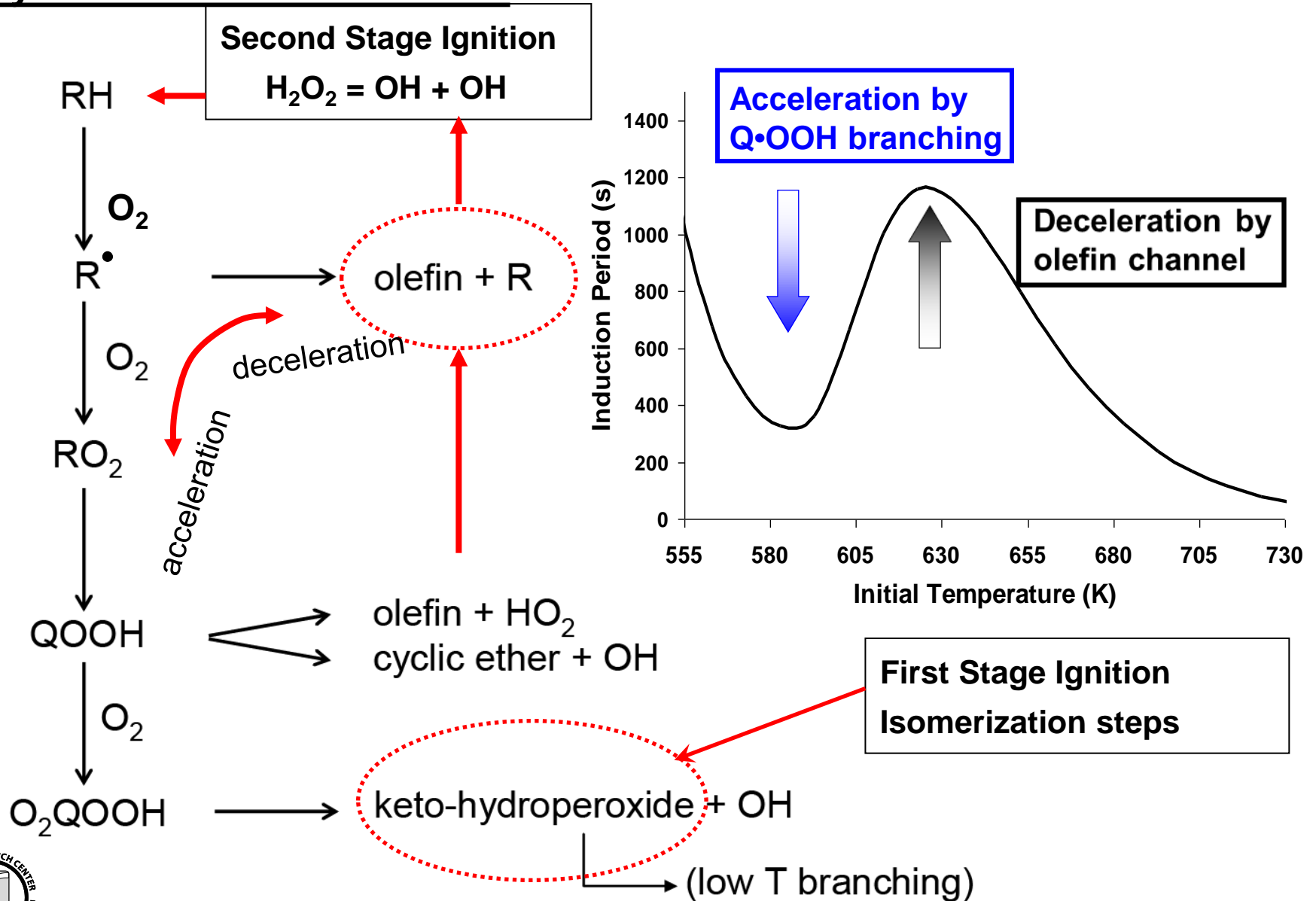


Biodiesel surrogates
- Significant mechanism reduction is required.

Soy biodiesel - Methyl:
- palmitate (C16:0)
- stearate (C18:0)
- oleate (C18:1)
- linoleate (C18:2)
- linolenate (C18:3)



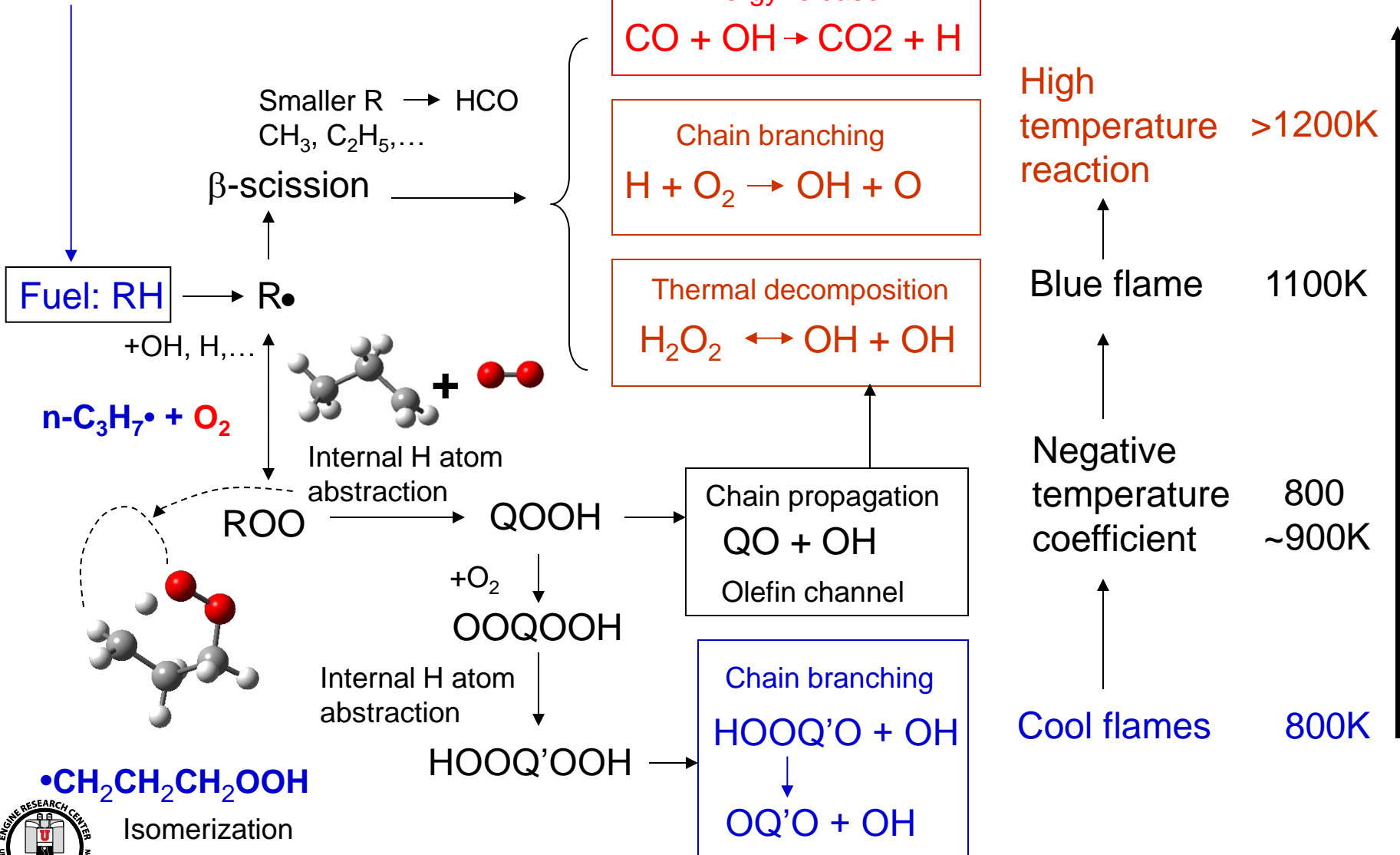
Hydrocarbon kinetics - NTC





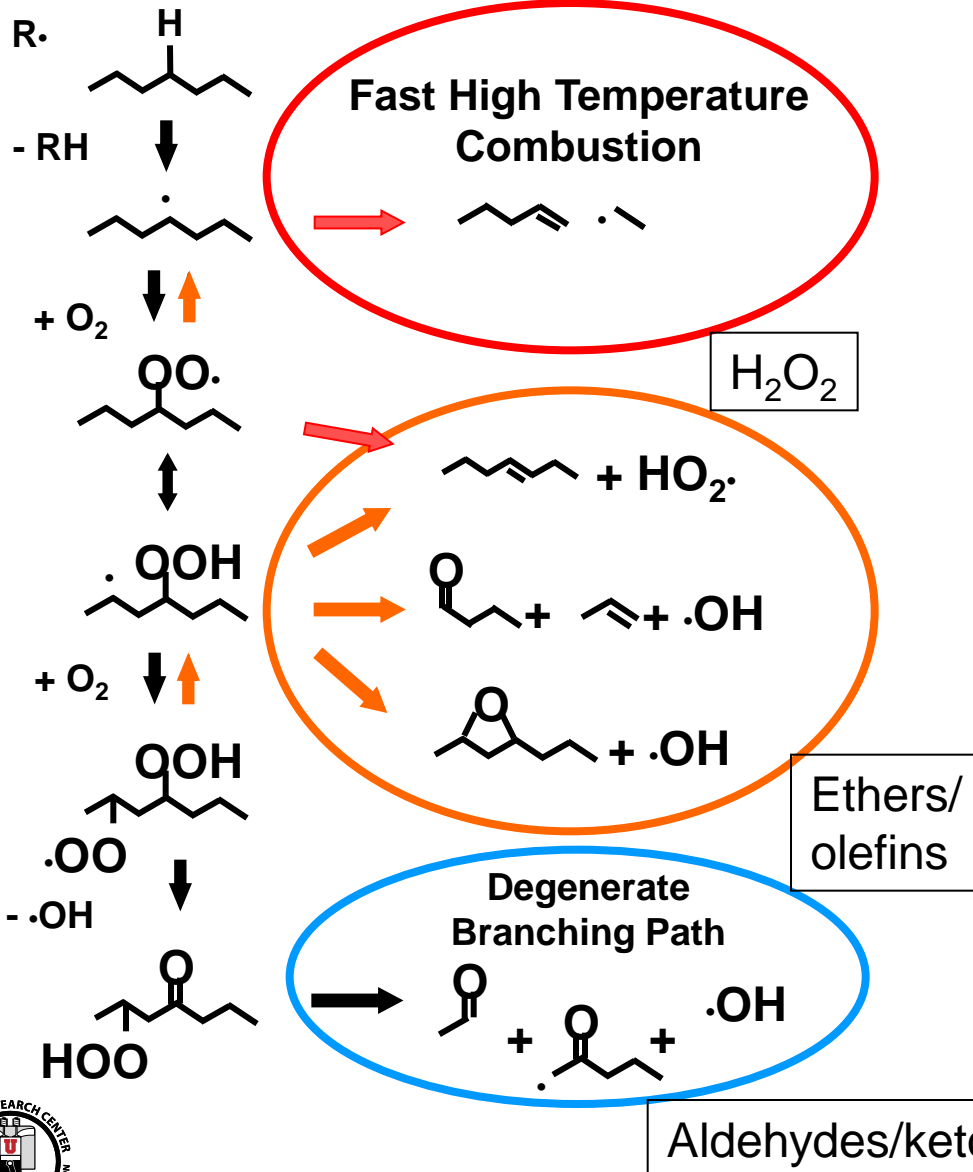
Alkane fuel oxidation

Example: Propane

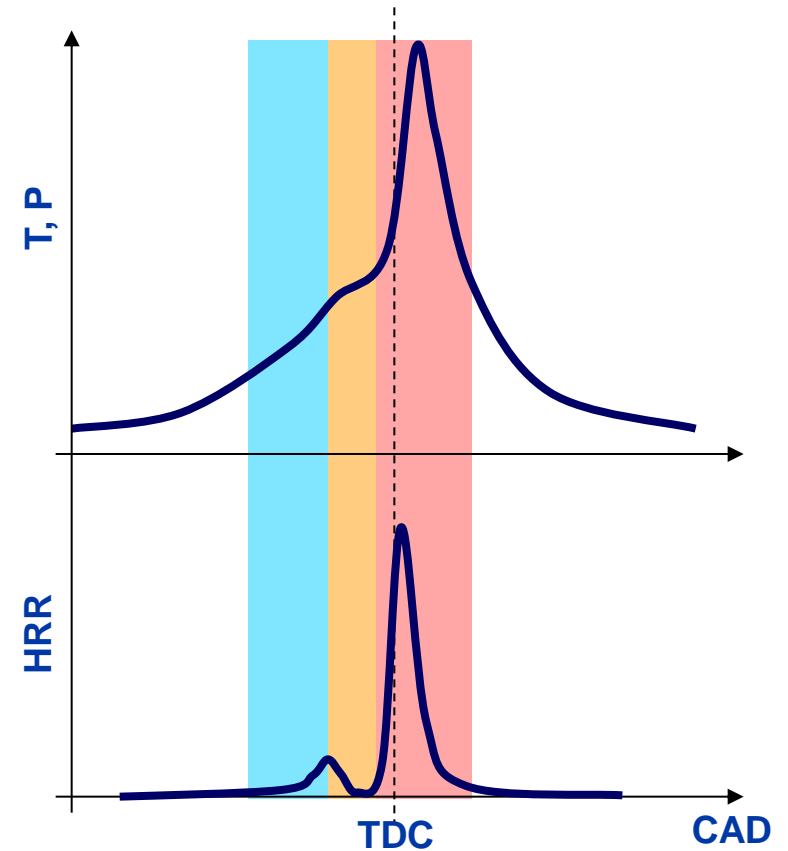




HCCI combustion kinetics

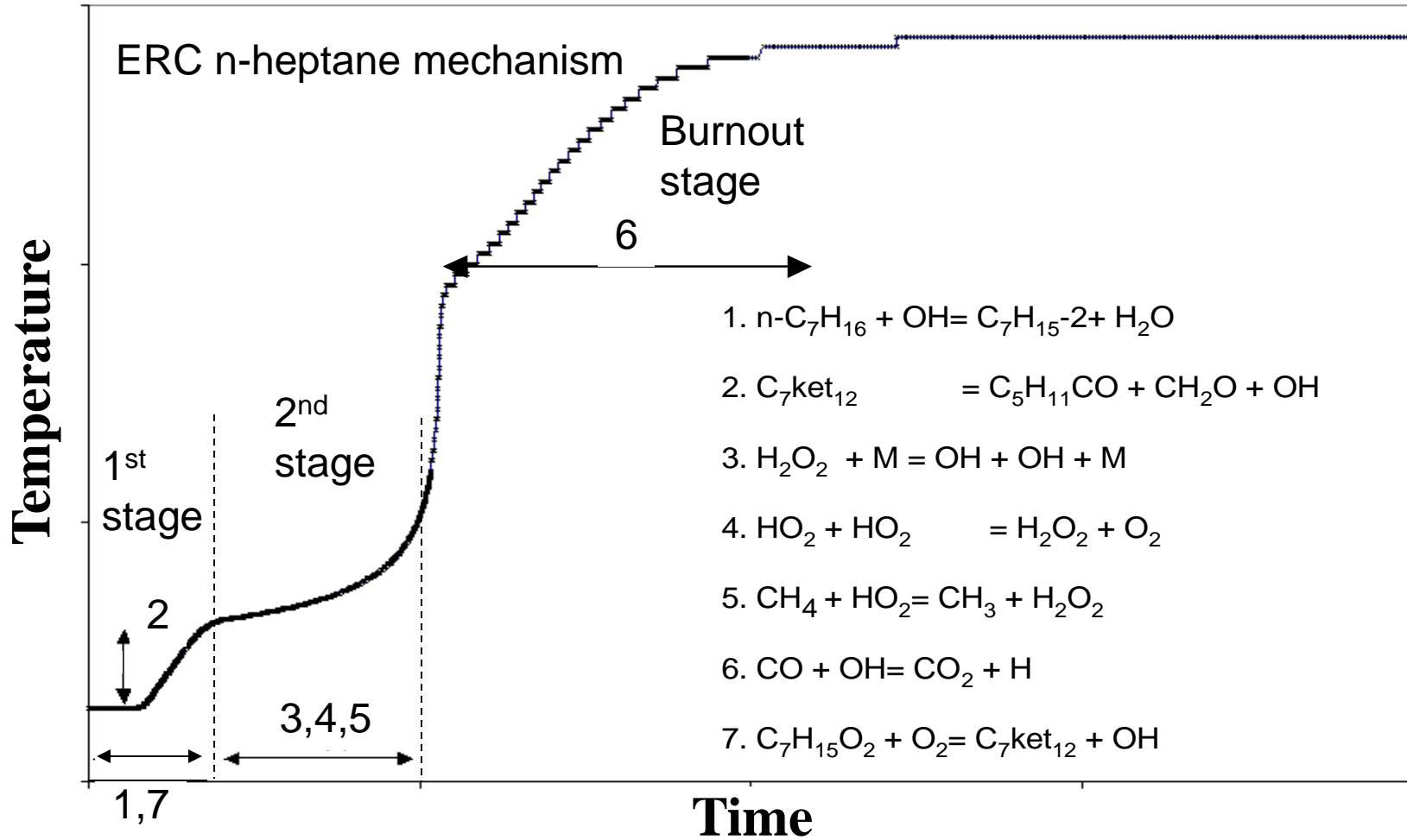


Typical HCCI Combustion Temperature and Heat Release Rate profiles



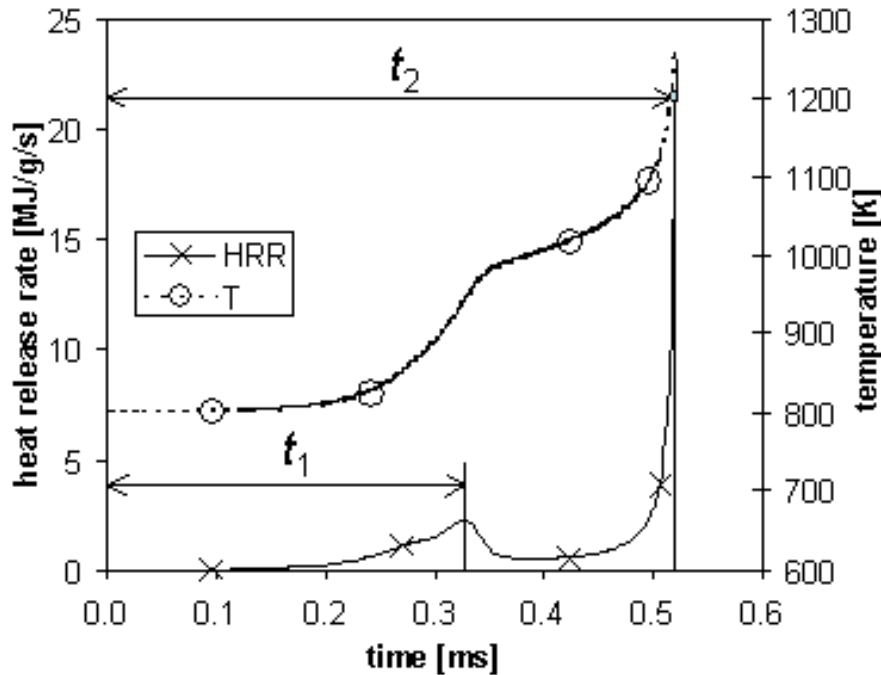


Mechanism reduction – identify key reaction steps



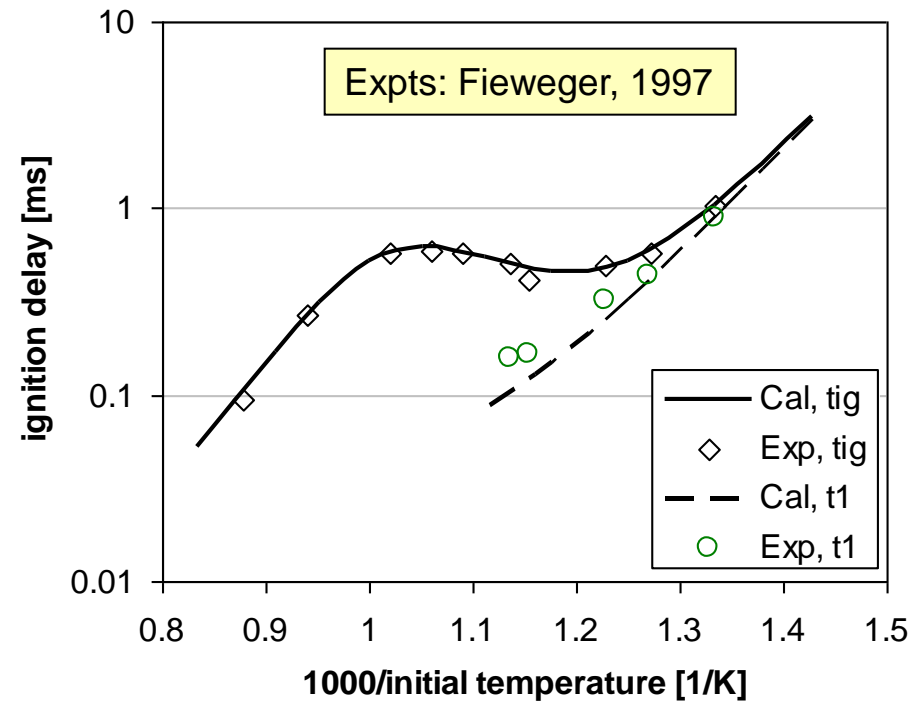


Reduced mechanisms: match shock tube and RCM data



Predicted ignition delay times
 validated against shock tube tests
 (data from Fieweger)
 $\phi=1.0$ and $P=40$ bar n-heptane/air

First stage (t_1), main ignition ($t_2=t_{ig}$) delay





Mechanism reduction methodology

Reduction of reaction pathways and species number

- combination of chemical lumping, graphical reaction flow analysis and elimination methods

Reaction rate optimization

- ignition delay curve sensitivity analysis

Pre-exponential: $A = k \times A_{base}$

Ignition delay sensitivity coefficient

$$S_{ig}(T) = 100 \times \frac{(\log_{10} t_{k_1} - \log_{10} t_{k_2})}{\log_{10} t_{base} \log_{10}(k_1/k_2)}$$

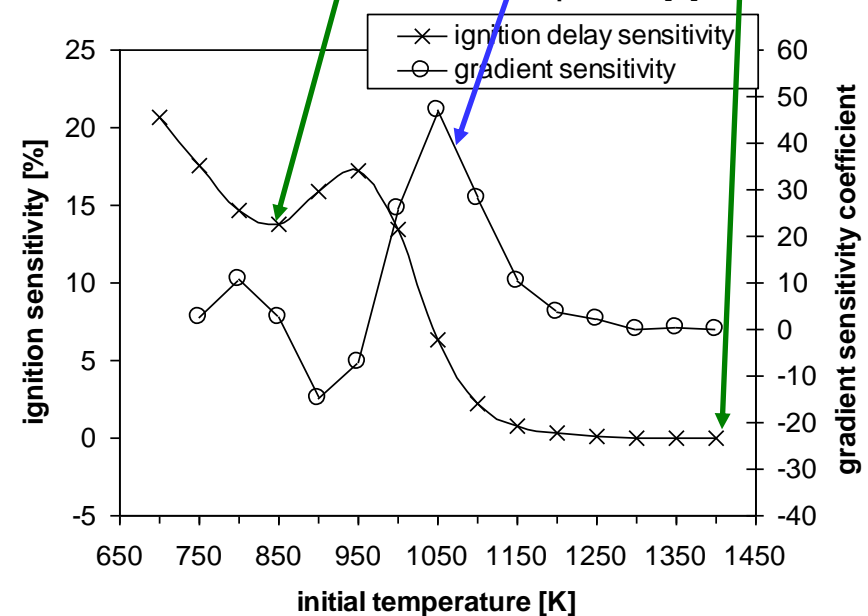
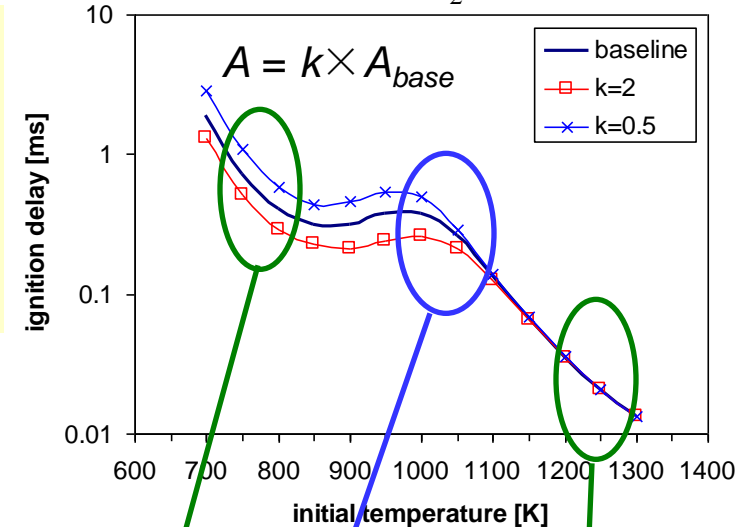
Ignition delay gradient sensitivity coefficient

$$S_{gr}(T) = \frac{\frac{d \log_{10} t_{k_1}}{dT} - \frac{d \log_{10} t_{k_2}}{dT}}{\log_{10}(k_1/k_2)} \times 100$$

Positive S_{gr} : counter-clockwise rotation

Negative S_{gr} : clockwise rotation

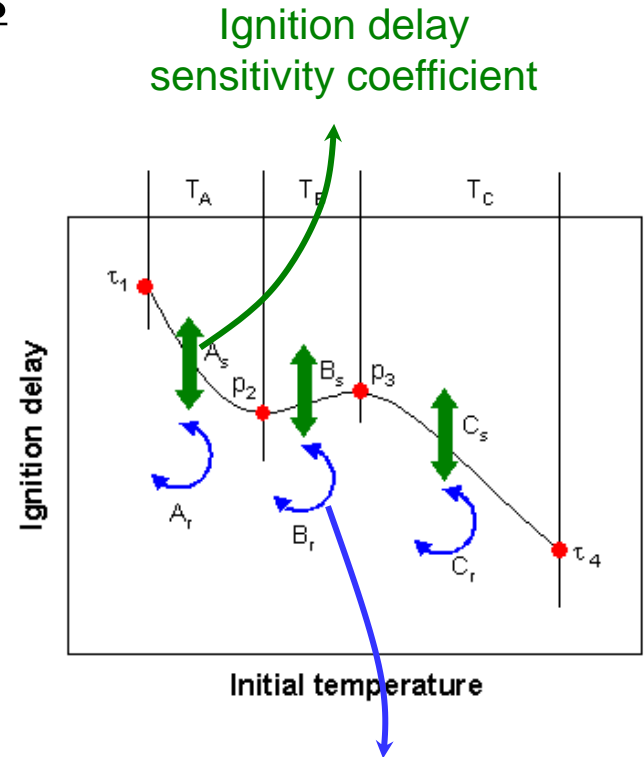
tetra-decane: $\dot{R}OO + O_2 = R\text{-keto} + OH$





Mechanism reduction – group reaction classes

No	Reaction	A _s	B _s	C _s	A _r	B _r	C _r	effect
I	$RH + H = \dot{R} + H_2O$							
II	$RH + OH = \dot{R} + H_2O$	●↓		●↑		●C		τ_1, p_2, p_3, τ_4
III	$RH + HO_2 = \dot{R} + H_2O_2$	○↓	○↓	○↓				τ_1, P_2, P_3, τ_4
IV	$RH + O_2 = \dot{R} + HO_2$		○↑	○↓		●		P_2, P_3
V	$\dot{R} + O_2 = R\dot{O}O$							
VI-a	$R\dot{O}O = \dot{Q}OOH$	●↓	●↓			○C		τ_1, P_2
VI-b	$\dot{Q}OOH + O_2 = \dot{O}OQOOH$	○↓	●↓					P_2, P_3
VI-c	$\dot{O}OQOOH = R\text{-keto} + OH$	○↓	●↓					P_2, P_3
VII	$R\text{-keto} = CH_2O + R'CO + OH$	●↓			○C			τ_1
VIII	$R'CO = X_1 + X_2 + CO$							
IX	$\dot{R} = S_1 + S_2 + S_3$		●↑				○	P_2, P_3, τ_4



Sensitivity of ignition delay curves of n-heptane oxidation

- solid circle, open circle and blank entry denote dominant, mild and not significant influence, respectively.
- C indicates counter-clockwise rotation.
- Circle only indicates clockwise rotation.





ERC-MultiChem: PRF

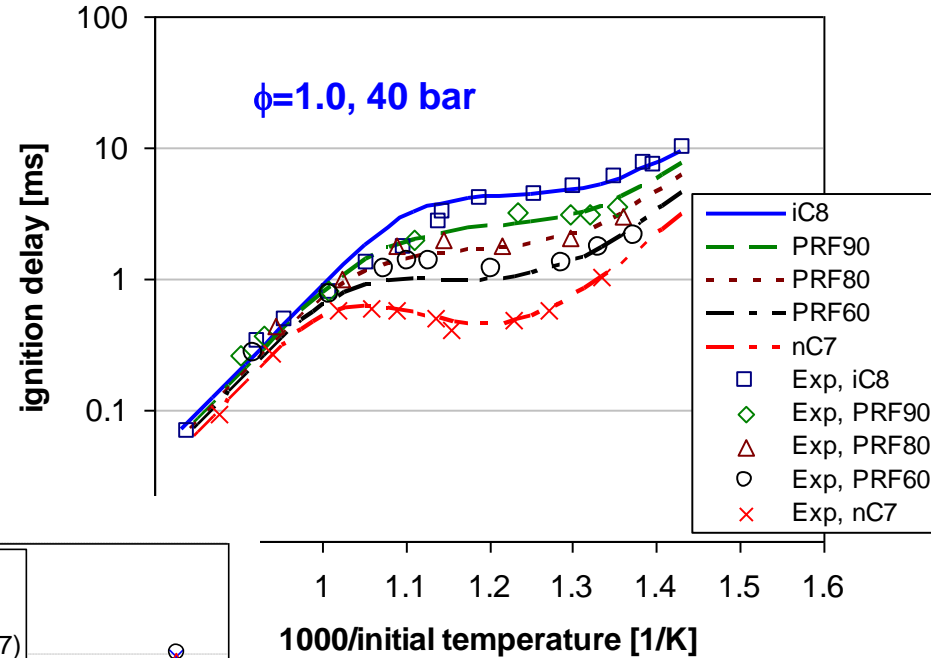
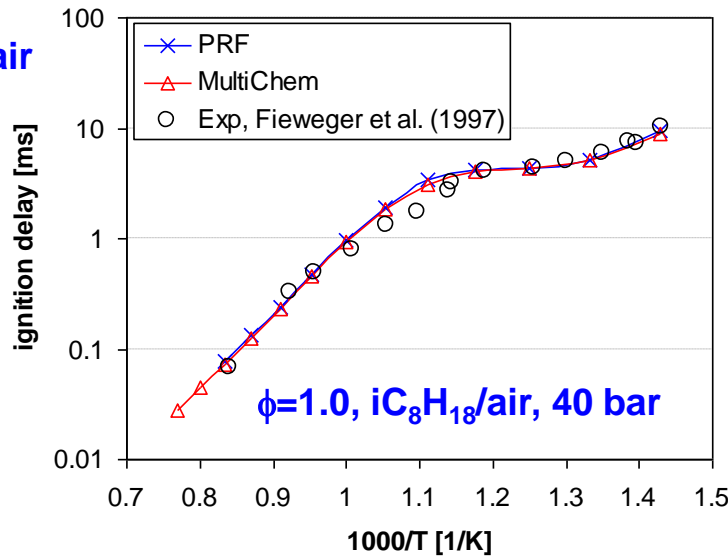
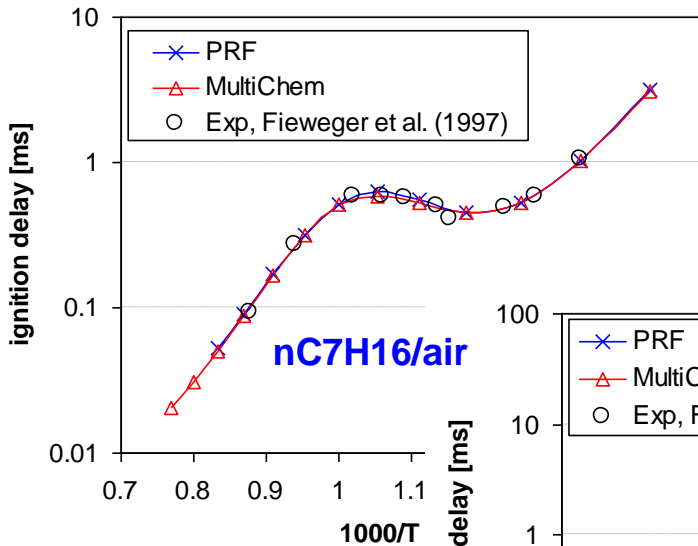
41 species, 158 reactions → base mechanism

Source mechanisms: LLNL n-heptane

(560 species; 2,539 reactions), isooctane

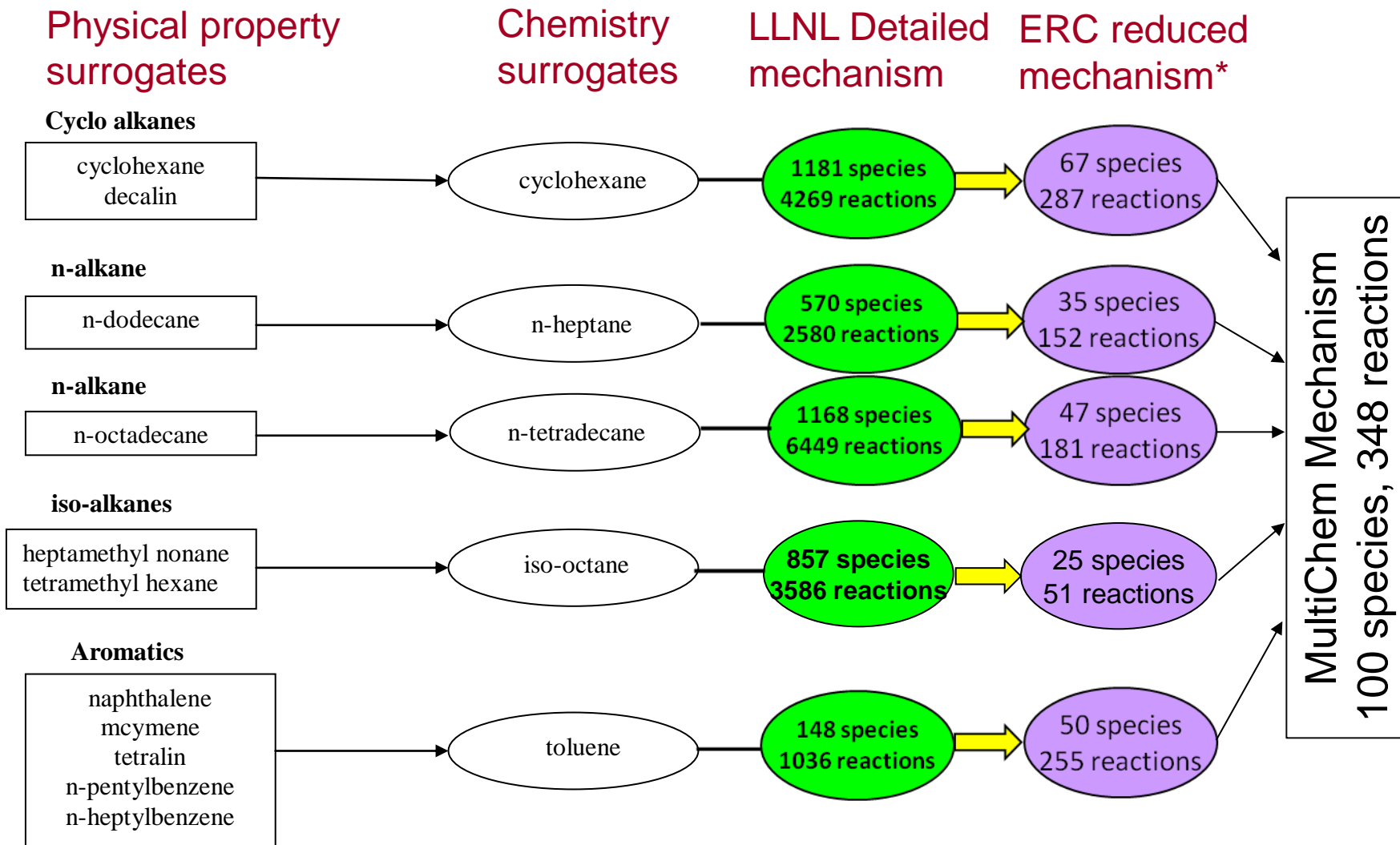
(857 species; 3,606 reactions),

ERC n-heptane (29 species; 52 reactions)





Chemical class grouping: “MultiChem” skeletal mechanism

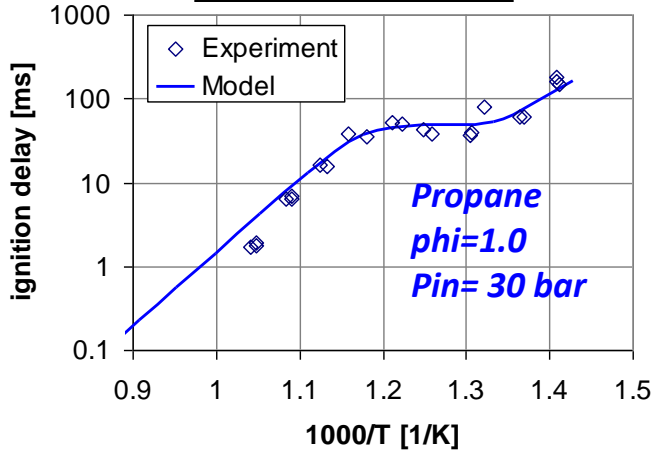




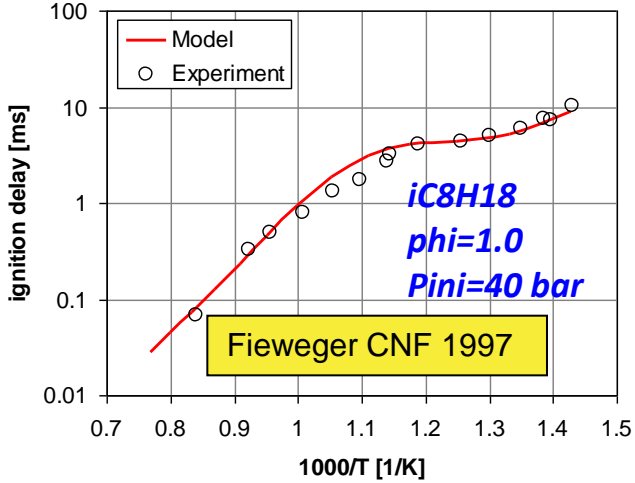
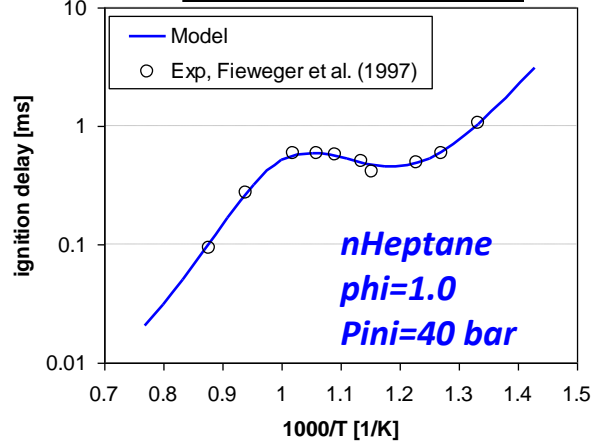
Ignition delay validations - "MultiChem"

8 Surrogate fuels: *n*-heptane, *iso*-octane, tetradecane, cyclohexane, toluene, decalin, ethanol, MB/D.....

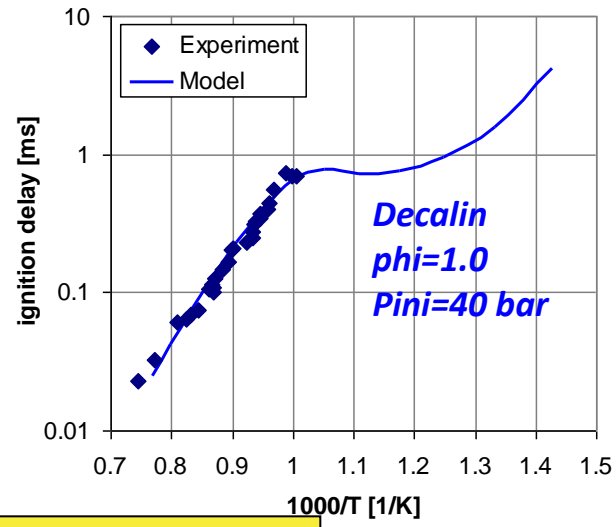
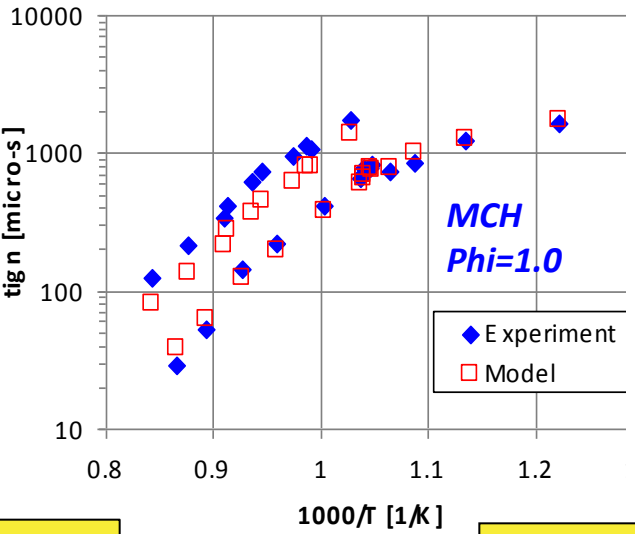
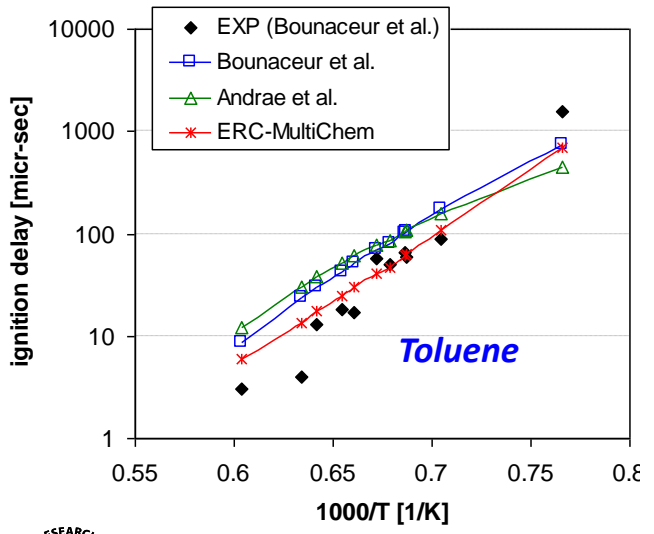
Gauthier CNF 2004



Fieweger CNF 1997



Fieweger CNF 1997



Bouaceur IJCK 2005; Andrae CNF 2005

Shen, Energy & Fuels, 2009





3-D CFD modeling

Solve conservation equations on (moving) numerical mesh

Mass

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = \dot{\rho}^s$$

Species

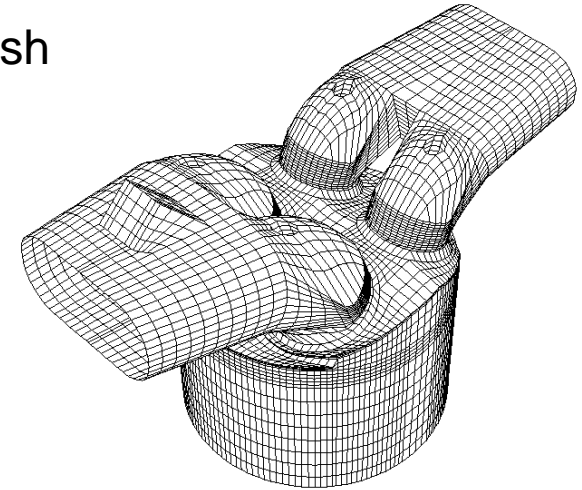
$$\frac{\partial \rho_m}{\partial t} + \nabla \cdot (\rho_m \mathbf{u}) = \nabla \cdot \left[\rho D \nabla \left(\frac{\rho_m}{\rho} \right) \right] + \dot{\rho}_m^c + \dot{\rho}_m^s$$

Momentum

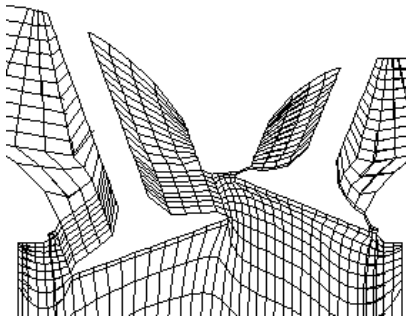
$$\frac{\partial (\rho \mathbf{u})}{\partial t} + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) = \rho \mathbf{g} + \mathbf{F}^s - \nabla p + \nabla \cdot \bar{\sigma}$$

Energy

$$\frac{\partial (\rho I)}{\partial t} + \nabla \cdot (\rho \mathbf{u} I) = -\nabla \cdot \mathbf{J} + \dot{Q}^c + \dot{Q}^s - p \nabla \cdot \mathbf{u} + \bar{\sigma} : \nabla \mathbf{u}$$



combustion source terms





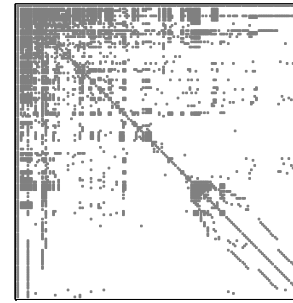
3-D CFD: Improved solver numerics

Sparse analytical Jacobian formulation

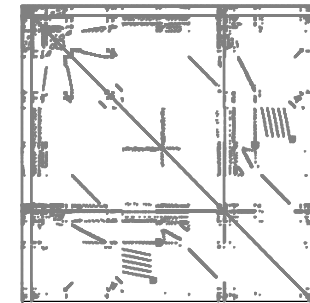
Sparsity of hydrocarbon fuel mechanisms increases with size



47 (62.7%)



160 (86.2%)



2878 (99.7%)

n_s

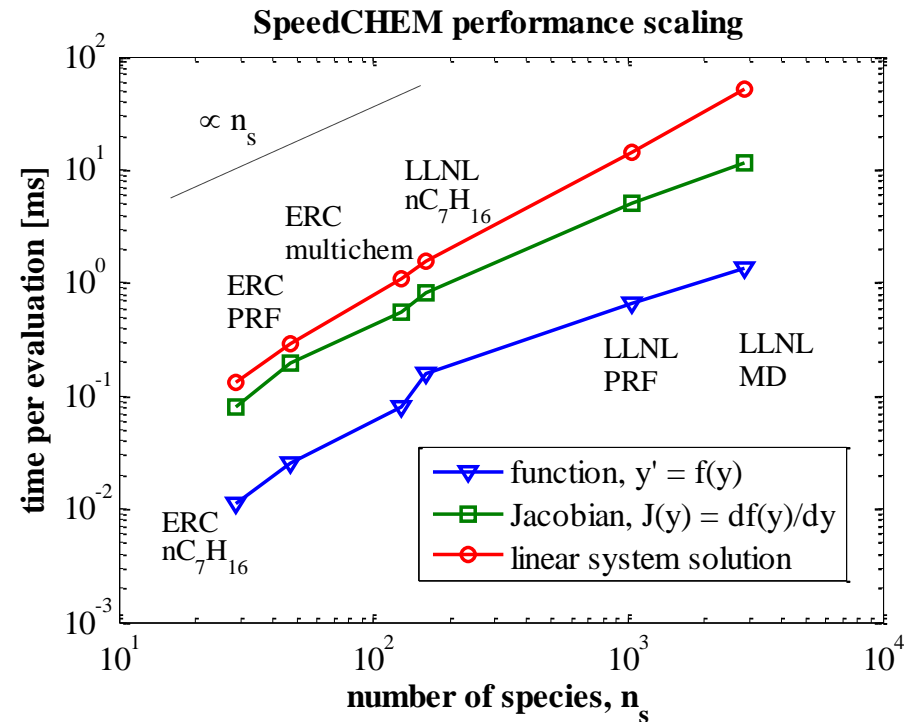
$$\frac{\partial Y^i}{\partial t} = \omega_i / \rho$$

$$\frac{\partial T}{\partial t} = - \sum_{i=1}^{n_s} \frac{\Delta h_{f,i}^0 \omega_i}{\rho c_p}$$

$$\mathbf{J} = \begin{array}{|c|c|} \hline \textcircled{4} \frac{\partial \dot{T}}{\partial T} & \frac{\partial \dot{T}}{\partial Y_j} \textcircled{2} \\ \hline \frac{\partial \dot{Y}_i}{\partial T} \textcircled{3} & \frac{\partial \dot{Y}_i}{\partial Y_j} \textcircled{1} \\ \hline \end{array}$$

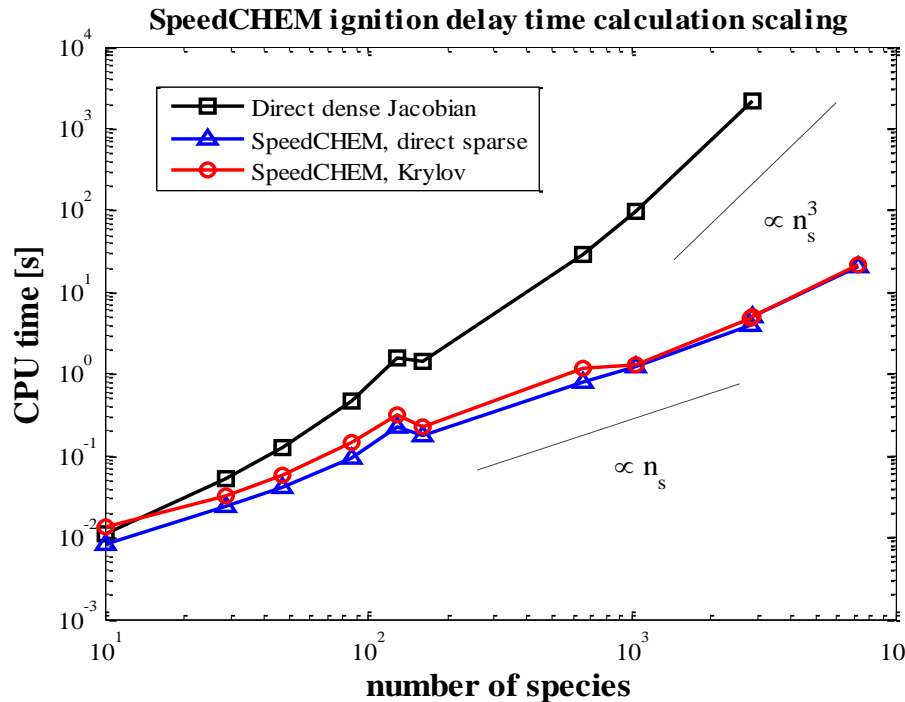
All functions and equations are evaluated in matrix form

ODE system function, analytical Jacobian evaluation and linear system solution achieve linear scaling with n_s





3-D CFD: Improved solver numerics



9 reaction mechanisms tested

- $n_s = 29$ to 7171

- $n_r = 52$ to 31669

18 ignition delay calculations per mech

- $\phi = [0.5, 1.0, 2.0]$

- $T_0 = [650, 800, 1000]$ K

- $p_0 = [20, 50]$ bar

- $t = [0.1]$ s

Promising, efficient approach for **practical engine simulations**

1. Numerically exact solution (no mechanism reduction or manipulation).
2. Speed-up of more than three orders of magnitude at large sizes ($n_s > 1000$)
3. Even for modest sizes (~50-500 species), overall CPU time for chemistry is reduced by 3-10 times in comparison with dense chemistry integrators
4. Preconditioned Krylov solution for future, very large mechanisms



Efficient chemistry solvers – cell clustering

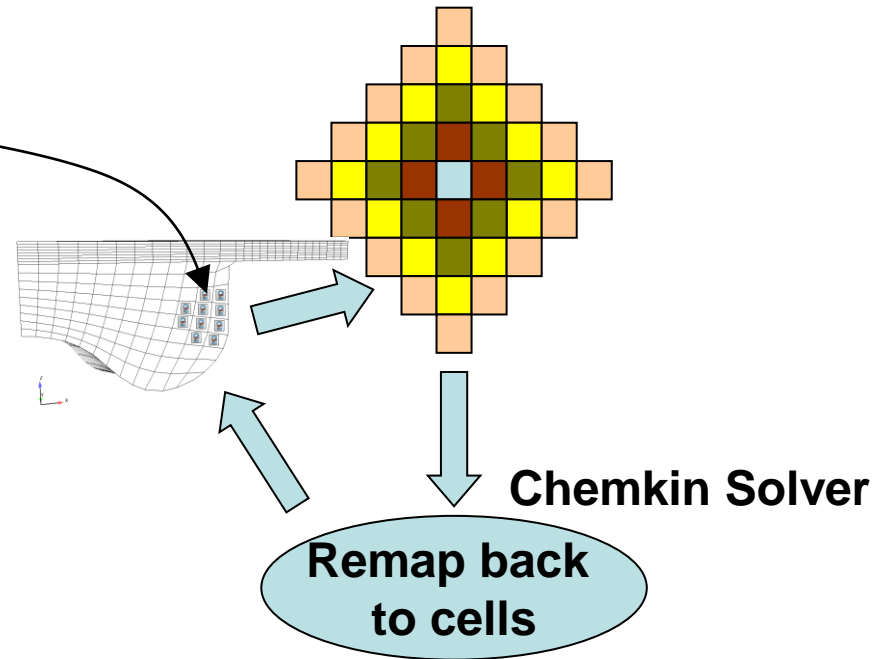
Group thermodynamically-similar cells to reduce the calling frequency to save computer time - Adaptive Mechanism Clustering (AMC) scheme

Extended dynamic adaptive chemistry (EDAC) scheme

Dynamically determine the size of fuel chemical mechanism based on the local and instantaneous thermal conditions of the cells

Thermodynamically similar cells
(similar temperature, equivalence ratio ϕ)

$$\phi = \frac{2C_{-CO_2}^\# + H_{-H_2O}^\# / 2 - z' C_{-CO_2}^\#}{O_{-CO_2-H_2O}^\# - z' C_{-CO_2}^\#}$$

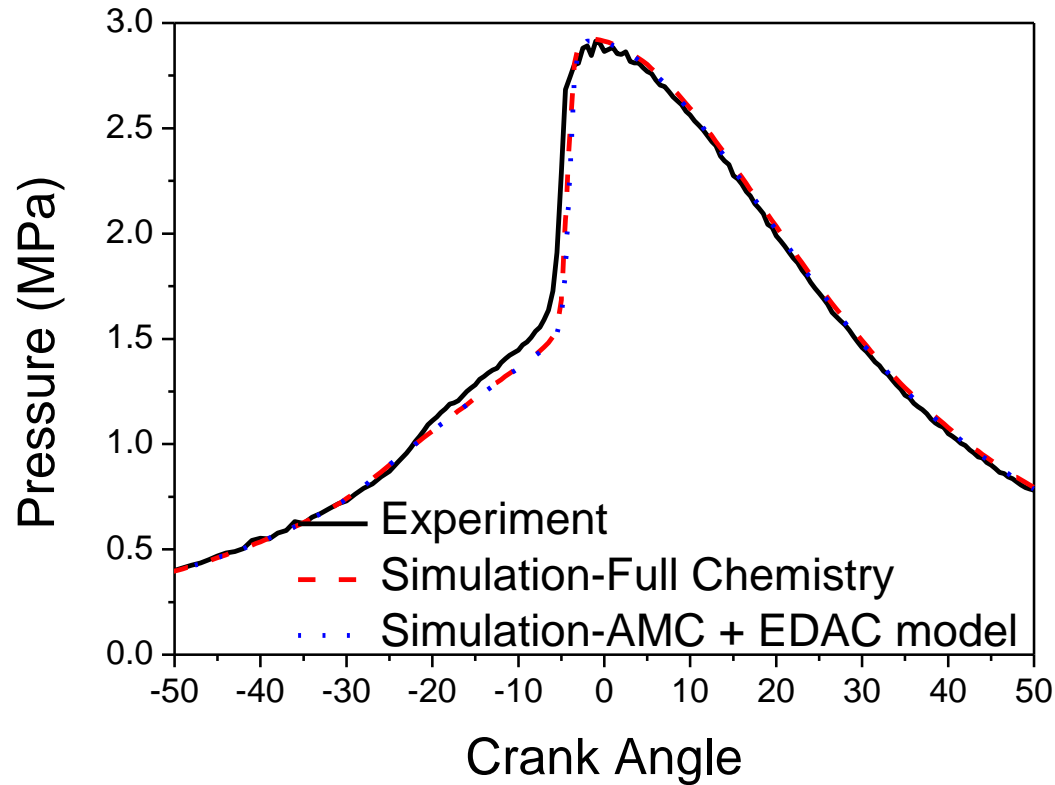




HCCI engine validation

ERC PRF mech.
(39 sp, 141 rxn)

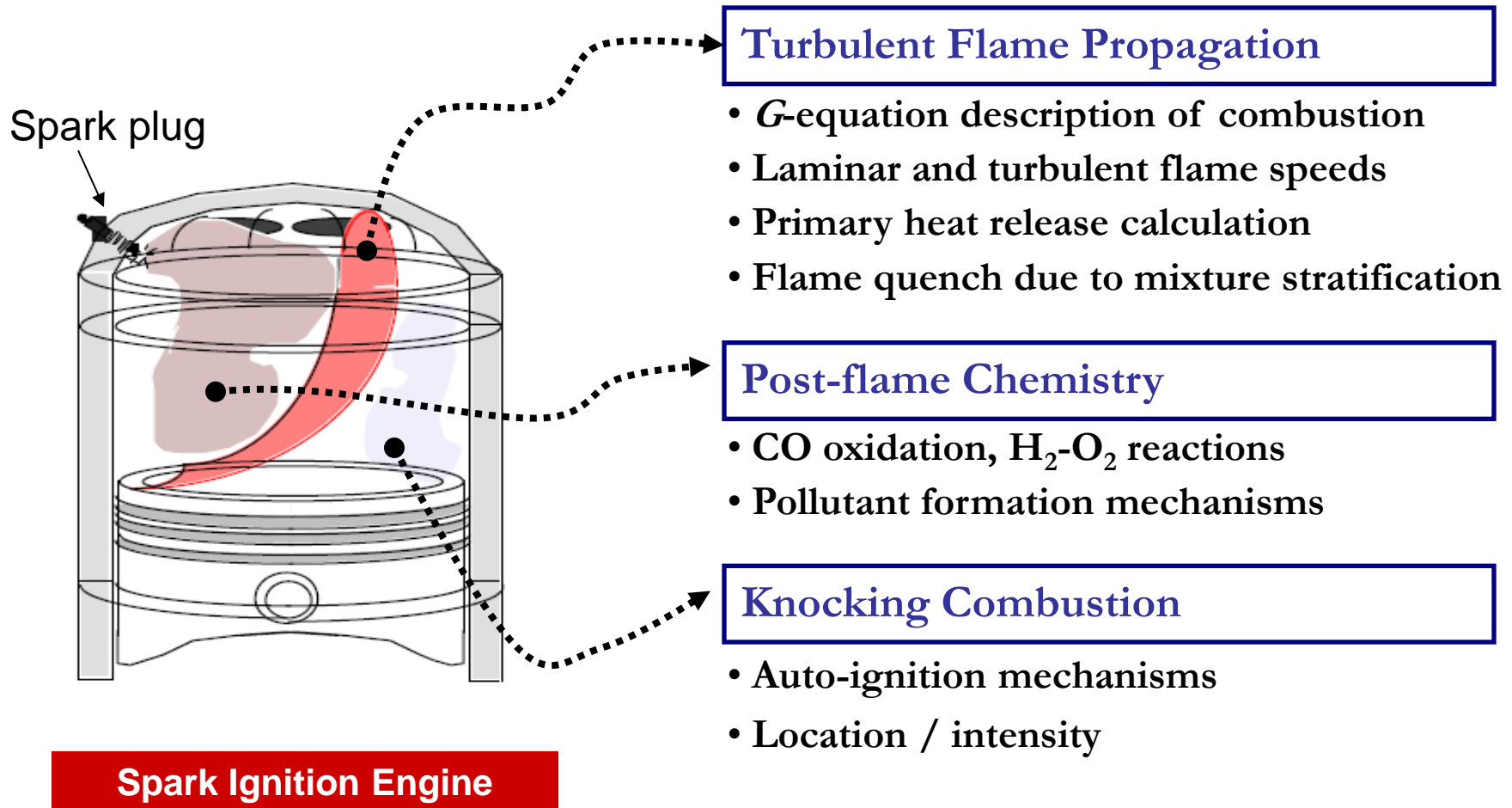
Full	AMC	AMC+EDAC
48.27 hrs.	3.99 hrs.	2.88 hrs.





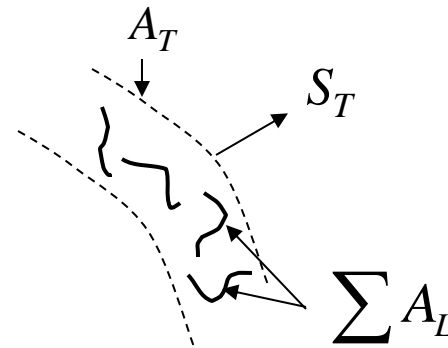
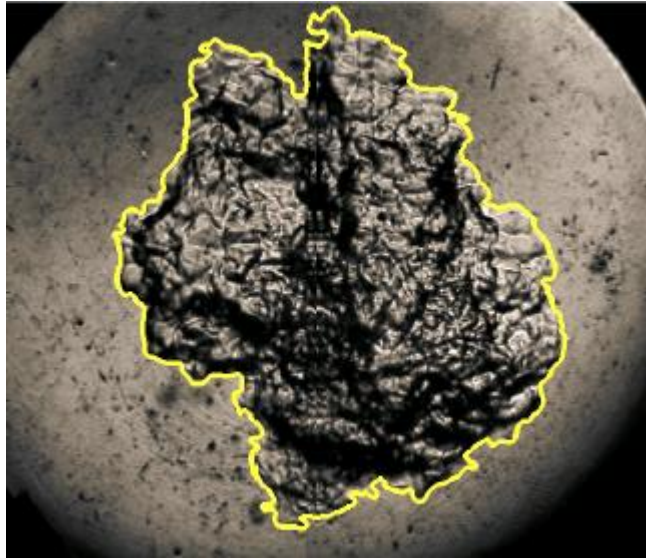
SI engine combustion modeling

Flame propagation Models with Detailed Chemistry



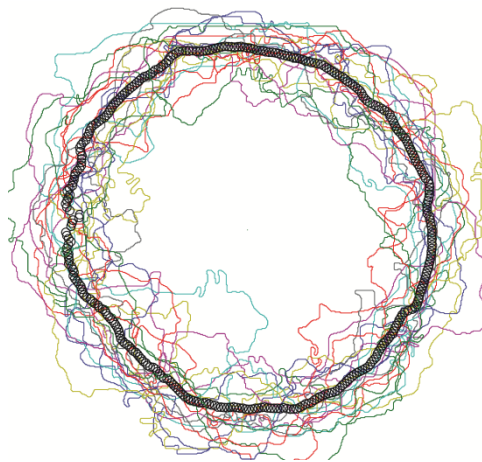


What is a turbulent flame?



Ensemble of thin (laminar) flamelets, interacting with the flow turbulence.

Due to increased surface area, turbulent flame “brush” propagates at enhanced velocity



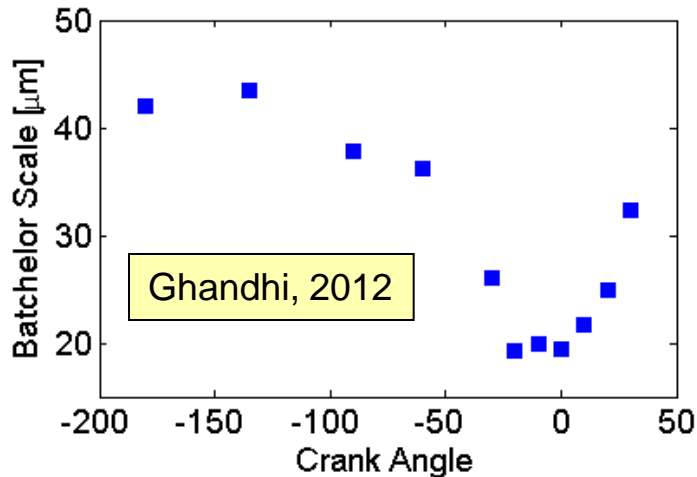
$$S_T = S_L \frac{\sum A_L}{A_T}$$



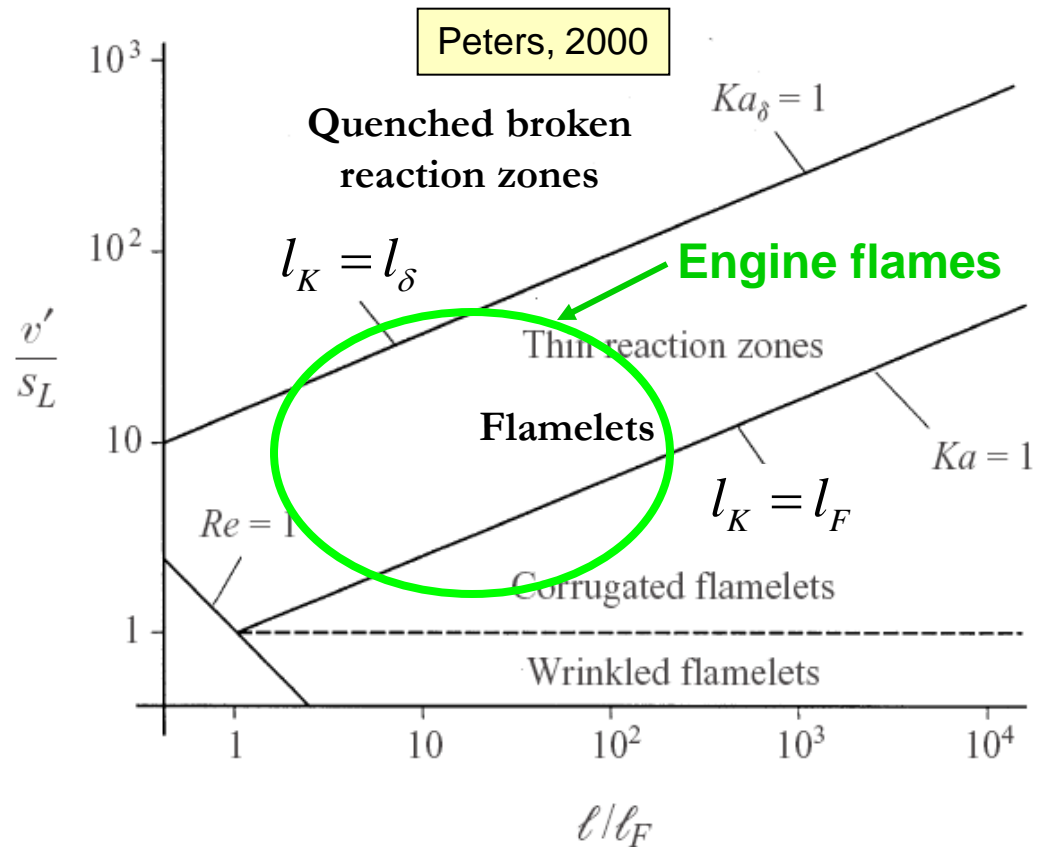
Turbulent flame structure

Kolmogorov/Batchelor length scales:

$$l_K = \left(\frac{v^3}{\varepsilon} \right)^{1/4} = Re^{-3/4} l_I$$



Combustion regime diagram



Laminar flame thickness:

$$l_F = \frac{(\lambda / c_p) |_{T_0}}{\rho_u S_L} \sim 20 \mu\text{m}$$

If $l_K < C_{m3} l_\delta = C_{m3} 0.1 l_F$, local $S_T^0 = 0$

Liang, 2007

It is not possible to resolve a turbulent flame on a practical engine simulation grid





Laminar flame speed: balance between reaction and diffusion

$$\left. \begin{aligned} \frac{\partial Y_i}{\partial t} &= D \frac{\partial^2 Y_i}{\partial x^2} + \omega_i / \rho \\ \frac{\partial T}{\partial t} &= D \frac{\partial^2 T}{\partial x^2} - \sum_{i=1}^N \Delta h_{f,i}^0 \omega_i / \rho c_p \end{aligned} \right\} S_T = \sqrt{D_T \frac{d\tilde{Y}_i}{dt}} \quad - \text{Mallard, Le Chatelier}$$

Consider the single component system:

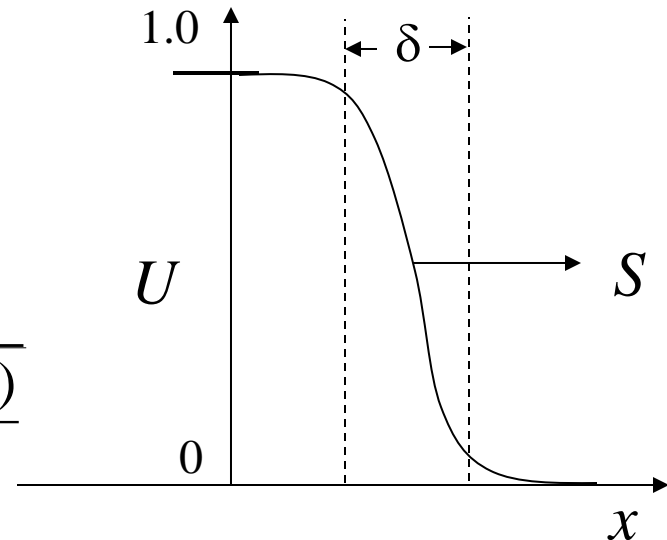
$$\frac{\partial U}{\partial t} = D \frac{\partial^2 U}{\partial x^2} + F(U) \quad \text{with } U = \frac{T - T_{unburned}}{T_{burned} - T_{unburned}} \quad \text{and } F(U) = \beta U^{m+1} (1-U)^m$$

Admits a traveling wave solution

$$U(x - St) = \left[1 / \left(1 + e^{\frac{mS}{D}(x-St)} \right) \right]^{1/m}$$

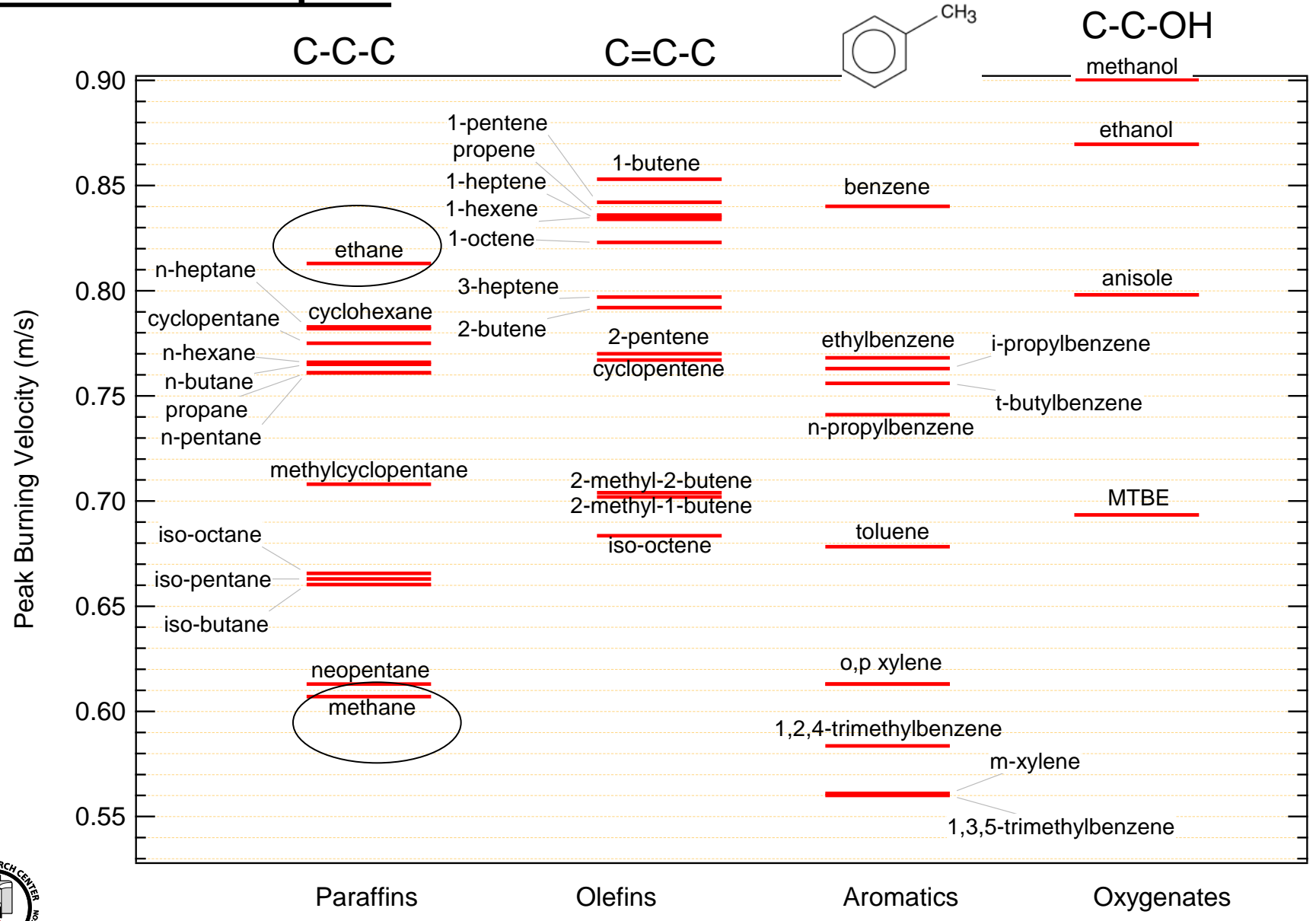
where

$$S = \sqrt{\frac{D\beta}{m+1}} \quad \text{and} \quad \delta = \frac{D}{mS} = \sqrt{\frac{D(m+1)}{\beta m^2}}$$





Laminar flame speed

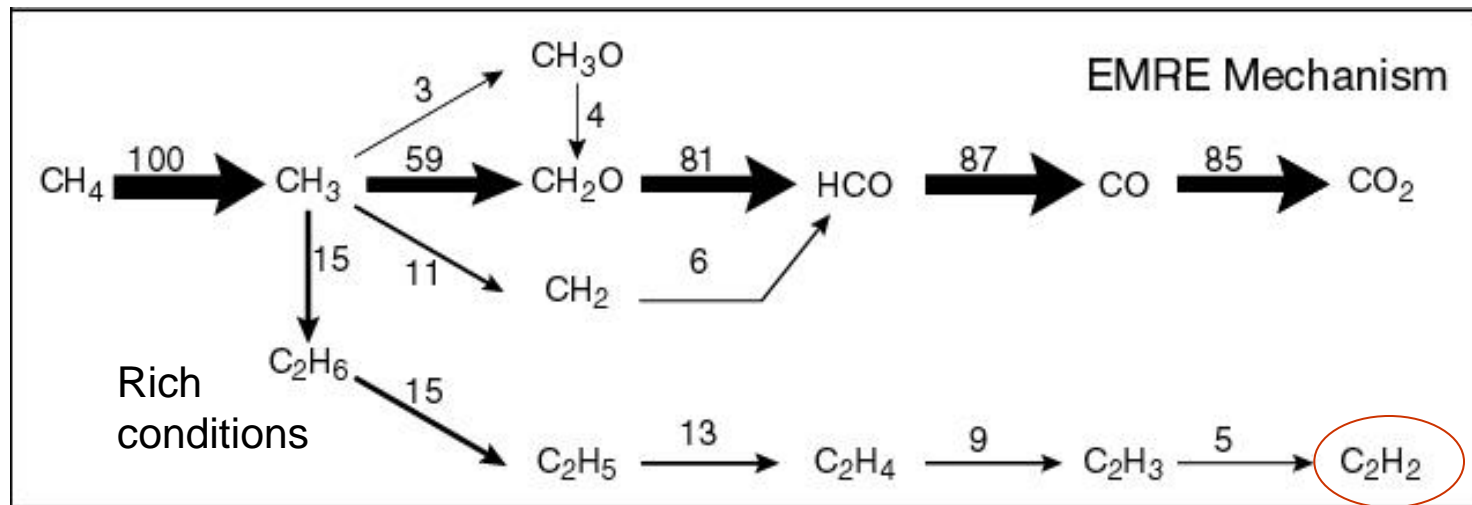




Importance of chemistry - Methane

Flux analysis: oxidation proceeds through methyl

– slow path, high activation energy due to tight C-H₃ bonds



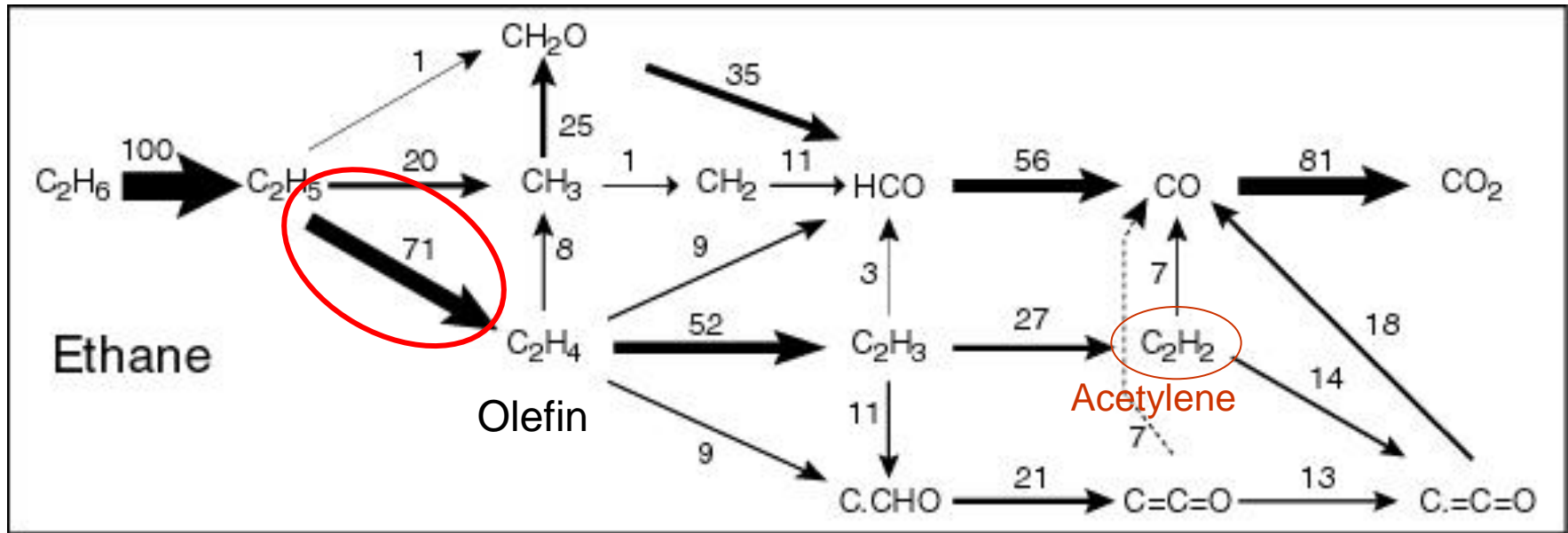
Acetylene



Importance of chemistry - Ethane

- Limited flux through slow methyl channels
 - hydrogen abstraction leaves weaker secondary C-H₂ bonds
- Greater flux through chain branching pathways, e.g.,

$$\text{H} + \text{O}_2 \leftrightarrow \text{OH} + \text{O}$$
- Ignition delays are very sensitive to rates of H atom production

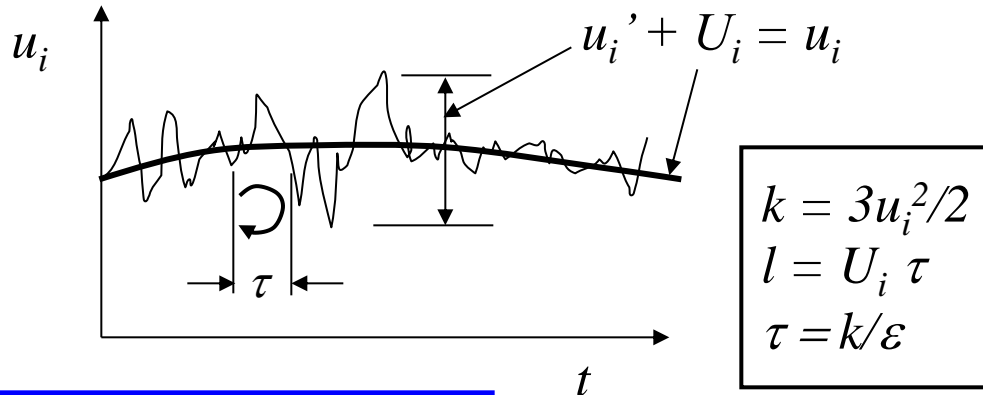


Ignition delay Ethane < Ignition delay Methane



Diffusion: Turbulence models

(RANS - RNG k-ε)



$$\rho \frac{Dk}{Dt} = P - \rho\epsilon + \text{Diffusion}$$

$$\rho \frac{D\epsilon}{Dt} = C_1 \frac{P\epsilon}{k} - C_2 \rho \frac{\epsilon^2}{k} + \text{Diffusion} - R + C_3 \rho \epsilon (\nabla \cdot \mathbf{u})$$

$$R = \frac{C_\mu \rho \eta^3 (1 - \eta/\eta_0) \epsilon^2}{1 + \beta \eta^3} \frac{1}{k}$$

$$\eta = \frac{k}{\epsilon} \sqrt{2S_{ij}S_{ij}} \sim \text{turbulent/mean flow time scale}$$

$$D_T = C_\mu k^2 / \epsilon$$

Production

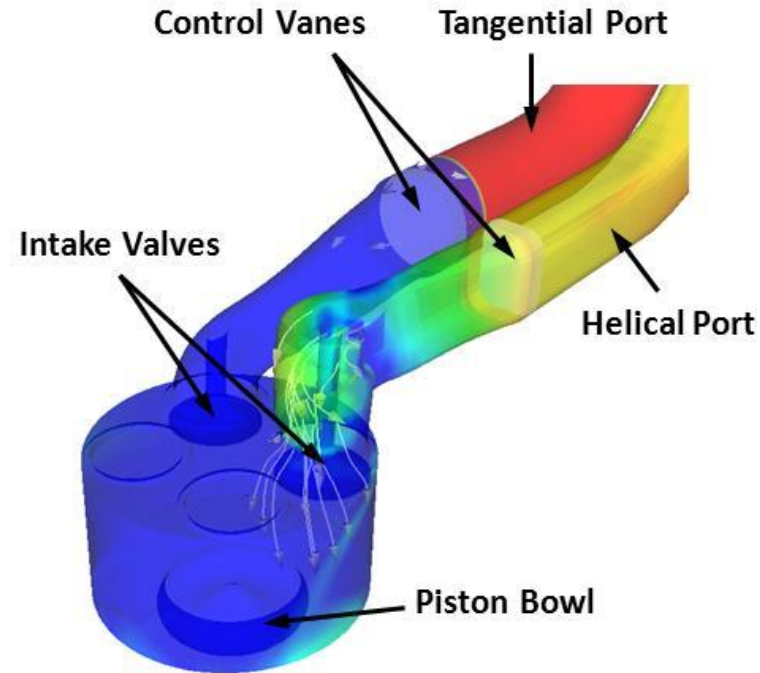
$$P = -\rho u_i u_j S_{ij}$$

Mean flow strain rate

$$S_{ij} = \frac{1}{2} (\partial u_i / \partial x_j + \partial u_j / \partial x_i)$$

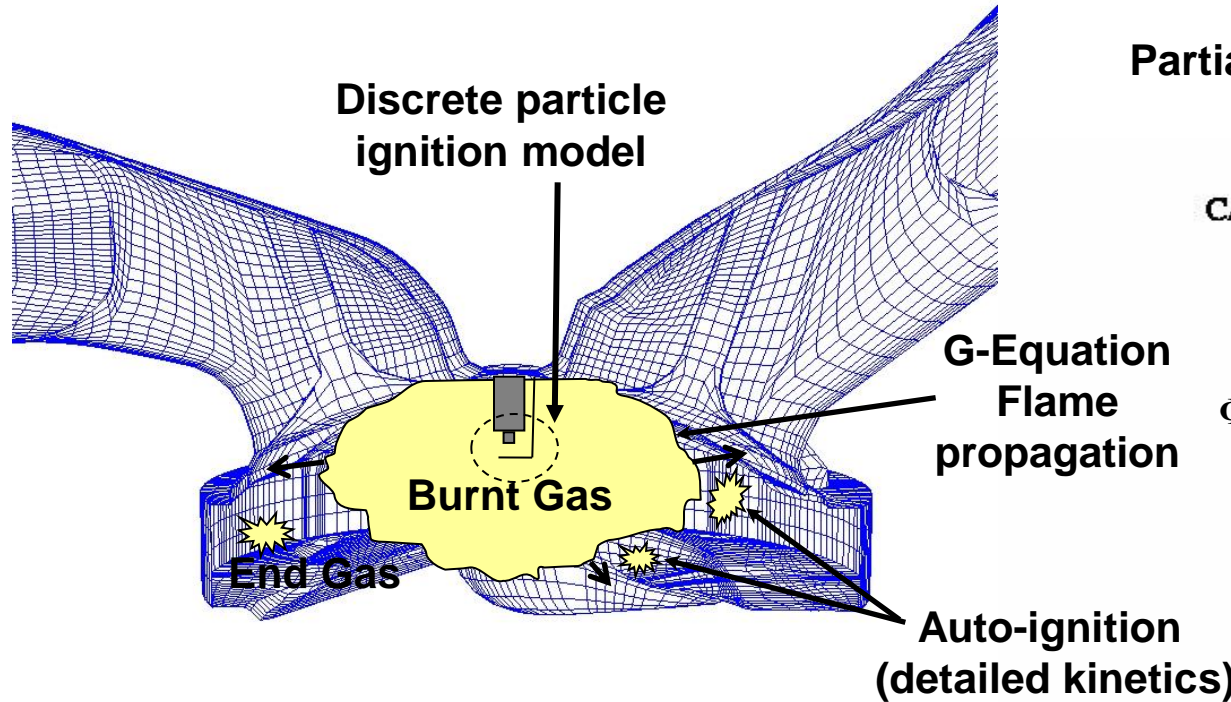
Reynolds stresses

$$u_i u_j - \frac{2}{3} k \delta_{ij} = -2v_t (S_{ij} - \frac{1}{3} (\nabla \cdot \mathbf{u}) \delta_{ij})$$

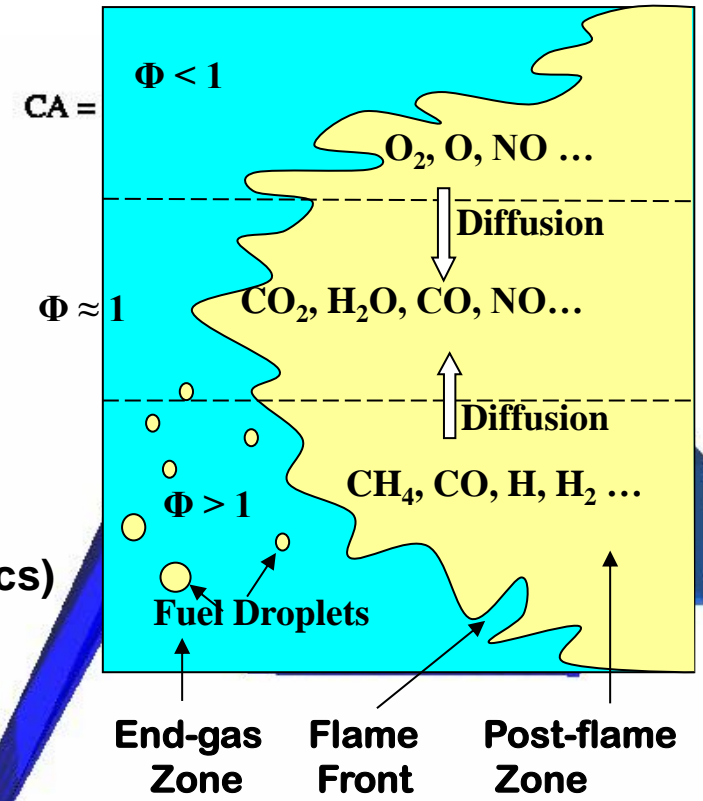




Ignition and level set (G-equation) models



Partially Premixed Flame (DI Engine)



S_T from flame speed correlations

Burned gas: $G > 0$
 Unburned gas: $G < 0$

$$\frac{\partial \tilde{G}}{\partial t} + (\vec{v}_f - \vec{v}_{vertex}) \cdot \nabla \tilde{G} = \frac{\bar{\rho}_u}{\bar{\rho}} S_T^0 |\nabla \tilde{G}| - D_T \tilde{k} |\nabla \tilde{G}|$$





Turbulent flame speed correlations

$$\frac{S_T}{S_L \cdot I_0} = 1 + \underbrace{\left[1 - \exp\left(-\frac{C_{m2} \cdot (t - t_{ign})}{\tau} \right) \right]^{1/2}}_{\text{Progress Term}} \cdot \left\{ -\frac{a_4 b_3^2 l}{2b_1 l_F} + \left[\left(\frac{a_4 b_3^2 l}{2b_1 l_F} \right)^2 + a_4 b_3^2 \frac{u'l}{S_l l_F} \right]^{1/2} \right\}$$

Peters, 2000

Stretch factor:

$$I_0 = 1 - \underbrace{\left(\frac{l_F}{15 \cdot l} \right)^{1/2} \left(\frac{u'}{S_L} \right)^{3/2}}_{\text{Turbulence stretch}} - \underbrace{2 \frac{l_F}{r_K} \cdot \frac{\rho_u}{\rho_K}}_{\text{Curvature}}$$

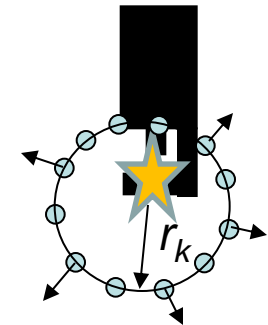
Discrete Particle Ignition Kernel (DPIK) model

Characteristic Timescale:

$$\tau = \frac{k}{\varepsilon}$$

Transition criterion:

$$r_k \geq C_{m1} \cdot l_I = C_{m1} \cdot 0.16 \frac{k^{1.5}}{\varepsilon}$$



Fan, 2000

$$\frac{\partial \tilde{G}}{\partial t} + (\vec{v}_f - \vec{v}_{vertex}) \cdot \nabla \tilde{G} = \frac{\bar{\rho}_u}{\bar{\rho}} S_T^0 |\nabla \tilde{G}| - D_T \tilde{k} |\nabla \tilde{G}|$$





Laminar flame speed correlations

Power Law (Metghalchi & Keck, 1982):

$$S_L = S_{L,0} \left(\frac{T}{T_0} \right)^\alpha \left(\frac{p}{p_0} \right)^\beta (1 - 2.1Y_{dil})$$

$$\alpha = 2.18 - 0.8(\varphi - 1)$$

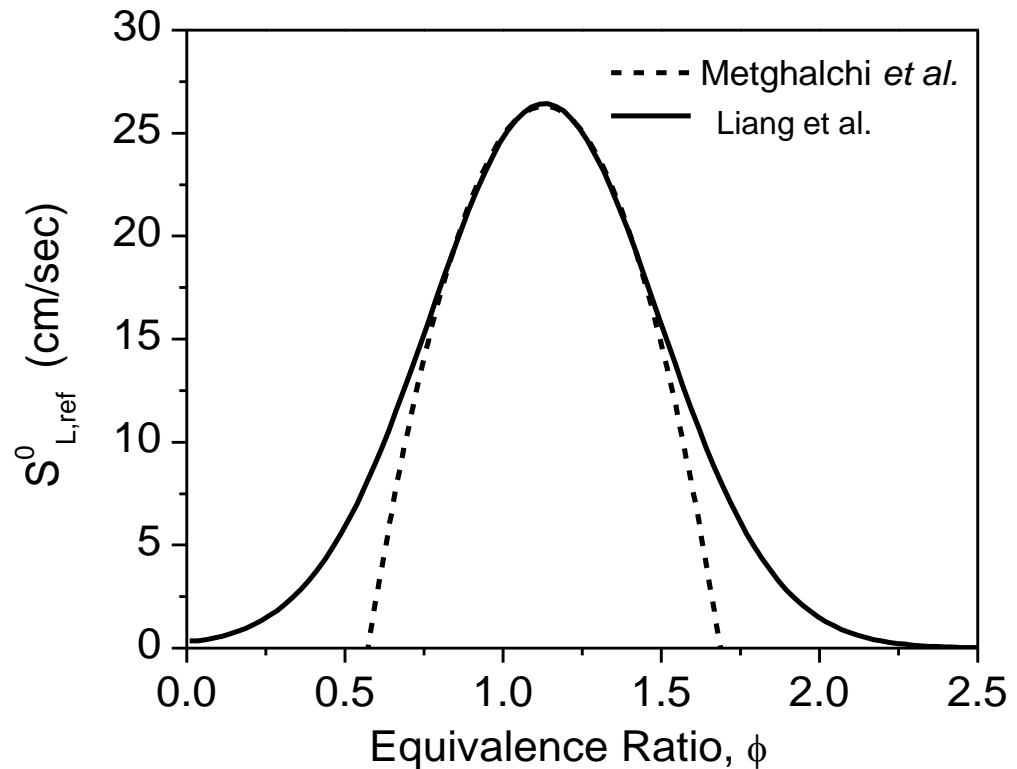
$$\beta = -0.16 + 0.22(\varphi - 1)$$

Reference State: 300K, 1bar

$$S_{L,0} = B_m + B_2(\varphi - \varphi_m)^2$$

Liang et al. :

$$S_{L,0} = \omega \varphi^\eta \exp(-\xi(\varphi - \sigma)^2)$$



For *iso*-octane, $\omega = 26.9$ $\eta = -0.134$ $\xi = 3.86$ $\sigma = 1.146$

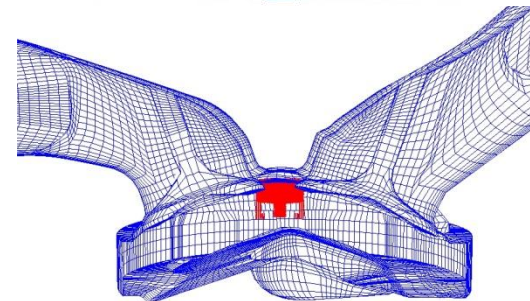
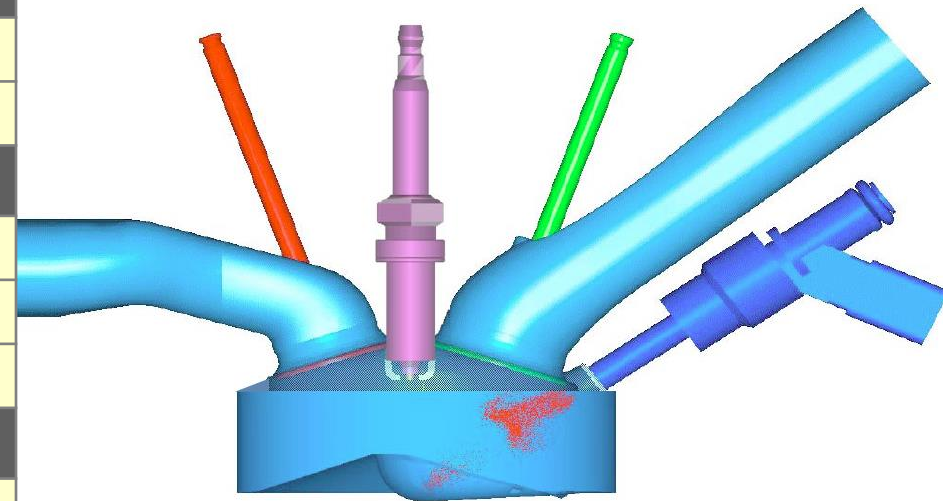


Validation - PFI/DI gasoline engines

Bore × Stroke	89 mm × 79.5 mm
Compression Ratio	12 : 1
Engine Speed	1500 rev/min
<i>PFI Mode</i>	
Spark timings (ATDC)	-44, -40, -36, -32
MAP (kPa)	65
<i>DI Mode (Spark timing sweeps)</i>	
Spark timings (ATDC)	-32, -28, -24, -20
MAP (kPa)	75
End of Injection (ATDC)	- 72
<i>DI Mode (Manifold-Absolute-Pressure sweeps)</i>	
MAP (kPa)	75, 80, 90, 100
Spark timing (ATDC)	- 33
End of Injection (ATDC)	- 68
<i>DI Mode (End-Of-Injection sweeps)</i>	
End of Injection (ATDC)	-76, -72, -68, -64
MAP (kPa)	75
Spark timing (ATDC)	- 32

Based on MIT PRF Mechanism
(25 species, 51 reactions)

Model constants: $C_{m1}=2.0$, $C_{m2}=1.0$
(Fixed in all cases)

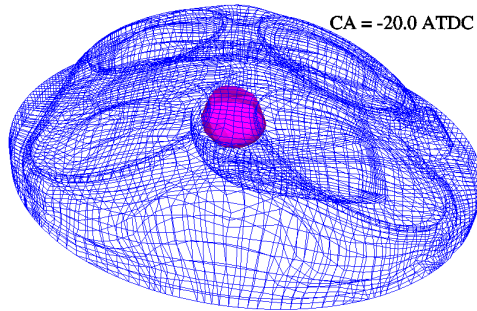


DI Configuration



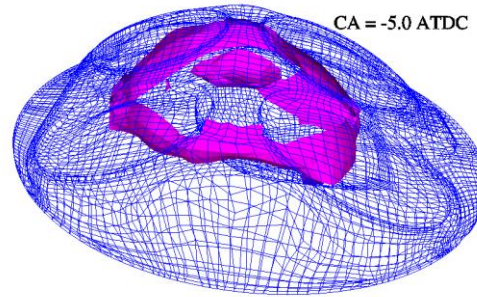
Validation - PFI engine operation

Spark Timing = 40 BTDC



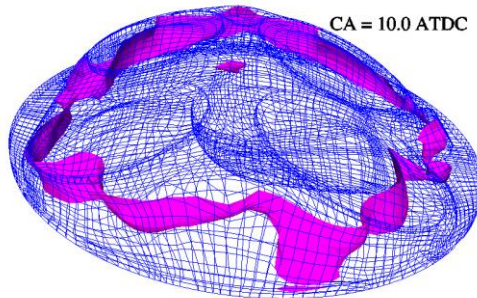
CA = -20.0 ATDC

CA = -20 ATDC



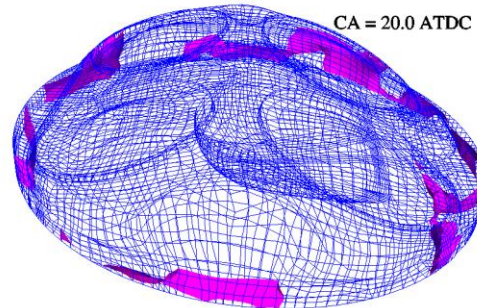
CA = -5.0 ATDC

CA = -5 ATDC



CA = 10.0 ATDC

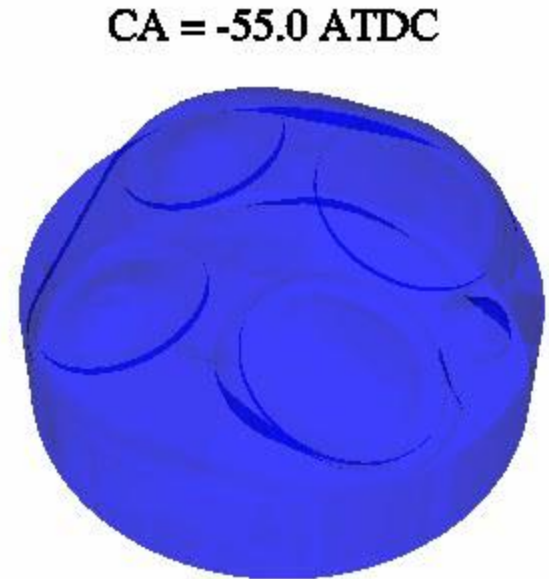
CA = 10 ATDC



CA = 20.0 ATDC

CA = 20 ATDC

Evolution of the G=0 surface



CA = -55.0 ATDC

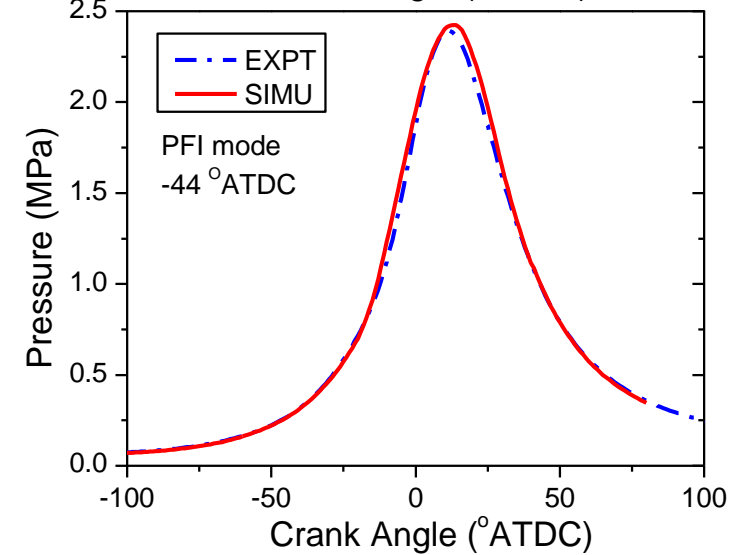
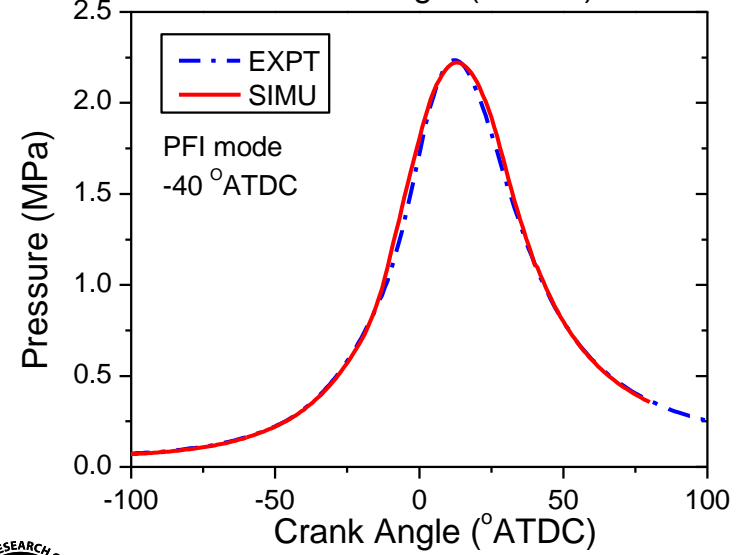
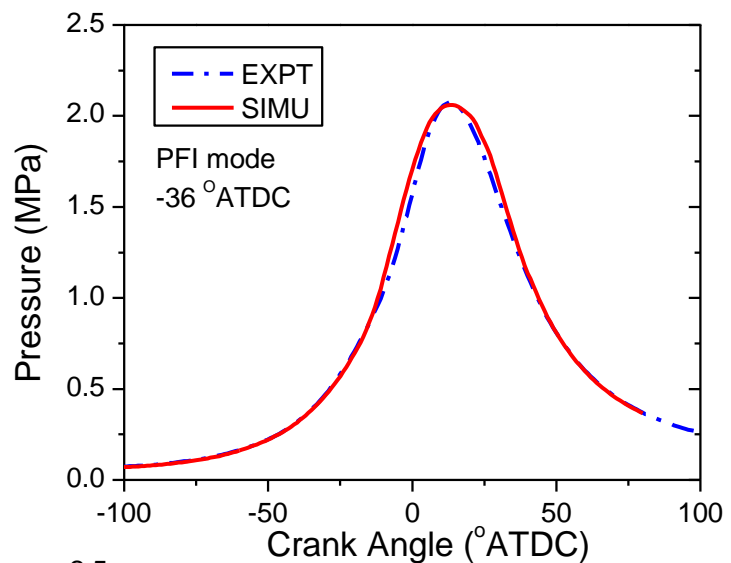
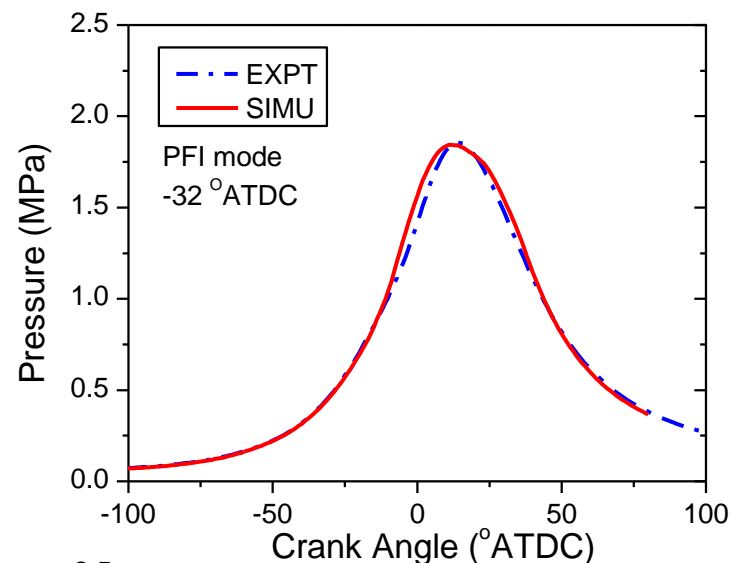


Evolution of Temperature





Validation - PFI engine operation



Spark Timing
-44, -40, -36,
-32 ATDC
Engine Speed
1500 rev/min

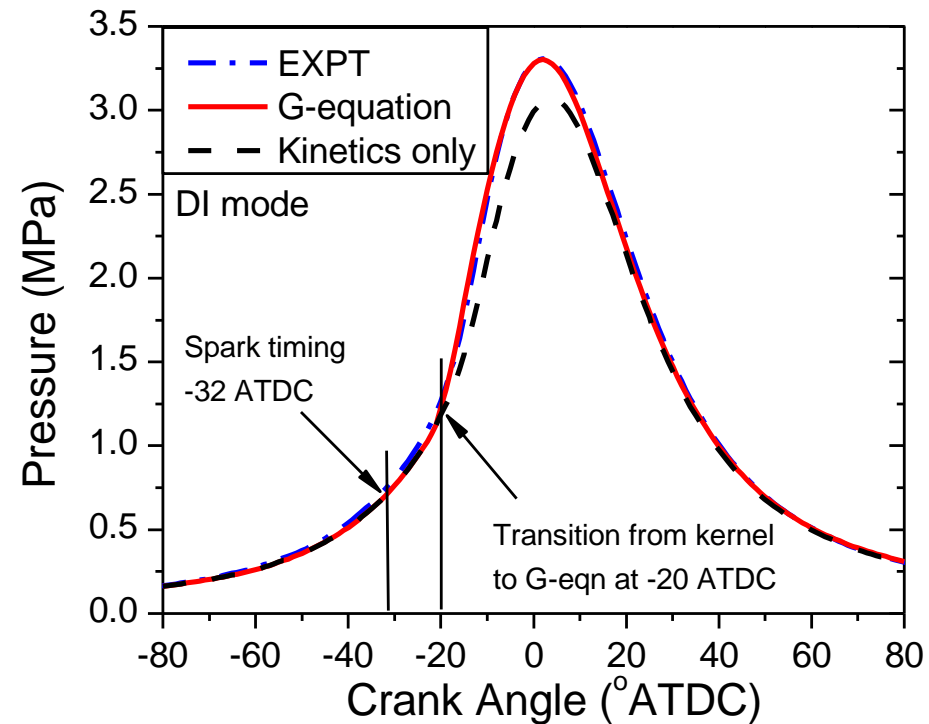
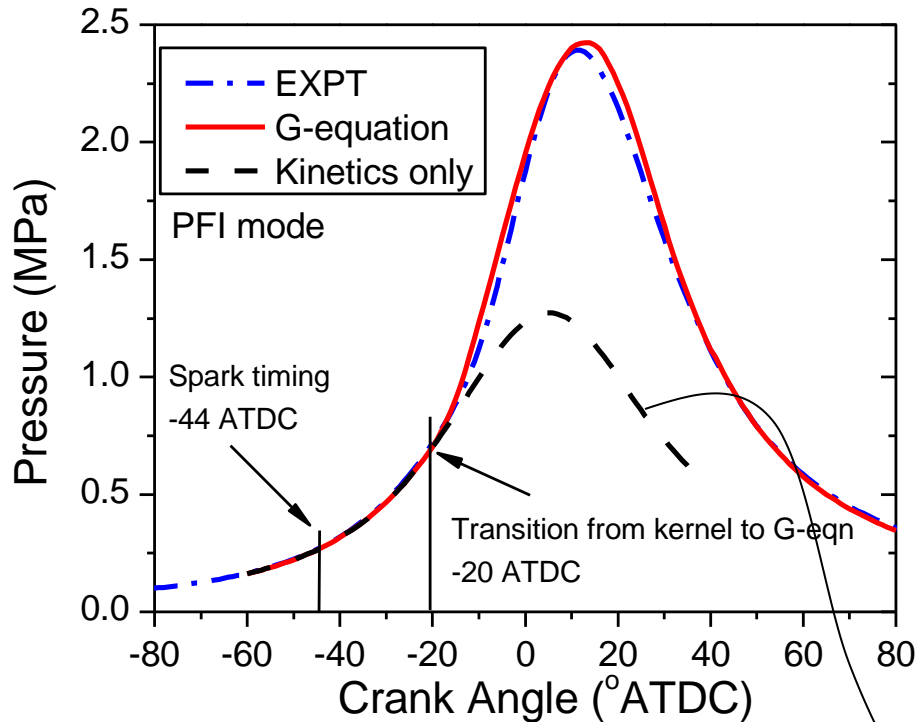




Role of flame propagation

Explore Kinetics-Controlled Formulation for Turbulent Flame Propagation:

After ignition kernel stage, each cell is modeled as a WSR, detailed chemistry is applied. “Flame propagation” is controlled by heat conduction and auto-ignition.



Mallard-Le Chatelier propagating wave speed: $S_T = \sqrt{D \frac{dY_i}{dt}}$



Role of flame propagation

PFI case

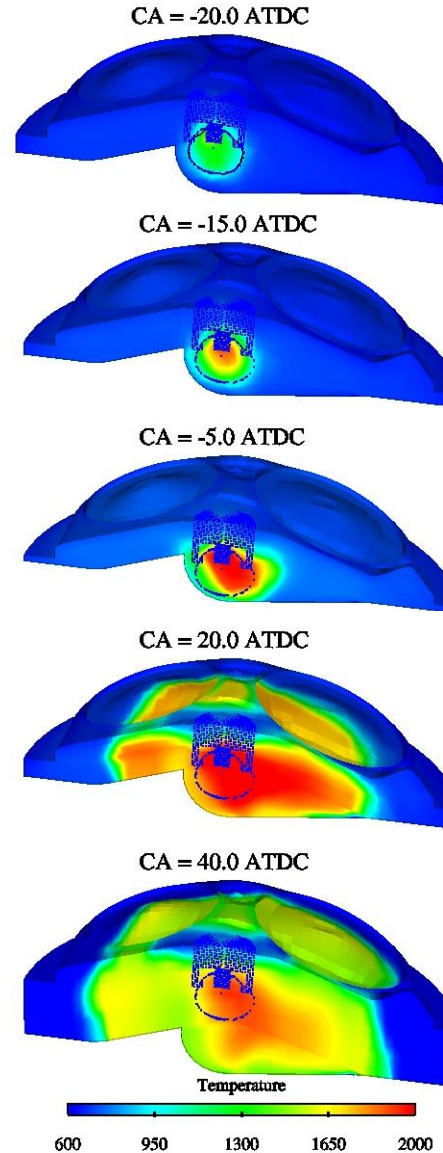
Spark timing = -44 ATDC

Summary:

Auto-ignition chemistry alone is NOT sufficient to properly model flame propagation.

Turbulence enhancing effect on flame propagation speed in SI engines CANNOT be neglected.

Kinetics Controlled



G-equation

